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GAS TURBINE FACE SEAL THERMAL DEFORMATION AND COMPUTER PROGRAM FOR CALCULATION OF AXISYMMETRIC TEMPERATURE FIELD

by Terrence E. Russell, Gordon P. Allen,
Lawrence P. Ludwig, and Robert L. Johnson

Lewis Research Center
Cleveland, Ohio

NATIONAL AERONAUTICS AND SPACE ADMINISTRATION • WASHINGTON, D. C. • DECEMBER 1969



0132396

1. Report No. NASA TN D-5605	2. Government Accession No.	3. Recipient's Catalog No.	
4. Title and Subtitle GAS TURBINE FACE SEAL THERMAL DEFORMATION AND COMPUTER PROGRAM FOR CALCULATION OF AXISYMMETRIC TEMPERATURE FIELD		5. Report Date December 1969	
7. Author(s) Terrence E. Russell, Gordon P. Allen, Lawrence P. Ludwig, and Robert L. Johnson		6. Performing Organization Code	
9. Performing Organization Name and Address Lewis Research Center National Aeronautics and Space Administration Cleveland, Ohio 44135		8. Performing Organization Report No. E-4389	
12. Sponsoring Agency Name and Address National Aeronautics and Space Administration Washington, D.C. 20546		10. Work Unit No. 126-15	
		11. Contract or Grant No.	
		13. Type of Report and Period Covered Technical Note	
		14. Sponsoring Agency Code	
15. Supplementary Notes			
16. Abstract A computer program, which is general and can be applied to a variety of steady-state thermal problems, is presented in detail. The program is written in FORTRAN IV language. Application of the program to a specific mainshaft seal design is illustrated; both computer input and output data are given. A sample problem, having an exact solution, is also given as a means of demonstrating program accuracy.			
17. Key Words (Suggested by Author(s)) Seal Steady state Computer program Axisymmetric Heat transfer Thermal deforma- Temperature tion		18. Distribution Statement Unclassified - unlimited	
19. Security Classif. (of this report) Unclassified	20. Security Classif. (of this page) Unclassified	21. No. of Pages 110	22. Price * \$3.00

* For sale by the Clearinghouse for Federal Scientific and Technical Information
Springfield, Virginia 22151



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GAS TURBINE FACE SEAL THERMAL DEFORMATION AND COMPUTER PROGRAM FOR CALCULATION OF AXISYMMETRIC TEMPERATURE FIELD

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Lewis Research Center

SUMMARY

The effects of seal deformation on seal balance are pointed out. In particular, divergent sealing faces are shown to be undesirable. As a first step in determining sealing face deformation, a computer program is presented for calculating the temperature field in the arbitrary body of revolution with arbitrary thermal boundary conditions. The program, which is written in FORTRAN IV language for an IBM 7094 digital computer, is general and can be applied to a variety of problems. Application of the program to a specific gas turbine mainshaft seal is demonstrated in detail; both computer input and output data are given. The program is also used to solve an example problem which has an exact solution; thus a partial check on program accuracy is provided.

INTRODUCTION

Face seals in advanced gas turbine engines will be subjected to temperatures, pressures, and sliding surface speeds higher than that of current engine practice. Increases in temperature arise from continuing increases in flight speed and turbine inlet temperature (ref. 1), increases in pressure result from use of higher pressure ratio compressors, and increases in surface speeds are due in part to increases in shaft diameter needed to carry increases in torque. As an example, proposed advanced engines have seal sliding speeds to 500 feet per second (127 m/sec) (ref. 2) as compared to 350 feet per second (88.9 m/sec) in engines in current use. In order to cope with these higher temperatures, pressures, and speeds, the contacting-type face seal may be replaced with noncontacting face seals such as the hydrostatic and hydrodynamic type (ref. 3). However, regardless of the type of face seal used, deformation of the sealing faces, due to thermal gradients, pressures, and centrifugal forces, will have significant effects on seal performance (ref. 4). In particular, deformations due to thermal gradients are a

major problem area. The first step in determining thermal deformation is calculation of temperature distribution in the seal assembly. Such calculation by computer program is the subject of this report. The specific objectives of this study were to (1) present in detail a computer program for calculation of temperature distribution in axisymmetric bodies, (2) show how the computer program is applied to mainshaft seal thermal analysis, and (3) demonstrate program accuracy by comparison with a thermal problem having an exact solution.

The computer program for calculation of temperature distribution is written in FORTRAN IV computer language for use on an IBM 7094 digital computer. The program is quite general and can be applied to a variety of axisymmetric body problems. The calculation procedure requires that these bodies be divided into an arbitrary finite number of axisymmetric volume elements or nodes. These nodes need not be equal in cross section. The program will take into account contact resistance at the interface between nodes and will also account for material properties that vary from node to node. Also provisions are made in the program to handle varying gas temperatures along the seal boundaries and internal viscous heat generation within the fluid at the boundaries.

SYMBOLS

A	area, ft ²
A _x	cross section area, ft ²
a	outer radius of rotor or stator, ft
C	thermal conductance, Btu/(sec)(°F)
C _f	skin friction coefficient
C _M	torque coefficient
C _p	specific heat, Btu/(lbm)(°F)
D	hydraulic diameter, ft
D _L	characteristic length for liquid film cooling, ft
d	differential
F	function of
f	view factor for radiation
Gr	Grashof number
Gr _D	Grashof number based on diameter, $D_o^3 g_o (T_b - T_s) / \nu_f^2 T_f$
Gr _L	Grashof number based on length, $L^3 g_o (T_b - T_s) / \nu_f^2 T_f$

g_0	gravitational acceleration, ft/sec ²
H	convective conductance, Btu/(sec)(°F)
h	heat transfer coefficient, Btu/(ft ²)(sec)(°F)
K	β/ω
k	thermal conductivity, Btu/(ft)(sec)(°F)
L	length of cylinder or surface, ft
Δl	axial length, in. or ft
N	radiative conductance, Btu/(sec)(°F)
Nu	Nusselt number, hD_L/k
P _w	wetted perimeter, ft
Pr	Prandtl number
Pr _f	Prandtl number of boundary film, $[C_p \mu/k]_f$
Q	heat flux, Btu/sec
q	internal heat generation, Btu/sec
q _f	fluid internal heat generation, Btu/sec
R	thermal resistance, (sec)(°F)/Btu
R _c	contact resistance, (sec)(°F)/Btu
Re	Reynolds number
Re _c	critical Reynolds number for transition
Re _v	Reynolds number based on total velocity, $\left(\sqrt{\omega^2 r^2 + V_a^2} \right)_s / \nu_f$
Re _w	Reynolds number based on mass flow, $W_a D / \mu_f$
Re _x	Reynolds number based on flow length, $V_\infty X / \nu_f$
Re _{ω}	Reynolds number based on rotation, $\omega r^2 / \nu_f$
r	radial coordinate, ft
Δr	radial width, in. or ft
r _{av}	average radius of element, in. or ft
r _i	inner radius of annulus between cylinders, ft
r _o	outer radius of annulus between cylinders, ft
s	clearance (e.g., seal gap), ft

T	temperature, $^{\circ}\text{F}$
T_{av}	average (or film) temperature, $^{\circ}\text{F}$
T_{in}	temperature entering fluid element, $^{\circ}\text{F}$
T_{out}	temperature leaving fluid element, $^{\circ}\text{F}$
T_{∞}	bulk fluid temperature, $^{\circ}\text{F}$
Ta_f	Taylor number of boundary film, $\omega \text{rs}^{3/2} / \nu_f^{3/2}$
V_a	axial velocity, ft/sec
V_R	linear velocity of inner cylinder, ft/sec
V_{tot}	total fluid velocity, ft/sec
V_{∞}	free stream velocity, ft/sec
W	mass flow rate, lbm/sec
W_a	mass flow per square foot of cross section, W/A_x , lbm/(ft 2)(sec)
w	over-relaxation factor
X	flow length, ft
z	axial coordinate, ft
α	coefficient of thermal expansion
β	angular velocity of fluid, rad/sec
∂	partial derivative
Δ	difference
ϵ	emissivity for radiation
μ	absolute viscosity, lbm/(ft)(sec)
ν	kinematic viscosity, ft 2 /sec
ρ	density, lbm/ft 3
τ_t	tangential shear stress at wall, lbf/in. 2
ω	rotor angular velocity, rad/sec

Subscripts:

b	at fluid bulk temperature
c	convective
e	environment
ei	between element and environment

es	from environment to element
f	at boundary film temperature
i	element
j	neighbor element of i
ji	between neighbor and element
k	environment "area" affecting element i by radiation
ki	between environment "area" k and element
l	environment "area" affecting element i by convection
lam	laminar
li	between environment "area" l and element
r	radiation
s	surface
se	from element to environment
tr	transition
turb	turbulent

DISCUSSION OF THERMAL DEFORMATION IN SEALS

Figure 1 is a schematic drawing of a gas turbine mainshaft seal for bearing sumps. The seal restricts leakage of surrounding high temperature, high pressure gas into the

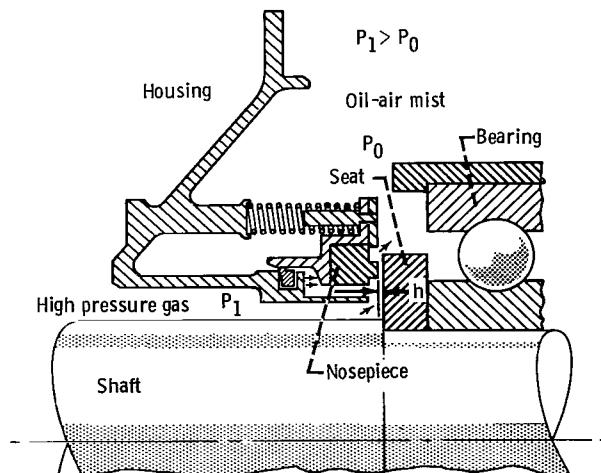


Figure 1. - Mainshaft seal for bearing sump in gas turbine engine.

sump. The gas leakage, through the seal into the sump, acts as a sweep gas which helps prevent oil leakage. However, it is desirable to minimize this gas leakage, since the hot gas degrades the lubricant and adds to the cooling requirements of the lubricant system.

Seal leakage and wear are grossly affected by seal force balance and it has been recognized that deformation of the sealing faces (which form the dam) can have a significant effect on the seal force balance (ref. 5). A discussion of seal force balancing can be found in reference 6. The manner in which the sealing face deformation affects the seal force balance and stability of a conventional face seal is discussed in reference 7. In general, thermal deformations cause the seal faces (dam) to form a nonparallel leakage path, and the pressure within these sealing faces is greatly dependent on the shape (convergent or divergent) of this leakage path; thus the force balance is affected by the thermal deformation.

Thermal gradients usually produce sealing gaps divergent from the dam inside diameter to the outside diameter. Thus, it is usually advantageous to locate the higher pressure at the seal outside diameter since this will result in convergence with respect to the leakage direction. However, many face seals are designed with the higher pressure at

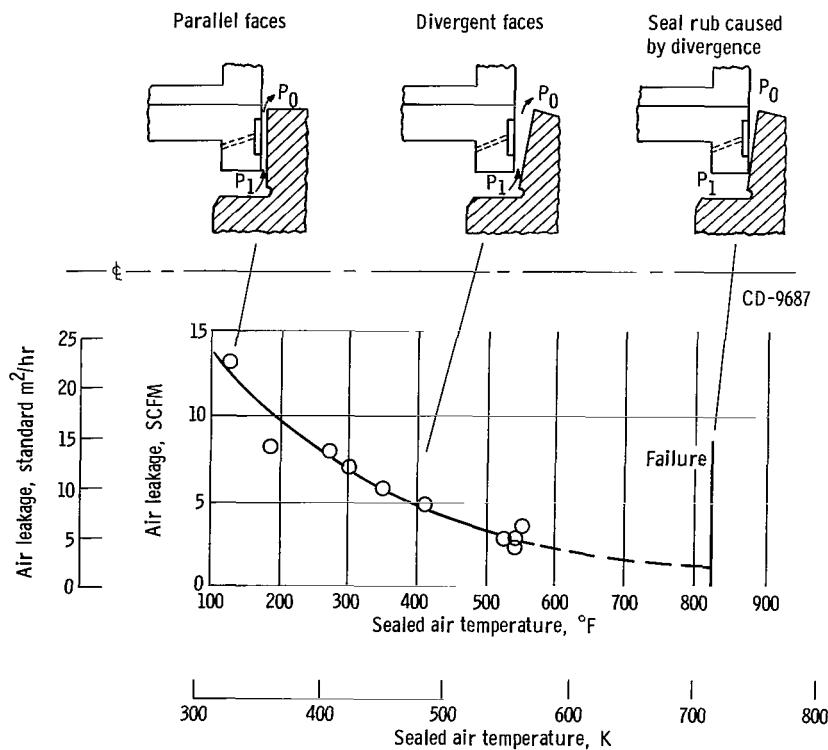


Figure 2. - Effect of thermal deformation on air leakage of orifice compensated hydrostatic seal. Sliding speed, 200 feet per second (61.0 m/sec); pressure differential, 100 pounds per square inch (6.89×10^4 N/m 2). (Data from ref. 4.)

the dam inside diameter and the gas turbine face seal is an example of this construction practice. The advantage of placing the higher pressure gas at the dam inside diameter puts the oil mist at the outside diameter; thus centrifugal force also acts to prevent oil leakage.

Thermal deformation also affects operation of hydrostatic seals. Figure 2, from reference 4, shows the effect of sealing face deformation on leakage through a hydrostatic seal operating at 200 feet per second (61.0 m/sec) and 100 pounds per square inch (6.89×10^4 N/m²) pressure differential. With a sealed air temperature of 120° F (322 K), the seal leakage is approximately 13 SCFM (0.0062 standard m³/sec) and as the air tem-

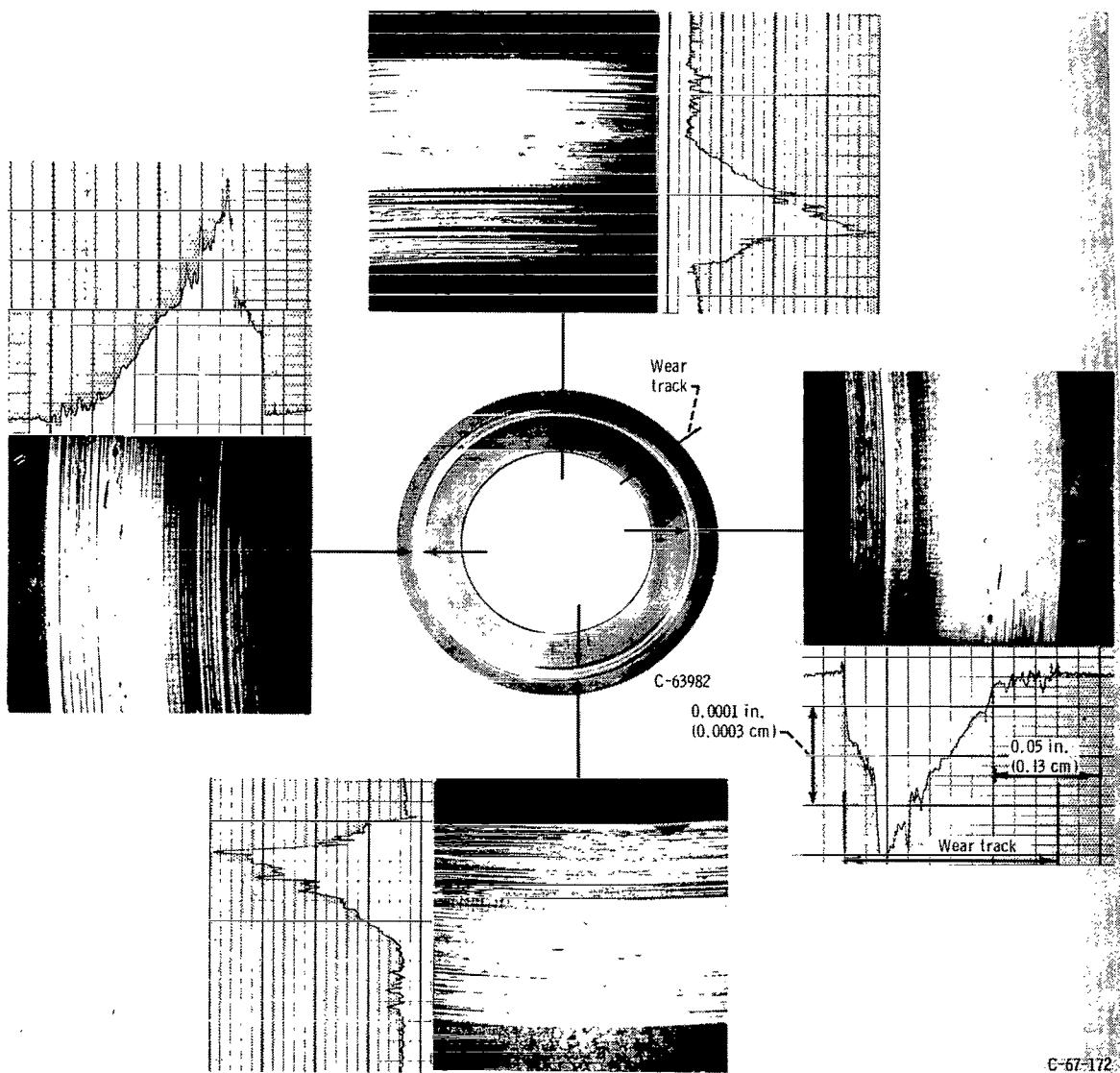


Figure 3'. - Overall wear pattern, surface profile traces, and photomicrographs of tungsten carbide seal seat. Sodium temperature, 1000° F (538° C); operating time, 4 hours; sliding velocity, 79 feet per second (24 m/sec); pressure, 50 pounds per square inch gage (34 N/cm² gage). Data from ref. 6.)

perature is increased, the leakage decreases. This leakage decrease is due to increasing angular deformation of the sealing gap. The result is that the seal runs with closer clearance. Eventually as the air temperature increases still further, the deformation causes the inside diameter of the nosepiece to rub against the seal seat and failure occurs.

Seal thermal deformation effects have also been noticed in other applications. As an example, reference 6 reports that the main problem in sealing liquid sodium with a face contact seal was thermal deformation of the sealing faces. Some results of this study are repeated in figure 3 which shows the wear pattern made by a nosepiece sliding against a seal seat. Surface profile traces have been taken at intervals around the wear track. These profile traces show that the sealing faces were not parallel during operation, the greatest wear occurring at the inside diameter. The slope of the wear pattern suggests a divergence in the range of 0.006 inch per inch (0.006 m/m) of radial distance.

Regardless of the seal type (face contact, hydrostatic, or hydrodynamic), the sealing gap is usually small (0.0001 to 0.0010 in. or 0.00025 to 0.0025 cm for gas film seals) and deformations can easily be of the same magnitude, thus affecting seal performance significantly. These sealing face deformations could arise from temperature, pressure, or centrifugal force effects. Careful design can minimize undesirable effects due to pressure and centrifugal force. Deformations due to temperature gradients are usually difficult to eliminate. Even the heat generated in shearing a thin film of gas within the interface can introduce a significant and undesirable thermal gradient in the seal rings.

The preceding evidence indicates that thermal deformation can significantly affect seal performance. The first step in analysis of these thermal deformations is calculation of the temperature fields in the seal assembly, and the computer program for these calculations is given in the following sections.

ANALYSIS OF TEMPERATURE FIELDS IN AXISYMMETRIC BODIES

Shaft seals are composed of basically axisymmetric bodies. Also, the circumferential temperature gradient approaches zero for most applications. Therefore, the cylindrical coordinate system is used as a basis for analysis. The following restrictions are placed on the thermal analysis:

- (1) A steady state must exist.
- (2) An axisymmetric temperature field must exist.

Therefore, with internal heat generation, the heat conduction equation in cylindrical coordinates is (ref. 8)

$$\frac{1}{r} \frac{\partial}{\partial r} \left(kr \frac{\partial T}{\partial r} \right) + \frac{\partial}{\partial z} \left(k \frac{\partial T}{\partial z} \right) + q(r, z) = 0 \quad (1)$$

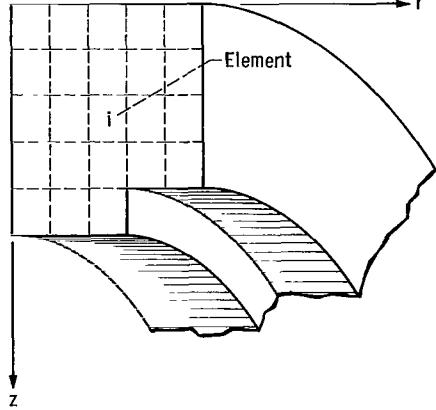


Figure 4. - Seal axisymmetric nosepiece subdivided into finite number of three-dimensional axisymmetric volume elements.

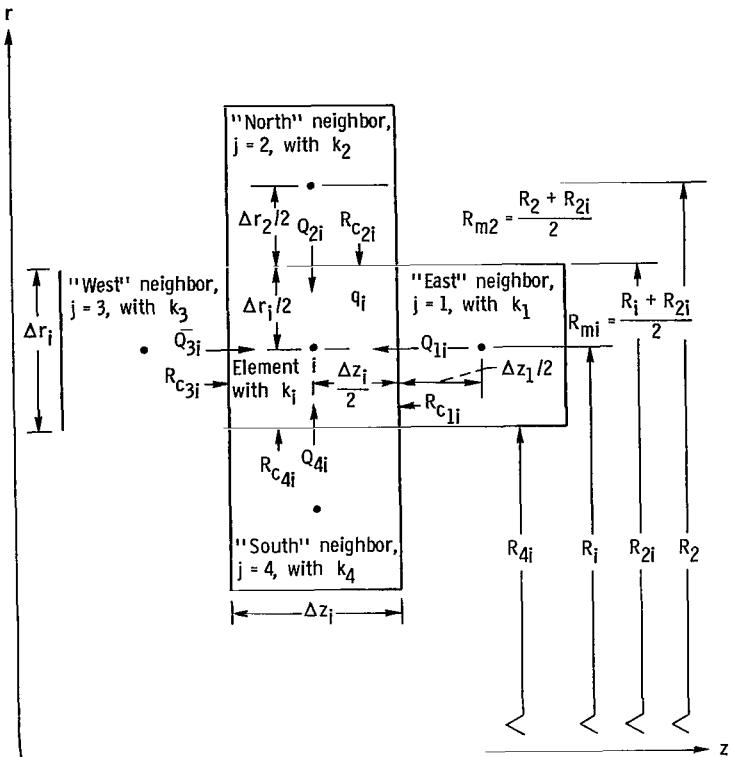


Figure 5. - Typical interior (i^{th}) element and its four neighbor elements.

where r is the radial coordinate, k is thermal conductivity, z is the axial coordinate, T is temperature, and q is internal heat generation.

Equation (1), which makes no restrictions of constant thermal conductivity k , can be approximated by a finite difference numerical approach in which thermal conductivity is held constant over small regions. In this finite difference approach, each of the axisymmetric bodies, which comprise the seal, is subdivided into a finite number of three-dimensional axisymmetric volume elements of rectangular cross section (see fig. 4). These elements need not be equal in cross-sectional area. In general, there will be P elements of which m are elements whose temperature is obtained by solving a heat balance equation and $P - m$ are elements in which the temperature is specified. Figure 4 indicates the position of a typical interior element (i^{th} element). The numbers assigned to the neighboring elements will be determined in the construction of the element pattern, but for the purpose of developing the heat balance equation these neighboring elements are numbered 1, 2, 3, and 4 (see fig. 5).

For the numerical solution, the application of the law of conservation of energy at each volume element allows good generality to be maintained. Referring to figure 5, a heat balance for steady-state conduction at element i results in the following difference equation:

$$Q_{1i} + Q_{2i} + Q_{3i} + Q_{4i} + q_i = 0$$

where the Q_{ji} terms are the heat fluxes from the neighboring elements or

$$C_{1i}(T_1 - T_i) + C_{2i}(T_2 - T_i) + C_{3i}(T_3 - T_i) + C_{4i}(T_4 - T_i) + q_i = 0 \quad (2a)$$

in which the conductances C_{ji} are computed as follows with reference to figure 5:

$$\left. \begin{aligned} R_{1i} &= \frac{1}{C_{1i}} = \frac{\frac{\Delta z_1}{2}}{2\pi R_1 \Delta r_1 k_1} + \frac{\frac{\Delta z_i}{2}}{2\pi R_i \Delta r_i k_i} + R_{c_{1i}} \\ R_{2i} &= \frac{1}{C_{2i}} \simeq \frac{\frac{\Delta R_i}{2}}{2\pi R_{mi} \Delta z_1 k_1} + \frac{\frac{\Delta R_2}{2}}{2\pi R_{m2} \Delta z_2 k_2} + R_{c_{2i}} \end{aligned} \right\} \quad (2b)$$

where R_{ji} is thermal resistance. As an example, for heat conduction from neighbor element 1 to the i^{th} element, the resistance is made up of the resistance of one-half that of the i^{th} element plus one-half that of neighbor element 1 plus the contact resistance $R_{c_{ji}}$. Thus the calculated temperature is that of the element center. However, the thermal conductivity assigned to the whole element volume is the value at the temperature of the element center.

Equation (2a) can be stated concisely as

$$\sum_{j=1}^4 C_{ji}(T_j - T_i) + q_i = 0 \quad (3)$$

where i is the element under consideration, the j 's are its four neighboring elements, and $1 \leq i \leq m$. At the outer surfaces of the axisymmetric bodies, which comprise the seal, the i^{th} element will have less than four solid neighbor elements but will have environmental radiation and convection effects on the external surface (or surfaces) (fig. 6). This means that some of the j neighbors are replaced by environmental regions which are identified as the k^{th} area for radiation and the l^{th} area for convection. It should be noted that an external surface could have both radiation and convection effects. The k^{th} and l^{th} areas would, therefore, be superimposed.

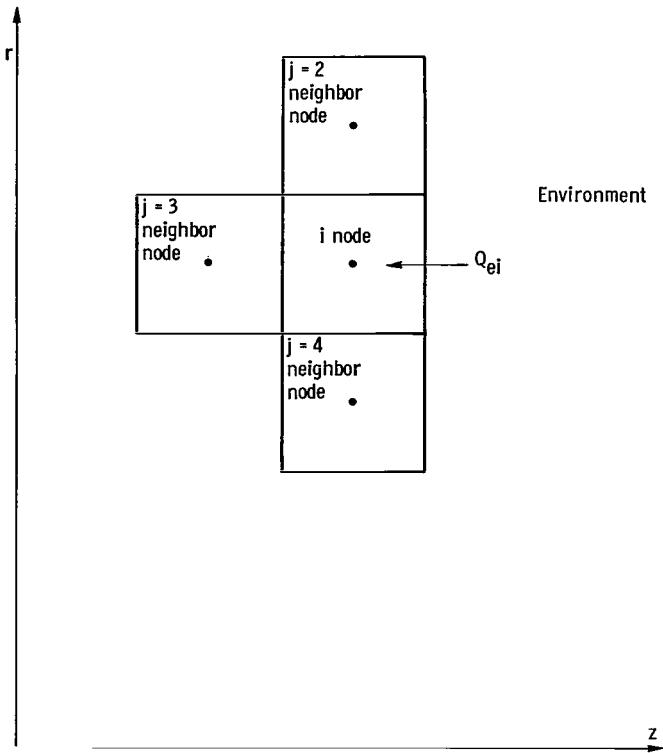


Figure 6. - Typical element with environment convection and/or radiation to one surface.

An i^{th} element could have radiation on more than one face. This radiation heat flux is

$$Q_{ki} = \sum_{k=1}^4 N_{ki}(T_k - T_i) \quad (4)$$

An i^{th} element could have more than one face with convective effects

$$Q_{li} = \sum_{l=1}^4 H_{li}(T_l - T_i) \quad (5)$$

Combining equations (3), (4), and (5) results in the difference equation for the heat balance of the i^{th} element:

$$\underbrace{\sum_{j=1}^4 C_{ji}(T_j - T_i)}_{\text{Conduction}} + \underbrace{\sum_{k=1}^4 N_{ki}(T_k - T_i)}_{\text{Radiation}} + \underbrace{\sum_{l=1}^4 H_{li}(T_l - T_i)}_{\text{Convection}} + \underbrace{q_i}_{\text{Internal heat generation}} = 0 \quad (6)$$

It should be noted that equation (6) establishes the convention that heat flowing from an element has a negative value and heat flowing into an element has a positive value.

In addition to the boundary conditions of radiation and convection, two other boundary surface conditions are possible. The heat flux may be a specified function

$$Q_{ei} \left\{ \begin{array}{l} = K_{ei} A \left(\frac{\partial T}{\partial r} \right)_i \\ = C_{ei} \left(\frac{\partial T}{\partial r} \right) \\ \text{or} \\ = C(r, z) \end{array} \right. \quad (7)$$

where $C(r, z) = 0$ for a perfectly insulated surface. Or the heat transfer coefficient may be a specified value such as

$$h_{ei} = f(r, z) \quad (\text{or } H_{ei} = f(r, z)) \quad (8)$$

Also the temperature of any element may be specified as

$$T_i = f(r, z) \quad (9)$$

The program has the special feature of calculating varying gas temperatures in flow over a surface or in small passages. In addition, heat generated within a fluid, such as that due to viscous shear in the sealing interfaces, can be accounted for. Referring to figure 7 reveals the heat balance for the center fluid element is

$$WC_p(T_{in} - T_{out}) + h_1 A_1 (T_{s1} - T_{in}) + h_2 A_2 (T_{s2} - T_{in}) + q_f = 0 \quad (10)$$

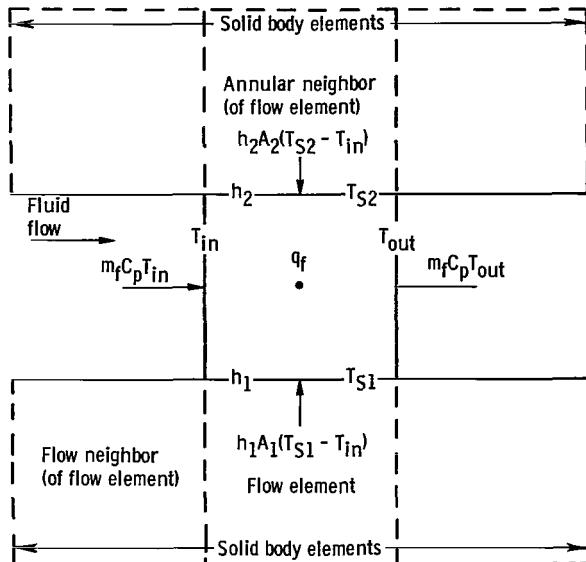


Figure 7. - Fluid volume element for varying temperature forced convection heat transfer.

in which q_f is the internal heat generated. Equation (10) enters into the element heat balance (eq. (6)) only through the determination of the fluid temperature.

Returning to the element heat balance (eq. (6)) matrix notation can be used to express this system of linear equations as follows:

$$\underbrace{- \sum_{j=1}^4 C_{ji} T_j}_{[A]} + \underbrace{\left(\sum_{j=1}^4 C_{ji} + \sum_{k=1}^4 N_{ki} + \sum_{l=1}^4 H_{li} \right) T_i}_{\{T\}} = \underbrace{\sum_{k=1}^4 N_{ki} T_k + \sum_{l=1}^4 H_{li} T_l - q_i}_{\{TL\}}$$

(11)

where $[A]$ is the $m \times m$ conductance matrix, $\{T\}$ is the $m \times 1$ temperature vector, and $\{TL\}$ is the $m \times 1$ thermal load vector.

In equations (6) and (11) it should be noted that, for interior elements, the N_{ki} and H_{li} terms vanish; also numbers are assigned to the j^{th} elements.

The matrix $[A]$ can be shown to be real, symmetric, and positive definite. The temperatures are obtained using the successive over-relaxation technique. By introducing the over-relaxation factor w , the successive over-relaxation algorithm is given for the temperature at the i^{th} element at the $(K+1)^{\text{th}}$ iteration by:

$$a_{i,i} T_i^{K+1} = a_{i,i} T_i^K + W \left[- \sum_{j=1}^{i-1} a_{i,j} T_j^{K+1} - \sum_{j=i+1}^m a_{i,j} T_j^K + (TL)_i - a_{i,i} T_i^K \right]$$

where

$$1 \leq W < 2 \text{ and } 1 < i \leq m$$

and

$$a_{i,i} = \left(\sum_{j=1}^4 C_{ji} + \sum_{k=1}^4 N_{ki} + \sum_{l=1}^4 H_{li} \right) \quad \begin{matrix} \text{diagonal term of } i^{\text{th}} \\ \text{row in matrix [A]} \end{matrix}$$

$$a_{i,j} = -C_{ji} = a_{j,i} \quad \begin{matrix} \text{off-diagonal terms of} \\ i^{\text{th}} \text{ row in matrix [A]} \end{matrix}$$

$$(TL)_i = \sum_{k=1}^4 N_{ki} T_k + \sum_{l=1}^4 H_{li} T_l + q_i \quad i^{\text{th}} \text{ thermal load term}$$

This system of m equations is iteratively solved until a specified level of convergence is obtained.

The boundary condition conductances N_{ki} and H_{li} are calculated with the aid of the empirical relations listed in table I and discussed later.

LIMITATIONS AND SCOPE

This program has a present capacity of 400 volume elements, 200 boundary condition elements, 95 varying temperature boundary elements (see Computer Input in appendix A), and 15 different materials. Several minor limitations are discussed in the section on input where the parameters involved are introduced. The program is designed for an IBM 7094 digital computer and is written in FORTRAN IV language.

Provision is made for adding subroutines to calculate additional boundary condition coefficients without interrupting the sequence of statement numbers or altering present statements. Up to four forced convection, five free convection, and two varying tempera-

TABLE I. - BOUNDARY HEAT TRANSFER COEFFICIENTS

Heat transfer type	Geometry and fluid	Regime	Coefficient equation
Forced convection	Duct flow, liquid	Laminar	$h = 1.24 (k_f/D)(Re_w Pr_f D/X)^{1/3}$
		Turbulent	$h = 0.023 (k_f/D)Re_w^{0.8} Pr_f^{0.4} \left[1 + 0.3 (D/X)^{0.7} \right]$
		Transition	$h_{tr} = h_{lam} + (h_{turb} - h_{lam})(Re - 2500)/4500$
	Sides of rotors, liquid or gas	Laminar	$h = 0.574 (k_f/r)(s/r)^{0.1} Re_\omega^{0.5} Pr_f^{1/3} / (\beta/\omega)$
		Turbulent	$h = 0.01826 (k_f/r)(s/r)^{0.1} Re_\omega^{0.8} Pr_f^{1/3} / (\beta/\omega)$
	Radial seal gap, liquid or gas	Laminar	$h = 2 (k_f/s) Pr_f^{1/3}$
		Turbulent	$h = 0.0297 (k_f/r)(r/s)^{1/6} Re_\omega^{3/4} Pr_f^{1/3}$
	Concentric cylinders, liquid or gas	Turbulent	$h = \frac{k}{\Delta r} \left[0.015 Re_d^{0.8} Pr_f^{1/3} \left(\frac{r_o}{r_i} \right)^{0.46} + 0.092 Ta_f^{2/3} Pr_f^{1/3} \right]$
	Flat plate, liquid or gas	Laminar	$h = 0.332 (k/X) Re_x^{1/2} Pr_f^{1/3}$
		Turbulent	$h = 0.0288 (k/X) Re_x^{0.8} Pr_f^{1/3}$
Free convection	Horizontal cylinder, liquid or gas	Laminar	$h = 0.53 (k_f/D_o)(Gr_{D,f} Pr_f)^{1/4}$
		Turbulent	$h = 0.13 (k_f/D_o)(Gr_{D,f} Pr_f)^{1/3}$
	Vertical cylinder or plane	Laminar	$h = 0.44 (k_f/X)(Gr_{D,f} Pr_f)^{1/4}$
		Turbulent	$h = 0.13 (k_f/X)(Gr_{D,f} Pr_f)^{1/3}$
	Liquid film cooling, gravity flow	-----	$h = 2C_p (W/L) / \pi D_l$
Radiation	Any surface	-----	$h_r = \frac{q}{A \Delta T} = \frac{\sigma \epsilon_e (1 - \epsilon_s) F_{es} (T_e^3 + T_e^2 T_s + T_e T_s^2 + T_s^3)}{1 - F_{es} F_{se} (1 - \epsilon_e) (1 - \epsilon_s)}$

ture conditions can be added by writing appropriate subroutines and by adding the required statements in subroutine CQN. The CQN statements required can be deduced from the portions labeled for present coefficients. Changes and some limitations are discussed in more detail in appendix B.

The present coefficient equations are based on properties evaluated at the boundary film temperature (average of bulk fluid and surface temperatures). Unless the initial temperature estimates (required as a starting point) are very close to the final temperatures calculated, the input required will have to be changed and the problem rerun at least once to obtain the best results.

CONCLUDING REMARKS

The program, which is written in FORTRAN IV language for an IBM 7094 digital computer, is general and can be applied to a variety of axisymmetric problems. Various convection and radiation boundary conditions which can be used are given in the mathematical formulation. The program listing and flowcharts for steady-state thermal solution of an axisymmetric solid in cylindrical coordinates are given. Computer program application to a nosepiece assembly is given in detail. Additional demonstration of the program is provided in a comparison of the program solution to the exact solution for a finite cylinder. This comparison shows a maximum error of 15 percent when a coarse mesh is used. Thus a partial check on program accuracy is provided.

Lewis Research Center,
National Aeronautics and Space Administration,
Cleveland, Ohio, July 10, 1969,
126-15.

APPENDIX A

COMPUTER PROGRAM

Preparation of Input Data

The recommended first step is the preparation of the element pattern. For the seal analyzed in appendix C, a layout of the seal assembly five times actual size was used. There is no restriction on the numbering sequence except the use of consecutive numbers (i.e., every number from 1 to P), but it is preferable to use an orderly system in order to avoid confusion and to expedite assembling the data required for input. The drawing also includes, for convenience, the radial dimension and mean radius of each element row and the axial dimension of each column.

Adjacent elements should have the same common dimension. Slight variations will not cause appreciable errors if a contact resistance is added to compensate for the increased conduction path length of off-center nonmatching elements.

Also, for convenience, the boundary conditions (pressure, temperature, fluid, and so forth, needed to determine the values of required properties) are included. The materials of the various parts are included in a table (on the drawing if room is available).

The items of data required are listed in the following section on computer input. A compact outline of most items can be obtained from the section Program Symbols and Definitions or from table II. The conduction element matrix (TD1) and boundary coefficient lists (TD2) include input data.

TABLE II. - SUMMARY OF TD2 LISTS FOR SUBROUTINES TO CALCULATE COEFFICIENTS

[Parameters in parentheses are calculated in subroutine. Except for TD2(20) of SN3 and VT2 and TD2(11) of FC1 and FC2, parameters after hA are merely to make writing FORTRAN expression for h easier.]

TD2 word or subscript	Subroutine										
	SN1 (duct flow, liquid)	SN2 (sides of rotors)	SN3 (radial seal gap)	SN4 (concentric cylinders)	SN5 (flat plate)	FC1 (horizontal cylinder)	FC2 (vertical cylinder or plane)	FC3 (liquid film cooling, gravity flow)	RA1 (radiation)	SC1 (specified heat transfer coefficient)	VT1 (varying temperature duct flow, liquid)
1	T _b	T _b	T _b	T _b	T _b	T _b	T _b	T _e	T _b or T _e	T _b	T _b
2	k _f	k _f	k _f	k _f	k _f	k _f	k _f	W/L	f _{es}	k _f	k _f
3	C _{p,f}	C _{p,f}	C _{p,f}	C _{p,f}	C _{p,f}	C _{p,f}	C _{p,f}	C _p	f _{se}	C _{p,f}	C _{p,f}
4	μ _f	μ _f	μ _f	μ _f	μ _f	μ _f	μ _f	D _L	ε _e	μ _f	μ _f
5	W _a	ν _f	ν _f	ν _f	ν _f	ν _f	ν _f	(h)	ε _s	W	ν _f
6	D	r _{av}	r _{av}	r _o	X	D	L	(hA)	(h)	D	r _{av}
7	X	s	s	r _i	V _∞	(Pr _f)	(Pr _f)	-----	(hA)	X	s
8	-----	ω	ω	(Re _x)	(Gr _D)	(Gr _L)	-----	(1 - ε _e)	-----	Annular neighbor conduction number	ω
9	-----	a	a	V _a	(Pr _f)	(h _f)	(h _f)	-----	(1 - ε _s)	Flow neighbor conduction number	a
10	-----	*	----	(Re _v)	(h)	(hA)	(hA)	-----	$\left(\frac{T_e^4 - T_s^4}{T_e - T_s}\right)$	Combining flow indicator	Combining flow indicator
11	-----	(Re _ω)	----	(Pr _f ^{1/3})	(hA)	(Pr _f Gr _D)	(Pr _f Gr _D)	-----	-----	Flow initiation indicator	Flow initiation indicator
12	-----	(Pr _f ^{1/3})	----	(h _f)	-----	(ΔT)	(ΔT)	-----	-----	A _X	Annular neighbor conduction number
13	(Re _w)	(h _f)	----	(hA)	-----	(T _{av})	(T _{av})	-----	-----	(Re _w)	Flow neighbor conduction number
14	(Pr _f)	(hA)	----	(V _R)	-----	(k _f /D)	(k _f /L)	-----	-----	(Pr _f)	W
15	(h _f)	(k _f /r _{av})	(Re _ω)	(V _{tot} ²)	-----	-----	-----	-----	-----	(h _f)	(Re _ω)
16	(hA)	([s/r _{av}] ^{0.1})	(Pr _f ^{1/3})	(V _{tot})	-----	-----	-----	-----	-----	(hA)	(Pr _f ^{1/3})
17	(D/X)	(K)	(Re _c)	(s)	-----	-----	-----	-----	-----	(D/X)	(Re _c)
18	(k _f /D)	-----	(h _f)	-----	-----	-----	-----	-----	-----	(k _f /D)	(h _f)
19	([(D/X)] ^{0.7})	-----	(hA)	-----	-----	-----	-----	-----	-----	([(D/X)] ^{0.7})	(hA)
20	-----	-----	(Heat generation factor)	-----	-----	-----	-----	-----	-----	(Heat generation factor)	-----

*Rotor or stator flag (zero for rotor, nonzero for stator).

Computer Input

The data input of a problem is submitted to the computer on the cards described in this section. Unless specifically stated, no input card may be omitted.

Item 1: Title card (72H)

word 1 columns 1 to 72 Title of problem being run

Item 2: Output control (LO) card (10I6) for obtaining printouts in addition to that listed in the section Computer Output

word 1	columns 1 to 6	A nonzero integer causes printout of the conduction matrix (TD1 table) input
word 2	columns 7 to 12	A nonzero integer causes printout of the boundary conductance matrix ($H(NBPT, J), J=1, 9$)
word 3	columns 13 to 18	A nonzero integer causes printout of the element temperatures for the next to last iteration (unless execution terminated by reaching maximum number of iterations) for comparison with temperatures of last iteration
word 4	columns 19 to 24	Leave blank. This word is set within the program to cause printout of the convergence criterion (Item 5, word 4) and of the temperature change for each element at each N^{th} iteration; N is specified by word 2 of the Run data card (Item 4).
word 5	columns 25 to 30	A nonzero integer causes printout of the boundary condition input matrix (TDA and TD2 lists)
word 6	columns 31 to 36	Not used
word 7	columns 37 to 42	Not used
word 8	columns 43 to 48	A nonzero integer causes the final element temperatures to be punched on cards for use as initial estimates for another run
word 9	columns 49 to 54	A nonzero integer causes thermal expansions to be punched on cards for use in other programs (e.g., a stress analysis)

word 10 columns 55 to 60 A nonzero integer causes printout of element temperatures and heat fluxes after each iteration. Also thermal expansion data (α , T, $\alpha \Delta T$) are printed. This option is meant only for debugging data and should not be included for a standard run.

Item 3: Miscellaneous options (NI) card (5I6)

word 1 columns 1 to 6 Number of cases (designs) to be analyzed. If only one case, this word may be left blank.

No other words now used; leave blank.

Item 4: Run data (RD) card (5F6.0)

word 1 columns 1 to 6 Over-relaxation factor w ($1 \leq w < 2$)

word 2 columns 7 to 12 Reference temperature for thermal expansion ($\alpha \Delta T$)

word 3 columns 13 to 18 The interval N required for word 4 of the LD card (Item 2)

No other words now used.

Item 5: Case data (CD) card (10F6.0)

word 1 columns 1 to 6 Number of elements (400 maximum at present)

word 2 columns 7 to 12 Number of boundary elements (200 maximum at present)

word 3 columns 13 to 18 Maximum number of iterations allowed for a run

word 4 columns 19 to 24 Temperature convergence criterion. The maximum change in temperature of any element from one iteration to the next that is considered an acceptable error.

word 5 columns 25 to 30 Not used

word 6 columns 31 to 36 Starting temperature for varying temperature flow 1 (see varying temperature under boundary condition input (Item 10))

word 7 columns 37 to 42 Starting temperature for varying temperature flow 2

word 8	columns 43 to 48	Not used
word 9	columns 49 to 54	To avoid numerical instability due to low flow rates in the varying temperature calculation, the boundary elements are subdivided. The number of subdivisions is specified between 1 and 100 in this word.
word 10	columns 55 to 60	Not used

Item 6: Thermal conductivity data cards

The thermal conductivity of each material is treated as a power series function of temperature ($k = AT^0 + BT^1 + \dots + NT^m$). Provision is made for curve fitting up to 15 materials. The coefficients required are computed by an auxiliary program (or, of course, by hand) from available data. The degree of fit of a curve is defined as the highest power of temperature appearing in the function. Thus, a linear fit is degree 1; a constant conductivity is degree 0; and so forth.

The auxiliary program is designed to produce fits of all degrees up to 11 from which the best agreement with a set of average values of k is selected as the function to be used. Therefore, words 4 and 5 were included to avoid exceeding the computer capacity when the higher powers of temperature occurred. Later it was somewhat arbitrarily decided to limit the maximum degree of fit to five in view of data scatter due to variation between material lots. The primary reason was to increase the number of materials possible and to save computer storage space.

Card 1 (5F10.0)

word 1	columns 1 to 10	Upper temperature limit of curve fit
word 2	columns 11 to 20	Material code number. Each material must be assigned a number so that the correct properties will be used in the program.
word 3	columns 21 to 30	Degree of fit (0 to 5)
word 4	columns 31 to 40	Thermal conductivity scaling factor. At present, this is 1.
word 5	columns 41 to 50	Temperature scaling factor. At present, this is 1.

Card 2 (6E13.6) - The coefficients of the equation: A in columns 1 to 13, B in columns 14 to 26, and so forth.

Card 3 (blank card) - If less than 15 materials are used, a blank card must be inserted following the last conductivity card in order to terminate the reading of data.

Item 7: Mean coefficient of linear thermal expansion cards

The remarks made about conductivity (see Item 6) also apply to expansion.

Card 1 (5F10.0)

word 1	columns 1 to 10	Upper temperature limit of curve fit
word 2	columns 11 to 20	Material code number
word 3	columns 21 to 30	Degree of fit (0 to 5)
word 4	columns 31 to 40	Thermal expansion scaling factor. At present, this is 1.
word 5	columns 41 to 50	Temperature scaling factor. At present, this is 1.

Card 2 (6E13.6) - The coefficients of the equation as in Item 6.

Card 3 (blank card) - To terminate data read in for less than 15 materials (see Item 6).

Item 8: Conduction matrix data (TD1) card (F4.0, 1X, F7.4, 2F5.3, 1X, 4F4.0, F3.0, 4F7.0) - 1 card per element; element numbers in numerical order

word 1	columns 1 to 4	Element conduction number
word 2	columns 6 to 12	Mean element radius, r_{av} , in.
word 3	columns 13 to 17	Element radial width, Δr , in.
word 4	columns 18 to 22	Element axial length, Δl , in.
word 5	columns 24 to 27	East neighbor conduction number, j_1
word 6	columns 28 to 31	North neighbor conduction number, j_2
word 7	columns 32 to 35	West neighbor conduction number, j_3
word 8	columns 36 to 39	South neighbor conduction number, j_4
word 9	columns 40 to 42	Material code number (see Item 6, word 2)
word 10	columns 43 to 49	East contact resistance, $R_{c_{1,i}}$, (sec)(°F)/Btu
word 11	columns 50 to 56	North contact resistance, $R_{c_{2,i}}$, (sec)(°F)/Btu
word 12	columns 57 to 63	West contact resistance, $R_{c_{3,i}}$, (sec)(°F)/Btu
word 13	columns 64 to 70	South contact resistance, $R_{c_{4,i}}$, (sec)(°F)/Btu

Item 9: Initial temperature cards (16F5.0) - Put 16 initial element temperatures per card.

words 1 columns 1 to 5,
to 16 6 to 10,
 11 to 15,
 and so forth

Initial element temperatures ($^{\circ}$ F) are listed in sequence from 1 to the total number of elements: elements 1 to 16 on the first card, elements 17 to 32 on the second, and so forth.

Item 10: Boundary heat transfer cards

Each boundary element requires an indicator card. Following the indicator card is a set of one or more cards for each boundary condition associated with the element. A partial outline is presented in table II. This sequence is repeated for each boundary element.

Card 1: Boundary indicator card (3I6) - 1 card per element

word 1 columns 1 to 16 Boundary number of the element. In addition to the conduction numbers which are assigned to the elements, each boundary element is given a boundary number. Any convenient order of numbering can be used. This is for convenience in preparing data.

word 2 columns 7 to 12 Conduction number of the boundary element. Most computation is based on the conduction number.

word 3 columns 13 to 18 Boundary heat transfer type code number for first basic type associated with the element. Code numbers are as follows:

- (1) Specified heat flux - the net flux for all faces for which it is specified. If this type is associated with a node, it must appear first; but the other types need not appear in any fixed order.
- (2) Forced convection
- (3) Free convection
- (4) Radiation
- (5) Specified heat transfer coefficient
- (6) Specified temperature - By definition this will be the only condition for an element; the program considers only its effect on adjacent elements.

Card 2: Index card (for each condition: basic type or subtype)

This card has two forms. Form A is used for specified parameters (types 1 and 7) which require no additional cards. Form B (TDA) is used for the remaining types which do require additional cards.

Form A for specified heat flux (I5, E13.6, I6)

word 1	columns 1 to 5	Conduction number of element
word 2	columns 6 to 18	Heat flux, Btu/sec
word 3	columns 19 to 24	A nonzero integer if other types or subtypes associated with the node follow; blank (or 0) if no types or subtypes follow.

Form A for specified temperature (I5, 1X, F6.0)

word 1	columns 1 to 5	Conduction number of element
word 2	columns 7 to 12	Temperature of element, °F

Form B (6F6.0, F12.0) - These (TDA) cards are the same for all types using them.

word 1	columns 1 to 6	Conduction number of element
word 2	columns 7 to 12	Heat transfer type (2 to 6)
word 3	columns 13 to 18	Heat transfer subtype code number. (For additions or substitutions see limitations and scope.)

Subtype code numbers for type 2 (forced convection) are as follows:

- (1) Duct flow, liquid - for explanation see headings under additional cards
- (2) Sides of rotors
- (3) Radial seal gap
- (4) Concentric cylinders
- (5) Flat plate
- (6) to (9) for additional subtypes

Subtype code numbers for type 3 (free convection) are as follows:

- (1) Horizontal cylinder
- (2) Vertical cylinder or plane
- (3) Liquid film cooling, gravity flow
- (4) to (8) for additional subtypes

Subtype code numbers for type 6 (varying temperature forced convection) are as follows:

- (1) Duct flow, liquid
- (2) Radial seal gap
- (3) to (4) for additional subtypes

Types 4 and 5, at present, have no subtypes; so word 3 = 0.

word 4	columns 19 to 24	Nonzero number if other types or subtypes follow
word 5	columns 25 to 30	Number of items to be read from the remaining cards for this condition
word 6	columns 31 to 36	Area indicator code number specifies to which face of the element the condition applies; these numbers are as follows: <ul style="list-style-type: none">(1) East face(2) North face(3) West face(4) South face(5) Specified area - used for special cases such as a small duct passing through an element or a boundary at an appreciably nonparallel or nonnormal angle to the axis. Since conductive resistance is assumed to be negligible compared with boundary film resistance, the problem of location does not occur.
word 7	columns 37 to 48	If a specified area (code number 5 in word 6) is used, the value in square feet is placed here; otherwise, this word is left blank.

For types 2 to 6, the following additional cards are needed as shown under types 4 and 5 and the subtypes of types 2, 3, and 6. Card 1 is the indicator card described previously. Card 2 is the TDA card for the type or subtype. The properties are evaluated at the temperature indicated by the equations in table I.

Steady-state forced convection (type 2):

Subtype 1 - Duct flow, liquid

Card 3 (7F11.0)

word 1 columns 1 to 11 Fluid bulk temperature, $^{\circ}\text{F}$

word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})(^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})(^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$
word 5	columns 45 to 55	Mass flow per square foot of cross section, $\text{lbm}/(\text{ft}^2)(\text{sec})$
word 6	columns 56 to 66	Hydraulic diameter, $4A_x/P_w$, ft
word 7	columns 67 to 77	Flow length (distance from start of duct to center of element), ft

Subtype 2 - Sides of rotors (see Use of Local Coefficients in appendix D)

Card 3 (7F11.0)

word 1	columns 1 to 11	Fluid bulk temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})(^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})(^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$
word 5	columns 45 to 55	Kinematic viscosity, ft^2/sec
word 6	columns 56 to 66	Average radius of element, ft
word 7	columns 67 to 77	Gap between rotor and stator, ft

Card 4 (3F11.0)

word 1	columns 1 to 11	Rotor angular velocity, rad/sec
word 2	columns 12 to 22	Outer radius of rotor or stator, ft
word 3	columns 23 to 33	Rotor or stator flag (zero for rotor, nonzero for stator)

Subtype 3 - Radial seal gap

Card 3 (7F11.0)

word 1	columns 1 to 11	Fluid bulk temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})(^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})(^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$

word 5	columns 45 to 55	Kinematic viscosity, ft^2/sec
word 6	columns 56 to 66	Average radius of element, ft
word 7	columns 67 to 77	Gap between rotor and stator, ft

Card 4 (2F11.0)

word 1	columns 1 to 11	Rotor angular velocity, rad/sec
word 2	columns 12 to 22	Outer radius of rotor or stator, ft

Subtype 4 - Concentric cylinders (inner cylinder rotating)

Card 3 (7F11.0)

word 1	columns 1 to 11	Fluid bulk temperature, ${}^{\circ}\text{F}$
word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})({}^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})({}^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$
word 5	columns 45 to 55	Kinematic viscosity, ft^2/sec
word 6	columns 56 to 66	Outer radius of annulus between cylinders, ft
word 7	columns 67 to 77	Inner radius of annulus, ft

Card 4 (2F11.0)

word 1	columns 1 to 11	Rotational velocity of inner cylinder, rad/sec
word 2	columns 12 to 22	Axial flow velocity, ft/sec

Subtype 5 - Flat plate

Card 3 (7F11.0)

word 1	columns 1 to 11	Fluid bulk temperature, ${}^{\circ}\text{F}$
word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})({}^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})({}^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$
word 5	columns 45 to 55	Kinematic viscosity, ft^2/sec
word 6	columns 56 to 66	Flow length (distance from start of plate to center of element), ft
word 7	columns 67 to 77	Velocity of bulk fluid, ft/sec

Free convection (type 3):

Subtype 1 (horizontal cylinder) or 2 (vertical cylinder or plane), gas - identical except for the characteristic length used

Card 3 (6F11.0)

word 1	columns 1 to 11	Fluid bulk temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})(^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})(^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$
word 5	columns 45 to 55	Kinematic viscosity, ft^2/sec
word 6	columns 56 to 66	Subtype 1: hydraulic diameter, ft Subtype 2: flow length (distance from start of flow to top of surface of which element is a part), ft

Subtype 3 - Liquid film cooling, gravity flow

Card 3 (4F11.0)

word 1	columns 1 to 11	Fluid film temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	Mass flow per unit length (at a right angle to flow direction), $\text{lbm}/(\text{ft})(\text{sec})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})(^{\circ}\text{F})$
word 4	columns 34 to 44	Flow length (distance from point where flow starts to where it leaves surface (e.g., one-half circumference of horizontal cylinder)), ft

Graybody radiation (type 4):

Card 3 (4F11.0)

word 1	columns 1 to 11	Environmental temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	View factor, environment to surface
word 3	columns 23 to 33	View factor, surface to environment
word 4	columns 34 to 44	Emissivity of environment
word 5	columns 45 to 55	Emissivity of surface

Specified heat transfer coefficient (type 5):

Card 3 (2F11.0)

word 1	columns 1 to 11	Fluid bulk (or environmental) temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	Heat transfer coefficient, $\text{Btu}/(\text{ft}^2)(\text{sec})(^{\circ}\text{F})$

Varying temperature forced convection (type 6):

Subtype 1 - Varying temperature duct flow, liquid

Card 3 (7F11.0)

word 1	columns 1 to 11	Fluid bulk temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})(^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})(^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$
word 5	columns 45 to 55	Mass flow per square foot of cross section, $\text{lbm}/(\text{ft}^2)(\text{sec})$
word 6	columns 56 to 66	Hydraulic diameter, $4A_x/P_w$, ft
word 7	columns 67 to 77	Flow length (distance from start of duct to center of element), ft

Card 4 (4F11.0)

word 1	columns 1 to 11	Conduction number of annular neighbor (element on other boundary of flow if flow is between two elements). If none, leave blank.
word 2	columns 12 to 22	Conduction number of flow neighbor (element up- stream of element under consideration). If this is the first element along the flow, leave blank.
word 3	columns 23 to 33	Combined flow indicator (see remarks at end of this subtype)
word 4	columns 34 to 44	Flow initiation indicator (see remarks at end of this subtype)
word 5	columns 45 to 55	Cross section of duct, ft^2

There is provision in the program for varying temperature flows of two starting temperatures. Any number of varying temperature flows can be handled subject to the fol-

lowing additional restrictions. The program will handle only one such boundary condition per element. The number of elements with varying temperature flows cannot exceed half the number of boundary elements (95) at present. There can be no more than five combined flows (explained later).

The flow initiation indicator distinguishes the two starting temperatures. If 1 is used, the starting temperature is word 1, Card 2 of Item 5 (Case data). If 2 is used, the starting temperature is word 2, Card 2 of Item 5.

If two flows (limit of program) combine at a boundary element to form a new flow, this element is a combined flow element. For a combined flow element, the flow initiation indicator must be zero. Five such combinations are permitted by the program. An additional card is then required.

Card 5 (2I6) - only for combined flow elements

word 1	columns 1 to 6	Conduction number of one upstream neighbor element
word 2	columns 7 to 12	Conduction number of other upstream neighbor element

Subtypes - Varying temperature radial seal gap

Card 1 (7F11.0)

word 1	columns 1 to 11	Fluid bulk temperature, $^{\circ}\text{F}$
word 2	columns 12 to 22	Thermal conductivity, $\text{Btu}/(\text{ft})(\text{sec})(^{\circ}\text{F})$
word 3	columns 23 to 33	Specific heat, $\text{Btu}/(\text{lbm})(^{\circ}\text{F})$
word 4	columns 34 to 44	Absolute viscosity, $\text{lbm}/(\text{ft})(\text{sec})$
word 5	columns 45 to 55	Kinematic viscosity, ft^2/sec
word 6	columns 56 to 66	Average radius of element, ft
word 7	columns 67 to 77	Gap between rotor and stator, ft

Card 2 (7F11.0)

word 1	columns 1 to 11	Rotor angular velocity, rad/sec
word 2	columns 12 to 22	Outer radius of rotor, ft
word 3	columns 23 to 33	Combined flow indicator
word 4	columns 34 to 44	Flow initiation indicator
word 5	columns 45 to 55	Annular neighbor conduction number

word 6	columns 56 to 66	Flow neighbor conduction number
word 7	columns 67 to 77	Mass flow, lbm/sec

Card 5 (2I6) - only for combined flow elements

word 1	columns 1 to 6	Conduction number of one upstream neighbor element
word 2	columns 7 to 12	Conduction number of other upstream neighbor element

Computer Output

Standard output of results. - The standard output of the program is obtained with all list options (Item 2 of Computer Input) set at zero with the possible exception of the punch options (words 8 and 9). This output is as follows:

- Item 1: Problem title
- Item 2: Printout options (see input Item 2)
- Item 3: Miscellaneous options (see input Item 3)
- Item 4: Run data (see input Item 4)
- Item 5: Case data (see input Item 5)
- Item 6: Thermal conductivity curve fit coefficients for each material
- Item 7: Thermal expansion curve fit coefficients for each material
- Item 8: Element starting temperature estimates
- Item 9: Varying temperature boundary element dimensionless coefficient, hA/WC_p
- Item 10: Varying temperature boundary element fluid internal heat generation
- Item 11: Conduction number and preceding element conduction numbers for each combined flow element
- Item 12: Conduction number, varying temperature number, and flow code for varying temperature boundary elements
- Item 13: Element steady-state temperatures
- Item 14: Boundary element forced convection, free convection, radiation, and varying temperature convection conductances
- Item 15: Varying temperature boundary condition fluid temperatures
- Item 16: Element thermal conductivities
- Item 17: Element heat fluxes to neighbor elements
- Item 18: Element conductances to neighbor elements
- Item 19: Element boundary conductance sums and boundary heat flux sums
- Item 20: Element free thermal expansion, $\alpha \Delta T$

An illustration of the output can be found in the listing for the sample problem in appendix C.

Program error messages. - The program includes checks of some of the input to ensure correct relations. First, the conductivity (TD1) cards are checked for numerical order of conduction numbers. Once this has been achieved, a check is made for neighbor agreement. For example, if element 10 has element 11 listed as east neighbor, element 11 must have element 10 as west neighbor, assuming this is the correct relation. When the neighbor agreement is complete, a check is made of boundary index cards to ensure numerical order of boundary numbers. Then a check is made to see that the conduction number(s) on the element boundary index card(s) agree with the conduction number on the indicator card. Also there is a check for agreement of the boundary number corresponding to an element conduction number with the conduction number corresponding to the element boundary number.

Program Symbols and Definitions

AFN(NTF)	conduction number of varying temperature element annular neighbor
ALPHA(15, 11)	thermal expansion curve fit matrix (input Item 6)
CE(NJPTS, 4)	neighbor conductance matrix
GFN(NTF)	conduction number of varying temperature element flow neighbor
H(NBPTS, 9)	boundary conductance matrix
JBNT(JBPT)	boundary number of element JBPT
JBP	conduction number of boundary element (in card check)
JBPT	conduction number of boundary element, NBND(NBP)
JNTF(JVPT)	varying temperature number of element JVPT
JPT	conduction number of element
JVPT	conduction number of varying temperature element, NODE(NTF)
MATL(15, 11)	thermal conductivity curve fit matrix (input Item 5)
NAT(NDR)	conduction number of one adjacent element upstream of NDR
NBDIM	maximum number of boundary elements accepted by program
NBND(NBP)	conduction number of boundary element NBP
NBP	boundary number of boundary element
NBPTS	actual number of boundary elements

NBR(NTR)	flow number (input Item 10, Card 4, word 3) of varying temperature element
NBT(NDR)	conduction number of other adjacent element upstream of NDR
NDIM	maximum number of conduction elements accepted by program
NDR	combination number of combined flow varying temperature element
NITS	maximum number of iterations allowed for analysis
NJPTS	actual number of conduction elements
NM(NDR)	conduction number of combined flow element NDR
NODE(NTF)	conduction number of varying temperature element NTF
NTF	varying temperature number of varying temperature boundary element
NTR	noncombining flow number of varying temperature element
NVDIM	maximum number of varying temperature elements accepted
QF(NTF)	fluid shear heat generation at varying temperature element NTF
Q(JBPT)	sum of boundary heat fluxes of conduction element JBPT
SUMH(NBPT)	sum of boundary conductances of boundary element NBPT
SUMT(NBPT)	sum of boundary heat fluxes of boundary element NBPT
TBND(NTF)	fluid temperature at varying temperature boundary element
TCF(NTF)	dimensionless coefficient of varying temperature element, kA/WC_p
TDA(7)	index card (input Item 10, Card 2) list
TD1(NJPTS, 19)	conduction data matrix
TD2(20)	properties cards (input Item 10, Card(s) 3 and those following) list
THEXP(JPT)	element thermal expansion, $\alpha \Delta T$
T(JPT)	initial temperature estimate for element JPT
TS(INC)	fluid temperature calculation by subdivision of boundary element

Conductance matrix CE(NJPTS, 4). - The symbols for conductance matrix CE(NJPTS, 4) are as follows:

CE(JPT, 1)	conductance between conduction element JPT and east neighbor
CE(JPT, 2)	conductance between conduction element JPT and north neighbor
CE(JPT, 3)	conductance between conduction element JPT and west neighbor
CE(JPT, 4)	conductance between conduction element JPT and south neighbor

Boundary conductance matrix H(NBPTS, 9). - The symbols for boundary conductance matrix H(NBPTS, 9) are as follows:

H(NBPT, 1)	specified heat flux
H(NBPT, 2)	sum of forced convection (including specific coefficient) conductances
H(NBPT, 3)	sum of forced convection conductance \times fluid temperature
H(NBPT, 4)	sum of free convection conductances
H(NBPT, 5)	sum of free convection conductance \times fluid temperature
H(NBPT, 6)	sum of radiation "conductances"
H(NBPT, 7)	sum of radiation "conductance" \times environmental temperature
H(NBPT, 8)	sum of varying temperature conductances
H(NBPT, 9)	sum of varying temperature conductance \times fluid temperature

Conduction data matrix TD1(NJPTS, 19). - The symbols for conduction data matrix TD1(NJPTS, 19) are as follows:

TD1(JPT, 1)	element conduction number
TD1(JPT, 2)	mean element radius
TD1(JPT, 3)	element radial width, Δr
TD1(JPT, 4)	element axial length, Δl
TD1(JPT, 5)	east neighbor conduction number, j_1
TD1(JPT, 6)	north neighbor conduction number, j_2
TD1(JPT, 7)	west neighbor conduction number, j_3
TD1(JPT, 8)	south neighbor conduction number, j_4
TD1(JPT, 9)	material code number
TD1(JPT, 10)	east contact resistance, $R_{c_{1i}}$
TD1(JPT, 11)	north contact resistance, $R_{c_{2i}}$
TD1(JPT, 12)	west contact resistance, $R_{c_{3i}}$
TD1(JPT, 13)	south contact resistance, $R_{c_{4i}}$
TD1(JPT, 14)	east and west boundary areas (added during run)
TD1(JPT, 15)	north boundary area (added during run)
TD1(JPT, 16)	south boundary area (added during run)
TD1(JPT, 17)	boundary condition type code number (added during run)

TD1(JPT,18) thermal conductivity (added during run)

TD1(JPT,19) element temperature (added during run)

TD2 list for subroutine SN1, type 2 (forced convection), subtype 1 (duct flow, liquid). - The TD2 list is as follows:

- TD2(1) fluid bulk temperature, T_b
- TD2(2) boundary film thermal conductivity, k_f
- TD2(3) boundary film specific heat, $C_{p,f}$
- TD2(4) boundary film absolute viscosity, μ_f
- TD2(5) fluid mass flow per square foot of cross section, W_a
- TD2(6) duct hydraulic diameter, D
- TD2(7) length from start of flow to center of element, X
- TD2(8) not used in order to obtain compatibility with VT1
- TD2(9) not used in order to obtain compatibility with VT1
- TD2(10) not used in order to obtain compatibility with VT1
- TD2(11) not used in order to obtain compatibility with VT1
- TD2(12) not used in order to obtain compatibility with VT1
- TD2(13) Reynolds number (calculated in subroutine), Re_w
- TD2(14) Prandtl number (calculated in subroutine), Pr_f
- TD2(15) heat transfer coefficient (calculated in subroutine), h_f
- TD2(16) conductance across boundary film (calculated in subroutine), hA
- TD2(17) hydraulic diameter/flow length (calculated in subroutine), D/X
- TD2(18) conductivity/hydraulic diameter (calculated in subroutine), k_f/D
- TD2(19) 0.7 power of TD2(16) (calculated in subroutine), $(D/X)^{0.7}$

TD2 list for subroutine SN2, type 2 (forced convection), subtype 2 (sides of rotors). - The TD2 list is as follows:

- TD2(1) fluid bulk temperature, T_b
- TD2(2) boundary film thermal conductivity, k_f
- TD2(3) boundary film specific heat, $C_{p,f}$
- TD2(4) boundary film absolute viscosity, μ_f
- TD2(5) boundary film kinematic viscosity, ν_f

TD2(6)	average radius of element, r_{av}
TD2(7)	clearance between rotor and stator, s
TD2(8)	rotor angular velocity, ω
TD2(9)	outer radius of rotor, a
TD2(10)	rotor or stator flag (zero for rotor, nonzero for stator)
TD2(11)	Reynolds number (calculated in subroutine), Re_ω
TD2(12)	cube root of Prandtl number (calculated in subroutine), $Pr_f^{1/3}$
TD2(13)	heat transfer coefficient (calculated in subroutine), h_f
TD2(14)	conductance across boundary film (calculated in subroutine), hA
TD2(15)	conductivity/average radius (calculated in subroutine), k_f/r_{av}
TD2(16)	0.1 power of clearance/average radius (calculated in subroutine), $(s/r_{av})^{0.1}$
TD2(17)	fluid angular velocity/rotor angular velocity (calculated in subroutine), K

TD2 list for subroutine SN3, type 2 (forced convection), subtype 3 (radial seal gap). -
The TD2 list is as follows:

TD2(1)	fluid bulk temperature, T_b
TD2(2)	boundary film thermal conductivity, k_f
TD2(3)	boundary film specific heat, $C_{p,f}$
TD2(4)	boundary film absolute viscosity, μ_f
TD2(5)	boundary film kinematic viscosity, ν_f
TD2(6)	average radius of element, r_{av}
TD2(7)	clearance between rotor and stator, s
TD2(8)	rotor angular velocity, ω
TD2(9)	outer radius of rotor, a
TD2(10)	not used to obtain compatibility with VT2
TD2(11)	not used to obtain compatibility with VT2
TD2(12)	not used to obtain compatibility with VT2
TD2(13)	not used to obtain compatibility with VT2
TD2(14)	not used to obtain compatibility with VT2
TD2(15)	Reynolds number (calculated in subroutine), Re_ω

TD2(16)	cube root of Prandtl number (calculated in subroutine), $\text{Pr}_f^{1/3}$
TD2(17)	critical Reynolds number (calculated in subroutine), Re_c
TD2(18)	heat transfer coefficient (calculated in subroutine), h_f
TD2(19)	conductance from center of seal gap to surface (calculated in subroutine), hA
TD2(20)	heat generation factor (calculated in subroutine)

TD2 list for subroutine SN4, type 2 (forced convection), subtype 4 (concentric cylinders). - The TD2 list is as follows:

TD2(1)	fluid bulk temperature, T_b
TD2(2)	boundary film thermal conductivity, k_f
TD2(3)	boundary film specific heat, $C_{p,f}$
TD2(4)	boundary film absolute viscosity, μ_f
TD2(5)	boundary film kinematic viscosity, ν_f
TD2(6)	outer radius of annulus between cylinders, r_o
TD2(7)	inner radius of annulus between cylinders, r_i
TD2(8)	angular velocity of inner rotating cylinder, ω
TD2(9)	axial flow velocity, V_a
TD2(10)	Reynolds number (calculated in subroutine), Re_v
TD2(11)	cube root of Prandtl number (calculated in subroutine), $\text{Pr}_f^{1/3}$
TD2(12)	heat transfer coefficient (calculated in subroutine), h_f
TD2(13)	conductance across boundary film (calculated in subroutine), hA
TD2(14)	linear velocity of inner cylinder (calculated in subroutine), V_R
TD2(15)	square of total fluid velocity (calculated in subroutine), V_{tot}^2
TD2(16)	total fluid velocity (calculated in subroutine), V_{tot}
TD2(17)	annular clearance (calculated in subroutine), s

TD2 list for subroutine SN5, type 2 (forced convection), subtype 5 (flat plate). - The TD2 list is as follows:

TD2(1)	fluid bulk temperature, T_b
TD2(2)	boundary film thermal conductivity, k_f
TD2(3)	boundary film specific heat, $C_{p,f}$
TD2(4)	boundary film absolute viscosity, μ_f

TD2(5)	boundary film kinematic viscosity, ν_f
TD2(6)	length from start of flow to center of element, X
TD2(7)	bulk fluid velocity, V_∞
TD2(8)	Reynolds number (calculated in subroutine), Re_x
TD2(9)	Prandtl number (calculated in subroutine), Pr_f
TD2(10)	heat transfer coefficient (calculated in subroutine), h
TD2(11)	conductance across boundary film (calculated in subroutine), hA

TD2 list for subroutine FC1, type 3 (free convection), subtype 1 (horizontal cylinder). - The TD2 list is as follows:

TD2(1)	fluid bulk temperature, T_b
TD2(2)	boundary film thermal conductivity, k_f
TD2(3)	boundary film specific heat, $C_{p,f}$
TD2(4)	boundary film absolute viscosity, μ_f
TD2(5)	boundary film kinematic viscosity, ν_f
TD2(6)	diameter of cylinder, D
TD2(7)	Prandtl number (calculated in subroutine), Pr_f
TD2(8)	Grashof number (calculated in subroutine), Gr_D
TD2(9)	heat transfer coefficient (calculated in subroutine), h_f
TD2(10)	conductance across boundary film (calculated in subroutine), hA
TD2(11)	Prandtl number \times Grashof number (calculated in subroutine), $Pr_f Gr_D$
TD2(12)	fluid to surface temperature difference (calculated in subroutine), ΔT
TD2(13)	average (or film) temperature (calculated in subroutine), T_{av}
TD2(14)	conductivity/cylinder outside diameter (calculated in subroutine), k_f/D

TD2 list for subroutine FC2, type 3 (free convection), subtype 2 (vertical cylinder or plane). - The TD2 list is as follows:

TD2(1)	fluid bulk temperature, T_b
TD2(2)	boundary film thermal conductivity, k_f
TD2(3)	boundary film specific heat, $C_{p,f}$
TD2(4)	boundary film absolute viscosity, μ_f
TD2(5)	boundary film kinematic viscosity, ν_f

TD2(6)	total height of surface, L
TD2(7)	Prandtl number (calculated in subroutine), Pr_f
TD2(8)	Grashof number (calculated in subroutine), Gr_L
TD2(9)	heat transfer coefficient (calculated in subroutine), h_f
TD2(10)	conductance across boundary film (calculated in subroutine), hA
TD2(11)	Prandtl number \times Grashof number (calculated in subroutine), $Pr_f Gr_D$
TD2(12)	fluid to surface temperature difference (calculated in subroutine), ΔT
TD2(13)	average temperature (calculated in subroutine), T_{av}
TD2(14)	conductivity/surface height (calculated in subroutine), k_f/L

TD2 list for subroutine FC3, type 3 (free convection), subtype 3 (liquid film cooling, gravity flow). - The TD2 list is as follows:

TD2(1)	fluid bulk temperature, T_b
TD2(2)	mass flow of liquid per unit length normal to flow, W/L
TD2(3)	fluid specific heat, C_p
TD2(4)	flow length (e.g., one-half circumference of horizontal cylinder), D_L
TD2(5)	heat transfer coefficient (calculated in subroutine), h
TD2(6)	conductance from surface to liquid (calculated in subroutine), hA

TD2 list for subroutine RA1, type 4 (radiation). - The TD2 list is as follows:

TD2(1)	environmental temperature, T_e
TD2(2)	view factor from environment to element surface, f_{es}
TD2(3)	view factor from element surface to environment, f_{se}
TD2(4)	emissivity of environment, ϵ_e
TD2(5)	emissivity of element surface, ϵ_s
TD2(6)	radiation coefficient (calculated in subroutine), h
TD2(7)	"conductance" from element surface to environment (calculated in subroutine), hA
TD2(8)	reflectivity of environment (calculated in subroutine), $1 - \epsilon_e$
TD2(9)	reflectivity of element surface (calculated in subroutine), $1 - \epsilon_s$
TD2(10)	difference between fourth powers of temperatures/temperature difference (calculated in subroutine), $(T_e^4 - T_s^4)/(T_e - T_s)$

TD2 list for subroutine SC1, type 5 (specified heat transfer coefficient). - The TD2 list is as follows:

- TD2(1) fluid bulk (or environmental) temperature, T_b (or T_e)
- TD2(2) specified heat transfer coefficient, h
- TD2(3) conductance between surface and bulk fluid (calculated in main program), hA

TD2 list for subroutine VT1, type 6 (varying temperature forced convection), sub-type 1 (duct flow, liquid). - The TD2 list is as follows:

- TD2(1) fluid bulk temperature, T_b
- TD2(2) boundary film thermal conductivity, k_f
- TD2(3) boundary film specific heat, $C_{p,f}$
- TD2(4) boundary film absolute viscosity, μ_f
- TD2(5) fluid mass flow per square foot of cross section, W_a
- TD2(6) duct hydraulic diameter, D
- TD2(7) length from start of flow to center of element, X
- TD2(8) annular neighbor conduction number
- TD2(9) flow neighbor conduction number
- TD2(10) combining flow indicator code number
- TD2(11) flow initiation indicator code number (must be zero for combined flow element)
- TD2(12) duct cross section, A_x
- TD2(13) Reynolds number (calculated in subroutine), Re_w
- TD2(14) Prandtl number (calculated in subroutine), Pr_f
- TD2(15) heat transfer coefficient (calculated in subroutine), h_f
- TD2(16) conductance across boundary film (calculated in subroutine), hA
- TD2(17) hydraulic diameter/flow length (calculated in subroutine), D/X
- TD2(18) conductivity/hydraulic diameter (calculated in subroutine), k_f/D
- TD2(19) 0.7 power of TD2(16) (calculated in subroutine), $(D/X)^{0.7}$

TD2 list for subroutine VT2, type 6 (varying temperature forced convection), sub-type 2 (radial seal gap). - The TD2 list is as follows:

- TD2(1) fluid bulk temperature, T_b
- TD2(2) boundary film thermal conductivity, k_f

TD2(3)	boundary film specific heat, $C_{p,f}$
TD2(4)	boundary film absolute viscosity, μ_f
TD2(5)	boundary film kinematic viscosity, ν_f
TD2(6)	average radius of element, r_{av}
TD2(7)	clearance between rotor and stator, s
TD2(8)	rotor angular velocity, ω
TD2(9)	outer radius of rotor, a
TD2(10)	combining flow indicator code number
TD2(11)	flow initiation indicator code number (must be zero for combined flow element)
TD2(12)	annular neighbor conduction number
TD2(13)	flow neighbor conduction number
TD2(14)	fluid mass flow rate, W
TD2(15)	Reynolds number (calculated in subroutine), Re_ω
TD2(16)	cube root of Prandtl number (calculated in subroutine), $Pr_f^{1/3}$
TD2(17)	critical Reynolds number (calculated in subroutine), Re_c
TD2(18)	heat transfer coefficient (calculated in subroutine), h_f
TD2(19)	conductance from center of seal gap to surface (calculated in subroutine), hA
TD2(20)	heat generation factor (calculated in subroutine)

Flow Charts and Program Listing

The flow charts for the main routine (SEAL2) and subroutines CQN and QT are presented in figures 8, 9, and 10. A listing of the program is as follows:

\$IBFTC SEAL 2

C STEADY STATE HEAT TRANSFER ANALYSIS OF AXISYMMETRIC SYSTEMS TO
C INCLUDE VARYING FLUID TEMPERATURES ALONG BOUNDARIES APPLIED TO
C ADVANCED AIR BREATHING ENGINE SEAL DESIGN
C
DIMENSION TD1(400,19),T(400),CE(400,4),Q(400),THEXP(400),TD2(20)
DIMENSION H(200,9),SUMH(200),SUMT(200),NBND(200),TBND(95)
DIMENSION LD(10),NI(5),RD(5),CD(10),TDA(7),MATL(15,11),NODE(95)
DIMENSION ALPHA(15,11),JNTF(400)
COMMON/BLK1/J3NT(400),KAN(200),NTF,NDR,NTR,QF(95),NQR
COMMON/B_K2/TCF(95),GPN(95),AFN(95),NBR(95),VM(5),NAT(5),NBT(5)
REAL MATL
C
101 FORMAT(1H1)
102 FORMAT(F4.0,1X,F7.4,2F5.3,1X,4F4.0,F3.0,4F7.0)
103 FORMAT(1H0,10X,43HCONDUCTION (TD1) CARD ORDER ERROR, CARD NO.,I3,2
2X,5HWRONG)
104 FORMAT(1H0,10X,23HNABOR ERROR FOR ELEMENT,I4,3X,6HAND/OR,I4)
105 FORMAT(1H0,45X,30HCONDUCTION ELEMENT TABLE (TD1)//(5X,I4,2X,7(2X,I
22,1H,,1PE11.4)/10X,6(2X,I2,1H,,1PE11.4)//))
106 FORMAT(16F5.0)
107 FORMAT(1H1,50X,29HELEMENT STARTING TEMPERATJRES//)
108 FORMAT(10(2X,I3,1X,F6.1))
109 FORMAT(25X,74HBOUNDARY COEFFICIENT MATRIX -(H*A)BTU/F.SEC AND (H*A
2*T-B) JR W*C-P BTU/SEC//1X,11HBNDRY COND.,2X,10HFIXED FLJK,6X,17HF
3)RCED CONVECTION,10X,15HFREE CONVECTION,14X,9HRADIATION,12X,19HVAR
4.TEMP.CONVECTION/1X,11HELEM. ELEM.,6X,1-HW,11X,3HH*A,3X,7HH*A*T-B,8
5X,3HH*A,8X,7HH*A*T-B,8X,3HH*A,8X,7HH*A*T-E,8X,3HH*A,8X,5H*A-C-P//(1
6X,2(I4,1X),1X,9(1X,E12.5)))
110 FORMAT(1H0,30X,58HVAR.TEMP.CONVECTION DIMENSIONLESS COEFFICIENTS (1
2H*A/W*C-P)//(6(1X,2I4,1H,,1PE11.4)))
111 FORMAT(1H0,45X,36HFLUID SHEAR HEAT GENERATION, BTJ/SEC//(6(1X,2I4,
21H,,1PE11.4)))
112 FORMAT(1H0,2X,10HDATA TIME=,F7.4,2X,7HMINUTES)
113 FORMAT(1H1,20X,61HTEMPERATURES (F) AND HEAT FLUXES (BTJ/SEC) FOR E
2ACH ITERATION)
114 FORMAT(3(4X,I3,1H,,1PE14.7,2X,1PE14.7))
115 FORMAT(1H1,30X,32HCONVERGENCE CRITERIA, ITERATION=,I4//23X,8HCOND.
2NJ.,6X,9HNEW TEMP.,10X,9HOLD TEMP.,9X,10HDIFFERENCE,8X,9HMAX.DIFF.
3//))
116 FORMAT(1H0,2X,42HCONVERGENCE CRITERION NOT MET, ITERATIONS=,I6)
117 FORMAT(1H0,2X,43HCONVERGENCE CRITERION ACHEIVED, ITERATIONS=,I6)
118 FORMAT(1H1,20X,56HELEMENT(AT CENTER) TEMPERATJRES (DEGREES F), ITE
2RATIONS=,I6//))
119 FORMAT(6(2X,I4,1H,,1PE14.7))
120 FORMAT(1H1,9X,102HELEMENT FORCED CONVECTION, FREE CONVECT., RADIAT
2ION AND VAR.TEMP.CONVECT. CONDUCTANCES(H*A) BTU/HR.F//))
121 FORMAT(16X,2I6,4E19.7)
122 FORMAT(1H1,45X,38HVAR.TEMP.CONVECTION BOJNDARY TEMPS.(F)//(6(1X,2I
24,1H,,1PE11.4)))
123 FORMAT(1H1,42X,43HELEMENT THERMAL CONDUCTIVITIES BTJ/HR.FT.F//))

```

124 FORMAT(3X,35HELEMENT ENWS CONDUCTION HEAT FLJXES,2X,I3,4(2X,E14.7)
2,2X,6HBTU/HR)
125 FORMAT(15X,45HELEMENT ENWS CONDUCTANCES TO NABORS(BTJ/HR.F)//(10X,
2I4,4(2X,E14.7)))
126 FORMAT(I10,10X,104HELEMENT BOUNDARY NO, CONDCTION NO, BNDRY CONDJ
2CTANCE(H*A) SUM(BTU/HR.F) AND BNDRY HEAT FLUX SUM(BTU/HR)//(3(3X,2
3I4,2X,E14.7,2X,E14.7)))
127 FORMAT(IH1,40X,43HELEMENT FREE THERMAL EXPANSION,ALPHA*(T-T0)//)
128 FORMAT(6E13.6)

C
C      CALL TIME 1 (START)
C
C      READ RUN PARAMETERS
60 DO 1 J=1,10
     LD(J)=0
1  CD(J)=0.
     DO 2 J=1,5
     NI(J)=0
2  RD(J)=0.
     DO 3 J=1,15
     DO 3 K=1,11
     MATL(J,K)=0.
3  ALPHA(J,K)=0.
     NK=0
     CALL CDA(LD,NI,RD,CD,MATL,ALPHA)
     IF (NK.NE.0) GO TO 99
C
     NDIM=400
     NBDIM=200
     NVDIM=95
     NJPTS=CD(1)
     NBPTS=CD(2)
     VITS=CD(3)
     NK=0
C
C      ZERO COMMON STURAGE
     DO 5 JPT=1,NJPTS
     T(JPT)=0.0
     Q(JPT)=0.0
     JBNT(JPT)=0
     JNTF(JPT)=0
     THEXP(JPT)=0.0
     DO 4 J=1,4
4   CE(JPT,J)=0.0
     DO 5 J=1,19
5   TD1(JPT,J)=0.0
C
     DO 6 NBPT=1,NBPTS
     NBND(NBPT)=0
     SUMH(NBPT)=0.0
     SUMT(NBPT)=0.0
     DO 6 J=1,9
6   H(NBPT,J)=0.0
C
     DO 7 K=1,NVDIM

```

```

QF(K)=0.0
TCF(K)=0.0
GFN(K)=0.0
AFN(K)=0.0
NBR(K)=0
NODE(K)=0
TBND(K)=0.0
C
DO 8 K=1,5
NM(K)=0
NAT(K)=0
8 NPT(K)=0
C
C READ ELEMENT GEOMETRY DATA, CHECK CARD ORDER
DO 10 JPT=1,NJPTS
READ(5,102) (TD1(JPT,J),J=1,13)
C
NPC=TD1(JPT,1)
IF (JPT-NPC) 9,10,9
9 WRITE(6,103) JPT
NK=1
10 CONTINUE
IF (NK.NE.0) GO TO 99
C
C CHECK FOR CONDUCTANCE NABOR ERRORS
NK=0
DO 15 JPT=1,NJPTS
DO 15 J=5,8
N=TD1(JPT,J)
TF (N) 14,15,11
11 IF (JPT-N) 12,14,12
12 RJPT=JPT
JN=J-4
GO TO (13,213,313,413),JN
13 TF (RJPT-TD1(N,7)) 14,15,14
213 IF (RJPT-TD1(N,8)) 14,15,14
313 IF (RJPT-TD1(N,5)) 14,15,14
413 IF (RJPT-TD1(N,6)) 14,15,14
14 WRITE(6,104) JPT,N
NK=1
15 CONTINUE
IF (NK.NE.0) GO TO 99
C
IF (LD(1).EQ.0) GO TO 16
WRITE(6,101)
WRITE(6,105) (JPT,(J,TD1(JPT,J),J=1,13),JPT=1,NJPTS)
C
C COMPUTE ELEMENT BOUNDARY AREAS, CONVERT TD1 DATA TO FEET
16 DO 17 JPT=1,NJPTS
RD=TD1(JPT,2)+TD1(JPT,3)/2.
RT=TD1(JPT,2)-TD1(JPT,3)/2.
TC1(JPT,14)=.04363323*TD1(JPT,2)*TD1(JPT,3)
TC1(JPT,15)=.04363323*TD1(JPT,4)*RD
TC1(JPT,16)=.04363323*TD1(JPT,4)*RI
TC1(JPT,2)=TD1(JPT,2)/12.
TC1(JPT,3)=TD1(JPT,3)/12.

```

```

17 TD1(JPT,4)=TD1(JPT,4)/12.

C
C      READ INITIAL TEMPERATURE GUESSES, CURVE FIT CONDUCTIVITIES
      READ(5,106) (T(JPT),JPT=1,NJPTS)
      WRITE(6,107)
      WRITE(6,108) (JPT,T(JPT),JPT=1,NJPTS)
      DO 18 JPT=1,NJPTS
      TD1(JPT,19)=T(JPT)
18 CALL FIT(TD1,JPT,NDIM,MATL)

C
C      READ BOUNDARY CONDITION DATA AND COMPUTE COEFFICIENTS
      IF (LD(5).NE.0) WRITE(6,101)
      NK=0
      NTF=0
      NCR=0
      NTR=0
      DO 19 NBPT=1,NBPTS
19 CALL CON(NBPT,NBDIM,H,NBND,TBND,TD1,TDA,TD2,NDIM,T,LD,NK,NVDIM,NOD
     1F,JNTF)
      IF (NK.NE.0) GO TO 99

C
C      CON PRINTOUT
      IF (LD(2).EQ.0) GO TO 20
      WRITE(6,101)
      WRITE(6,109) (NBPT,NBND(NBPT),(H(NBPT,J),J=1,9),NBPT=1,NBPTS)
20 IF (NTF.EQ.0) GO TO 21
      WRITE(6,101)
      WRITE(6,110) (J,NODE(J),TCF(J),J=1,NTF)
      WRITE(6,111) (J,NODE(J),QF(J),J=1,NTF)

C
C      PERFORM ITERATIVE ANALYSIS
21 CALL TIME 1 (TDX)
      TDAT=(TDX-START)/3600.
      WRITE(6,112) TDAT
      NCC=0
      NPRT=RD(3)

C
      DO 29 NIT=1,NITS
      NK=0
      NCR=0
      NTF=0
      NDR=1
      NTR=0
      NCC=NCC+1
      LD(4)=0
      DO 22 NBPT=1,NBPTS
22 KAN(NBPT)=0

C
C      BOUNDARY CONDITION ITERATION
      DO 23 NBPT=1,NRPTS
      JRPT=NBND(NBPT)
      CALL QT(NBPT,NBDIM,NDIM,JBPT,H,SUMT,SUMH,TD1,TBND,T,CD,NVDIM,NIT,N
     1OEF,JNTF)
      23 O(JBPT)=SUMT(NBPT)

C
C      OVER-RELAXATION

```

```

NQR=0
DO 24 JPT=1,NJPTS
24 CALL TATS(TD1,JPT,NDIM,NBND,NBDIM,Q,T,H,RD,LD,CE,NK)
IF (NK.NF.0) GO TO 99
C
IF (LD(10).EQ.0) GO TO 25
WRITE(6,113)
WRITE(6,114) (JPT,T(JPT),Q(JPT),JPT=1,NJPTS)
C
C CHECK FOR CONVERGENCE, CORRECTION OF TD1 TEMPERATURES
25 ERP=CD(4)
IF (NIT.EQ.NITS) GO TO 30
IF (NCC.NE.NPRT) GO TO 26
NCC=0
LDC(4)=1
WRITE(6,115) NIT
26 DO 27 JPT=1,NJPTS
27 CALL CONCHK(JPT,NDIM,TD1,ERR,LD,NK,T)
IF (NK) 28,31,28
C
C RECALC. K FROM NEWEST TEMP.
28 DO 29 JPT=1,NJPTS
T1(JPT,19)=T(JPT)
29 CALL FIT(TD1,JPT,NDIM,MATL)
C
30 WRITE(6,116) NIT
GO TO 33
31 WRITE(6,117) NIT
C
C TEMPERATURE PRINTOUT
IF (LD(3)) 32,33,32
32 NITM1=NIT-1
WRITE(6,118) NITM1
WRITE(6,119) (JPT,TD1(JPT,19),JPT=1,NJPTS)
33 WRITE(6,118) NIT
WRITE(6,119) (JPT,T(JPT),JPT=1,NJPTS)
IF (LD(8).NE.0) PUNCH 106, (T(JPT),JPT=1,NJPTS)
C
C CONVERT FROM SEC.TO HRS.
DO 34 NBPT=1,NBPTS
SUMT(NBPT)=SUMT(NBPT)*3600.
SUMH(NBPT)=SUMH(NBPT)*3600.
DO 34 J=2,8,2
34 H(NBPT,J)=H(NBPT,J)*3600.
C
C PRINT OUT BOUNDARY CONDUCTANCES(H*A)
WRITE(6,120)
WRITE(6,121) (NBPT,NBND(NBPT),(H(NBPT,J),J=2,8,2),NBPT=1,NBPTS)
C
C PRINT OUT VAR.TEMP.BOUNDARY TEMPS.
IF (NTF.NF.0) WRITE(6,122) (J,NODE(J),TBND(J),J=1,NTF)
C
C PRINT OUT ELEMENT THERMAL CONDUCTIVITIES
DO 35 JPT=1,NJPTS
35 TE1(JPT,18)=TD1(JPT,18)*3600.
WRITE(6,123)

```

```

      WRITE(6,119) (JPT,TD1(JPT,18),JPT=1,NJPTS)
C
C      COMPUTE AND WRITE HEAT FLUXFS
      DO 36 JPT=1,NJPTS
      DO 36 K=1,4
      36 CE(JPT,K)=CE(JPT,K)*3600.
C
      WRITE(6,101)
      DO 48 JPT=1,NJPTS
      NE=TD1(JPT,5)
      IF (NE) 38,37,38
      37 QJE=0.0
      GO TO 39
      38 QJE=CE(JPT,1)*(T(NE)-T(JPT))
      39 NN=TD1(JPT,6)
      IF (NN) 41,40,41
      40 QJN=0.0
      GO TO 42
      41 QJN=CE(JPT,2)*(T(NN)-T(JPT))
      42 NW=TD1(JPT,7)
      IF (NW) 44,43,44
      43 QJW=0.0
      GO TO 45
      44 QJW=CE(JPT,3)*(T(NW)-T(JPT))
      45 NS=TD1(JPT,8)
      IF (NS) 47,46,47
      46 QJS=0.0
      GO TO 48
      47 QJS=CE(JPT,4)*(T(NS)-T(JPT))
      48 WRITE(6,124) JPT,QJE,QJN,QJW,QJS
C
      WRITE(6,101)
      WRITE(6,125) (JPT,(CE(JPT,J),J=1,4),JPT=1,NJPTS)
C
C      PRINT OUT BOUNDARY CONDUCTANCE SUMS AND HEAT FLUX SUMS
      WRITE(6,101)
      WRITE(6,126) (NBPT,NBND(NBPT),SUMH(NBPT),SUMT(NBPT),NBPT=1,NBPTS)
C
C      THERMAL EXPANSION CALCN. AND PRINTOUT
      IF (LD(10).NE.0) WRITE(6,101)
      DO 49 JPT=1,NJPTS
      CALL FIT2(TD1,NDIM,JPT,ALPHA,THEXP)
      49 CALL DEFORM(JPT,NDIM,TD1,RD,LD,THEXP)
      WRITE(6,127)
      WRITE(6,119) (JPT,THEXP(JPT),JPT=1,NJPTS)
      IF (LD(9).NE.0) PUNCH 128,(THEXP(JPT),JPT=1,NJPTS)
C
C      CHECK FOR ADDTL.CASES
      IF (NI(1)-1) 99,99,50
      50 GO TO 60
C
      99 CALL EXIT
      STOP
      END

```

\$IBFTC CDAM

```
SUBROUTINE CDA(LD,NI,RD,CD,MATL,ALPHA,NK)
C      PROBLEM PARAMETER INPUT, CONDUCTIVITY AND EXPANSION INPUT
C
C      DIMENSION LD(10),NI(5),RD(5),CD(10),MATL(15,11),ALPHA(15,11)
C      DIMENSION FILE(11),WCOM(12)
C      REAL MATL
C
101 FORMAT(12A6)
102 FORMAT(1H1,29X,12A6//)
103 FORMAT(10I6)
104 FORMAT(1H0,13X,3HLD=,10(3X,I2,1H,I3))
105 FORMAT(1H0,13X,3HNI=,5(3X,I2,1H,I3))
106 FORMAT(10F6.0)
107 FORMAT(1H0,13X,3HRD=,5(3X,I2,1H,1PE13.6))
108 FORMAT(1H0,13X,3HCD=,5(3X,I2,1H,1PE13.6)/16X,5(3X,I2,1H,1PE13.6))
109 FORMAT(1H0,2X,58ND.CONDUCTION OR BOUNDARY ELEMENTS EXCEEDS ALL DTE
2D STORAGE)
110 FORMAT(5F10.0)
111 FORMAT(6E13.6)
112 FORMAT(1H0,59X,11HDATA FOR K./(17X,6(2X,I2,1PE14.7)))
113 FORMAT(1H0,59X,15HDATA FOR ALPHA./(17X,6(2X,I2,1PE14.7)))
C
C      READ(5,101) WCOM
C      WRITE(6,102) WCOM
C
C      GENERAL DATA
C      READ(5,103) (LD(J),J=1,10)
C      WRITE(6,104) (J,LD(J),J=1,10)
C      READ(5,103) (NI(I),I=1,5)
C      WRITE(6,105) (I,NI(I),I=1,5)
C      READ(5,106) (RD(I),I=1,5)
C      WRITE(6,107) (I,RD(I),I=1,5)
C      READ(5,106) (CD(J),J=1,10)
C      WRITE(6,108) (J,CD(J),J=1,10)
C      IF (400.-CD(1)) 2,1,1
1 IF (200.-CD(2)) 2,3,3
2 WRITE(6,109)
NK=1
GO TO 11
C
C      CONDUCTIVITY DATA
3 DD 6 L=1,15
READ(5,110) (FILE(NCQ),NCQ=1,5)
IF (FILE(1)) 4,7,4
4 MN=FILE(2)
NP6=FILE(3)+6
READ(5,111) (FILE(NCQ),NCQ=6,NP6)
DJ 5 NCQ=1,NP6
5 MATL(MN,NCQ)=FILE(NCQ)
```

```

6 WRITE(6,112) (NCQ,FILE(NCQ),NCQ=1,NP6)
C
C      EXPANSION DATA
7 DO 10 I=1,15
     READ(5,110) (FILE(NCQ),NCQ=1,5)
     TF (FILE(1)) 8,11,8
8 MN=FILE(2)
     NP6=FILE(3)+6.
     RFAD(5,111) (FILE(NCQ),NCQ=6,NP6)
     DO 9 NCQ=1,NP6
9 ALPHA(MN,NCQ)=FILE(NCQ)
10 WRITE(6,113) (NCQ,FILE(NCQ),NCQ=1,NP6)
11 RETURN
END

```

\$IBETC FITM

```

SUBROUTINE FIT(TD1,JPT,NDIM,MATL)
C
C      FIT CONDUCTIVITY (K) FROM POLYNOMINAL CURVE
C
C      DIMENSTON TD1(NDIM,19),COS(5),CALC(6),MATL(15,11)
C      REAL MATL
C
101 FORMAT(1H0,2CX,4I1)TEMPERATURE EXCEEDS CURVE FIT LIMIT FOR K)
C
     TFMP= TD1(JPT,19)
     MAN = TD1(JPT,9)
     DO 1 NCQ=1,5
1   COS(NCQ)= MATL(MAN,NCQ)
     IF(TFMP-COS(1)) 3,3,2
2   WRITE(6,101)
     GO TO 9
3   NOP = COS(3)
     NOP1=NOP+1
     DO 4 NCQ=1,NOP1
     LC = 5+NCQ
4   CALC(NCQ)= MATL(MAN,LC)
     IF(COS(3)) 6,5,6
5   Y= CALC(1)*COS(4)
     GO TO 8
6   Y = CALC(NOP1)
     TFM1 = TFMP*COS(5)
     DO 7 NPY=1,NOP
     J2 = NOP1-NPY
7   Y= CALC(J2)+Y*TFM1
     Y = Y*COS(4)
8   TD1(JPT,18)=Y
C
9   RETURN
END

```

\$IBFTC CQNM

```
SUBROUTINE CQN(NBPT,NBDIM,H,NBND,TBND,TDL,TDA,TD2,NDIM,T,LD,NK,NVD
LIM,NODE,JNTF)

C      COMPUTE HEAT TRANSFER COEFFICIENTS

C      DIMENSION H(NBDIM,9),NBND(NBDIM),TBND(NVDIM),TDA(7),TD2(20)
DIMENSION TD1(NDIM,19),T(NDIM),LD(10),NODE(NVDIM),JNTF(NDIM)
COMMON/BLK1/J3NT(400),KAN(200),NTF,NDR,NTR,QF(95),NQR
COMMON/BLK2/TCF(95),GFN(95),AFN(95),NBR(95),NM(5),NAT(5),VBT(5)

C      101 FORMAT(3I6)
102 FORMAT(1H0,15X,60HBOUNDARY INDICATOR CARD ORDER ERROR,      BOUNDARY
ELEMENT NO.=,I4,11H CARD READS,I4)
103 FORMAT(I5,1X,F6.0)
104 FORMAT(1H0,10X,71HBOUNDARY INDEX (TYPE 1 OR 7) CARD ORDER ERROR,
2CONDUCTION ELEMENT NJ.=,I4,11H CARD READS,I4)
105 FORMAT(I5,E13.0,I6)
106 FORMAT(6F6.0,F12.0)
107 FORMAT(7F11.0)
108 FORMAT(1H0,10X,71HBOUNDARY INDEX (TYPE 2 TO 6) CARD ORDER ERROR,
2CONDUCTION ELEMENT NJ.=,I4,11H CARD READS,I4)
109 FORMAT(1H0,2X,8HELEMENT=,F4.0,2X,5HTYPE=,F2.0,2X,8HSJBTYPE=,F2.0,2
2X,5HNEXT=,F2.0,2X,11HITEMS READ=,F3.0,3X,10HAREA CODE=,F2.0,2X,13H
3SPECIAL AREA=,E12.5,1X,7HSQ.FEET)
110 FORMAT(1H0,2X,17HDUCT FLOW, LIQUID/2X,4HT-B=,F5.0,2X,4HK-F=,E11.4,
22X,4HC-P=,E11.4,2X,3HMU=,E11.4,2X,10HMASS FLOW=,E11.4,2X,7HD-HYDR=
3,E11.4,2X,7HL-FLOW=,E11.4/2X,3HRE=,E11.4,2X,3HPR=,E11.4,9X,8HH COE
4FF=,E14.7,2X,11HCoeff*AREA=,E14.7)
111 FORMAT(1H0,2X,15HSIDES OF ROTORS/2X,4HT-B=,F5.0,2X,4HK-F=,E11.4,2X
2,4HC-P=,E11.4,2X,3HMU=,E11.4,2X,3HNU=,E11.4,2X,5HR-AV=,E11.4,2X,4H
3GAP=,E11.4,2X,6HOMEGA=,F6.0/4HR-O=,E11.4,2X,5HFLAG=,F2.0,9X,3HRE=,
4E11.4,2X,8HPR**1/3=,E11.4,2X,8HH COEFF=,E14.7,2X,11HCoeff*AREA=,E1
54.7)
112 FORMAT(1H0,2X,15HRADIAL SEAL GAP/2X,4HT-B=,F5.0,2X,4HK-F=,E11.4,2X
2,4HC-P=,E11.4,2X,3HMU=,E11.4,2X,3HNU=,E11.4,2X,5HR-AV=,E11.4,2X,4H
3GAP=,E11.4,2X,6HOMEGA=,F6.0/2X,4HR-O=,E11.4,15X,3HRE=,E11.4,2X,8HP
4R**1/3=,E11.4,2X,5HRE-C=,E11.4/2X,8HH COEFF=,E14.7,2X,11HCoeff*ARE
5A=,E14.7)
113 FORMAT(1H0,2X,20HCENTRIC CYLINDERS/2X,4HT-B=,F5.0,2X,4HK-F=,E11
2.4,2X,4HC-P=,E11.4,2X,3HMU=,E11.4,2X,3HNJ=,E11.4,2X,4HR-O=,E11.4,2
3X,4HK-I=,E11.4,2X,6HOMEGA=,F6.0/2X,5HV-AX=,E11.4,15X,3HRE=,E11.4,2
4X,8HPR**1/3=,E11.4,2X,8H COEFF=,E14.7,9X,11HCoeff*AREA=,E14.7)
114 FORMAT(1H0,2X,10HFLAT PLATE/2X,4HT-B=,F5.0,2X,4HK-F=,E11.4,2X,4HC-
2P=,E11.4,2X,3HMU=,E11.4,2X,3HNU=,E11.4,2X,7HL-FLON=,E11.4,2X,7HV-F
3LOW=,E11.4/2X,3HRE=,E11.4,2X,3HPR=,E11.4,9X,3HH COEFF=,E14.7,2X,11
4HCoeff*AREA=,E14.7)

C      FUTURE FORCED CONVEC.COEFF.FORMATS (115-8)
119 FORMAT(1H0,2X,39HHORIZONTAL CYLINDER OR VERTICAL SURFACE/2X,4HT-B=
2,F5.0,2X,4HK-F=,E11.4,2X,4HC-P=,E11.4,2X,3HMJ=,E11.4,2X,3HNU=,E11.
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34,2X,17HL-FLOW OR 3-HYDR=,E11.4/2X,3HPR=,E11.4,2X,3HGR=,E11.4,9X,8
4HH COEFF=,E14.7,2X,11HCUEFF*AREA=,E14.7)
120 FORMAT(1H0,2X,19HLIQUID FILM COOLING/2X,4HT-B=,F5.0,2X,4HN/L=,E11.
24,2X,4HC-P=,E11.4,2X,7HL-FLOW=,E11.4,10X,8HH COEFF=,E14.7,2X,11HCJ
3EFF*AREA=,E14.7)

C FUTURE FREE CONVEC.COEFF.FORMATS (121-5)
126 FORMAT(1H0,2X,9HRADIATION/2X,4HT-B=,F5.0,2X,10HFACTOR-SE=,E11.4,2X
2,10HFACTOR-ES,E11.4,2X,8HEMIS.-E=,E11.4,2X,8HEMIS.-S=,E11.4/2X,8HH
3 COEFF=,E14.7,2X,11HCUEFF*AREA=,E14.7)
127 FORMAT(1H0,2X,21HSPECIFIED COEFFICIENT/2X,4HT-B=,F5.0,2X,8HH COEFF
2=,E14.7,5X,11HCUEFF*AREA=,E14.7)
128 FORMAT(1H0,2X,26HVAK.TEMP.DUCT FLOW, LIQUID/2X,4HT-B=,F5.0,2X,4HK-
2F=,E11.4,2X,4HC-P=,E11.4,2X,3HMU=,E11.4,2X,10HMASS FLOW=,E11.4,2X,
37HD-HYDR=,E11.4,2X,7HL-FLOW=,E11.4/2X,9HANN.NBR.=,F4.0,2X,9HFLDW N
4BR=,F4.0,2X,7HFLAG-C=,F2.0,2X,7HFLAG-I=,F2.0,2X,64X-SEC=,E11.4/2X,
53HRE=,E11.4,2X,3HPR=,E11.4,6X,8HH COEFF=,E14.7,2X,11HCUEFF*AREA=,E
614.7)
129 FORMAT(1H0,2X,24HVAK.TEMP.RADIAL SEAL GAP/2X,4HT-B=,F5.0,2X,4HK-F=
2,E11.4,2X,4HC-P=,E11.4,2X,3HMU=,E11.4,2X,3HNJ=,E11.4,2X,5HR-AV=,E1
31.4,2X,4HGAP=,E11.4,2X,64HOMEGA=,F6.0/2X,4HK-O=,E11.4,2X,7HFLAG-C=,
4F2.0,2X,7HFLAG-I=,F2.0,2X,9HANN.NBR.=,F4.0,2X,9HFLU.NBR.=,F4.0,2X,
510HMASS FLOW=,E11.4/2X,3HRE=,E11.4,2X,8HPR*#1/3=,E11.4,2X,5HRE-C=,
6E11.4,9X,8HH COEFF=,E14.7,2X,11HCUEFF*AREA=,E14.7/2X,14HHT.GEN.FAC
7TDR=,E12.5)

C FUTURE VAR.TEMP.COEFF.FORMATS (130-1)
132 FORMAT(1H0,2X,38HCOMBINED FLOW ELEMENT, CONDUCTION NO.=,I4,2X,24HF
2LOW FROM CNDN.ELEMENTS ,I3,4HANL ,14)

C FUTURE COEFF.SUBPROGR.FORMATS (115-8(FORCED),121-5(FREE),130-1
C (VAR.TEMP.))

C READ INDICATOR CARD, CHECK ORDER
READ(5,101) NBPT,NBND(NBPT),INDB
IF (NBPT-NBPT) 1,2,1
1 WRITE(5,102) NBPT,NBPT
NK=1

C SET PARAMETERS
2 JBPT=N3ND(NBPT)
JBNT(JBPT)=NBPT
TD1(JBPT,17)=INDB

C SPECIFIED TEMPERATURE
IF (INDB.NE.7) GO TO 4
READ(5,103) JBP,T(JBP)
IF (JBP.NE.JBPT) GO TO 3
TD1(JBPT,19)=T(JBP)
GO TO 99
3 WRITE(6,104) JBPT,JBP
NK=1
GO TO 99

C 4 GO TO (5,7,7,7,7,7),INDB

```

```

C      SPECIFIED HEAT FLUX
5 READ(5,105) JBP,+(NBPT,1),IADDQ
  IF (JBP.EQ.JBPT) GO TO 6
  WRITE(6,104) JBPT,JBP
  NK=1
6 IF (IADDQ.EQ.0) GO TO 99
C      BOUNDARY AREAS
7 AE=TD1(JBPT,14)
  AN=TD1(JBPT,15)
  AS=TD1(JBPT,16)
C      READ DATA FOR TYPES 2 TO 6
90 READ(5,106) (TDA(J),J=1,7)
  NITM=TDA(5)
  READ(5,107) (TD2(J),J=1,NITM)
C      CHECK CONDUCTION NO.MATCH
  JBP=TDA(1)
  IF (JBP-JBPT) 3,9,6
3 WRITE(6,108) JBPT,JBP
  NK=1
9 IF (NK.NE.0) GO TO 99
C      ITYPE=TDA(2)
  GO TO (99,10,29,46,48,55),ITYPE
C      FORCED CONVECTION
10 ISTYPE=TDA(3)
  GO TO (11,13,15,17,19),ISTYPE
C      DUCT FLOW, LIQUID
11 CALL SN1(TDA,TD2,AE,AN,AS)
  H(NBPT,2)=H(NBPT,2)+TD2(16)
  H(NBPT,3)=H(NBPT,3)+TD2(16)*TD2(1)
  IF (LD(5).EQ.0) GO TO 12
  WRITE(6,109) (TDA(J),J=1,7)
  WRITE(6,110) (TD2(J),J=1,7),(TD2(K),K=13,16)
12 IF (TDA(4)) 90,99,90
C      SIDES OF ROTORS
13 CALL SN2(TDA,TD2,AE,AN,AS)
  H(NBPT,2)=H(NBPT,2)+TD2(14)
  H(NBPT,3)=H(NBPT,3)+TD2(14)*TD2(1)
  IF (LD(5).EQ.0) GO TO 14
  WRITE(6,109) (TDA(J),J=1,7)
  WRITE(6,111) (TD2(J),J=1,14)
14 IF (TDA(4)) 90,99,90
C      RADIAL SEAL GAP
15 CALL SN3(TDA,TD2,AE,AN,AS)
  H(NBPT,2)=H(NBPT,2)+TD2(19)
  H(NBPT,3)=H(NBPT,3)+TD2(19)*TD2(1)
  IF (LD(5).EQ.0) GO TO 16
  WRITE(6,109) (TDA(J),J=1,7)
  WRITE(6,112) (TD2(J),J=1,9),(TD2(K),K=15,19)

```

```

16 IF (TDA(4)) 90,99,90
C
C      CONCENTRIC CYLINDERS
17 CALL SN4(TDA,TD2,AE,AN,AS)
H(NBPT,2)=H(NBPT,2)+TD2(13)
H(NBPT,3)=H(NBPT,3)+TD2(13)*TD2(1)
IF (LD(5).EQ.0) GO TO 18
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,113) (TD2(J),J=1,13)
18 IF (TDA(4)) 90,99,90
C
C      FLAT PLATE
19 CALL SN5(TDA,TD2,AE,AN,AS)
H(NBPT,2)=H(NBPT,2)+TD2(11)
H(NBPT,3)=H(NBPT,3)+TD2(11)*TD2(1)
IF (LD(5).EQ.0) GO TO 20
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,114) (TD2(J),J=1,11)
20 IF (TDA(4)) 90,99,90
C
C      FOR FUTURE SUBROUTINES (4 MORE) (STATEM. NOS 21-2,23-4,25-6,27-8)
C
C      FREE CONVECTION
29 ISTYPE=TDA(3)
GO TO (30,32,34),ISTYPE
C
C      HORIZONTAL CYLINDER
30 CALL FC1(TDA,TD2,AE,AN,AS,T,JBPT,NDIM)
H(NBPT,4)=H(NBPT,4)+TD2(10)
H(NBPT,5)=H(NBPT,5)+TD2(10)*TD2(1)
IF (LD(5).EQ.0) GO TO 31
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,119) (TD2(J),J=1,10)
31 IF (TDA(4)) 90,99,90
C
C      VERTICAL PLANE OR CYLINDER
32 CALL FC2(TDA,TD2,AE,AN,AS,T,JBPT,NJIM)
H(NBPT,4)=H(NBPT,4)+TD2(10)
H(NBPT,5)=H(NBPT,5)+TD2(10)*TD2(1)
IF (LD(5).EQ.0) GO TO 33
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,119) (TD2(J),J=1,10)
33 IF (TDA(4)) 90,99,90
C
C      LIQUID FILM COOLING, GRAVITY FLOW
34 CALL FC3(TDA,TD2,AE,AN,AS)
H(NBPT,4)=H(NBPT,4)+TD2(6)
H(NBPT,5)=H(NBPT,5)+TD2(6)*TD2(1)
IF (LD(5).EQ.0) GO TO 35
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,120) (TD2(J),J=1,6)
35 IF (TDA(4)) 90,99,90
C
C      FOR FUTURE SUBROUTINES (5 MORE) (STATEM. 36-7,38-9,40-1,42-3,44-5)
C
C      RADIATION

```

```

46 CALL RA1( TDA, TD2, AE, AN, AS, T, JBPt, NDIM )
H(NBPT,6)=H(NBPT,6)+TD2(7)
H(NBPT,7)=H(NBPT,7)+TD2(7)*TD2(1)
IF (LD(5).EQ.0) GO TO 47
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,126) (TD2(J),J=1,7)
47 IF (TDA(4)) 90,99,90
C
C      SPECIFIED COEFFICIENT
48 NCR=TDA(6)
GO TO 49,50,49,>1,52),NCR
49 AF=AE
GO TO 53
50 AF=AN
GO TO 53
51 AF=AS
GO TO 53
52 AF=TDA(7)
53 TD2(3)=TD2(2)*AF
H(NBPT,2)=H(NBPT,2)+TD2(3)
H(NBPT,3)=H(NBPT,3)+TD2(3)*TD2(1)
IF (LD(5).EQ.0) GO TO 54
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,127) (TD2(J),J=1,3)
54 IF (TDA(4)) 90,99,90
C
C      VARIABLE TEMPERATURE FORCED CONVECTION
55 NTF=NTF+1
ISIYPE=TDA(3)
GO TO 56,57),ISIYPE
C
C      VAR.TEMP.DUCT FLOW, LIQUID
56 CALL SN1( TDA, TD2, AE, AN, AS )
H(NBPT,8)=TD2(16)
H(NBPT,9)=TD2(5)*TD2(3)*TD2(12)
TBND(NTF)=TD2(1)
TCF(NTF)=H(NBPT,8)/H(NBPT,9)
AFN(NTF)=TD2(8)
GFN(NTF)=TD2(9)
NODE(NTF)=JBPT
JXPT=NODE(NTF)
JNTF(JXPT)=NTF
IF (LD(5).EQ.0) GO TO 60
WRITE(6,109) (TDA(J),J=1,7)
WRITE(6,128) (TD2(J),J=1,16)
GO TO 60
C
C      VAR.TEMP.RADIAL SEAL GAP
57 CALL SN3( TDA, TD2, AE, AN, AS )
TBND(NTF)=TD2(1)
H(NBPT,8)=TD2(19)
H(NBPT,9)=TD2(14)*TD2(3)
TCF(NTF)=H(NBPT,8)/H(NBPT,9)
AFN(NTF)=TD2(12)
GFN(NTF)=TD2(13)
NODE(NTF)=JBPT

```

```

C JXPT=NODE(NTF)
C JNTF(JXPT)=NTF
C
C FLUID SHEAR HEAT GENERATION
C OMKP=TD2(8)*TD2(8)*TD1(JBPT,2)*TD1(JBPT,2)
C QF(NTF)=TD2(20)*.0000399416*TD2(4)*OMKP*TD1(JBPT,14)/TD2(7)
C
C IF (LD(5).EQ.0) GO TO 60
C WRITE(6,109) (TDA(J),J=1,7)
C WRITE(6,129) (TD2(J),J=1,20)
C GO TO 60
C
C FOR FUTURE SUBROUTINES (2 MORE) (STATEMENTS 58,59)
C
C FLOW INITIATION ELEMENT
60 IF (TD2(11).EQ.0.) GO TO 61
  NTR=NTR+1
  NBR(NTR)=TD2(11)
  GO TO 62
C
C COMBINED FLOW ELEMENT
61 IF (TD2(10).EQ.0.) GO TO 62
  NDR=NDR+1
  READ(5,101) NAT(NDR),NBT(NDR)
  WRITE(6,132) JBPT,NAT(NDR),NBT(NDR)
  VM(NDR)=JBPT
62 IF (TDA(4)) 90,99,90
C
99 RETURN
END

```

\$IBFTC SN1M

```
SUBROUTINE SN1(TDA,TD2,AE,AN,AS)
C      HEAT TRANSFER COEFFICIENTS FOR LIQUIDS IN DUCTS
C
C      DIMENSION TD2(20),TDA(7)
C
C      COMPUTE REYNOLDS AND PRANDTL NUMBERS
C      TD2(13)=TD2(5)*TD2(6)/TD2(4)
C      TD2(14)=TD2(3)*TD2(4)/TD2(2)
C
C      LAMINAR OR TURBULENT COEFFICIENT
C      TD2(17)=TD2(6)/TD2(7)
C      TD2(18)=TD2(2)/TD2(6)
C      TD2(19)=TD2(17)**.7
C      IF (TD2(13)-2500.) 1,1,2
1 TD2(15)=1.24*TD2(18)*(TD2(13)*TD2(14)*TD2(17))**(.1/3.)
      GO TO 5
2 IF (TD2(13)-7000.) 4,3,3
3 TD2(15)=.023*TD2(18)*(TD2(13)**.8)*(TD2(14)**.4)*(1.+.3*TD2(19))
      GO TO 5
4 TD2(15)=.5*((7000.-TD2(13))/4500.)*1.24*(TD2(13)*TD2(14)*TD2(17))*2*(1./3.)+.5*((TD2(13)-2500.)/4500.)*.023*TD2(18)*(TD2(13)**.8)*(TD2(14)**.4)*(1.+.3*TD2(19))
C
C      COEFFICIENT*AREA
5 NCR=TDA(6)
      GO TO (6, 7, 8, 9), NCR
6 AF=AE
      GO TO 10
7 AF=AN
      GO TO 10
8 AF=AS
      GO TO 10
9 AF=TDA(7)
10 TD2(16)=AF*TD2(15)
      RETURN
      END
```

\$IBFTC SN2M

```
SUBROUTINE SN2(TDA,TD2,AF,AN,AS)
C
C      HEAT TRANSFER COEFFICIENTS FOR FLUID MOVING RELATIVE TO RADIAL
C      SURFACE SEPERATE BOUNDARY LAYERS
C
C      DIMENSION TD2(20),TDA(7)
C
C      REYNOLDS AND PRANDTL NUMBERS
C      TD2(11)=TD2(1)*TD2(6)*TD2(6)/TD2(5)
C      TD2(12)=(TD2(3)*TD2(4)/TD2(2))**(.1./3.)
C
C      LAMINAR OR TURBULENT COEFFICIENT
C      TD2(15)=TD2(2)/TD2(6)
C      TD2(16)=(TD2(7)/TD2(6))**.1
C      IF (TD2(11)-158000.) 1,1,4
C
C      LAMINAR
1 IF (TD2(10).EQ.0.) GO TO 2
2 TD2(17)=.501E5-.6508*TD2(7)/TD2(9)
   GO TO 3
3 TD2(13)=.574*TD2(15)*TD2(16)*(TD2(11)**.5)*TD2(12)/TD2(17)
   GO TO 7
C
C      TURBULENT
4 IF (TD2(10).EQ.0.) GO TO 5
5 TD2(17)=.48E5-.35778*TD2(7)/TD2(9)
   GO TO 6
6 TD2(13)=.01826*TD2(15)*TD2(16)*(TD2(11)**.8)*TD2(12)/TD2(17)
C
C      COEFFICIENT*AREA
7 NCR=TDA(6)
   GO TO (8,9,9,10,11),NCR
8 AF=AF
   GO TO 12
9 AF=AN
   GO TO 12
10 AF=AS
   GO TO 12
11 AF=TDA(7)
12 T2(14)=AF*TD2(13)
RETURN
END
```

```
$TBFTC SN3M
```

```
      SUBROUTINE SN3(TDA,TD2,AF,AN,AS)
C
C      HEAT TRANSFER COEFFICIENTS FOR ROTOR AND STATOR WITH SMALL
C      CLEARANCE     MERGED BOUNDARY LAYERS
C
C      DIMENSION TD2(20),TDA(7)
C
C      REYNOLDS AND PRANDTL NUMBERS
C      TD2(15)=TD2(5)*TD2(6)*TD2(6)/TD2(5)
C      TD2(16)=(TD2(3)*TD2(4)/TD2(2))**(1./3.)
C
C      LAMNTAR OR TURBULENT COEFFICIENT
C      TC2(17)=366.24*((TD2(9)/TD2(7))**(10./9.))
C      TF=(TD2(15)-TD2(17))/1.1.2
C      1 TD2(18)=2.*TC2(2)*TD2(16)/TD2(7)
C      TF2(20)=1.
C      GO TO 3
C      2 TF2(18)=.0297*(TD2(2)/TD2(6))*((TD2(6)/TD2(7))**(1./6.))*TD2(16)*(
C      1TC2(15)**.8)
C      TC2(20)=.0002286*(TD2(17)**1.5)*((TD2(7)/TD2(6))**(5./3.))
C
C      COEFFICIENT*AREA
C      3 NCR=TDA(6)
C      GO TO 4,5,6,7,NCR
C      4 AF=AF
C      GO TO 8
C      5 AF=AN
C      GO TO 8
C      6 AF=AS
C      GO TO 8
C      7 AF=TDA(7)
C      8 TF2(19)=AF*TF2(18)
C      RETURN
CEND
```

\$IBFTC SN4M

```
SUBROUTINE SN4(TDA,TD2,AF,AN,AS)
C
C      HEAT TRANSFER COEFFICIENTS FOR FLOW BETWEEN CONCENTRIC CYLINDERS
C      INNER ROTATING, NO AXIAL FLOW EFFECT ON BOUNDARY LAYERS
C
C      DIMENSION TD2(20),TDA(7)
C
C      TURBULENT COEFFICIENT
C      TD2(11)=(TD2(3)*TD2(4)/TD2(2))**(.1./3.)
C      TD2(14)=TD2(5)*.5*(TD2(6)+TD2(7))
C      TD2(15)=TD2(14)*TD2(14)+TD2(9)*TD2(9)
C      TD2(16)=SORT(TD2(15))
C      TD2(17)=TD2(6)-TD2(7)
C      TD2(18)=2.*TD2(17)*TD2(16)/TD2(5)
C      TD2(12)=(TD2(2)/TD2(17))*(.015*(TD2(10)**.8)*TD2(11)*((TD2(6)/TD2(17))**.46)+.052*(TD2(14)**(.2./3.))*TD2(17)*TD2(11)/TD2(5))
C
C      Coefficient*ARFA
C      NCR=TDA(6)
C      GO TO (1,2,1,3,4),NCR
1 AF=AF
      GO TO 5
2 AF=AN
      GO TO 5
3 AF=AS
      GO TO 5
4 AF=TDA(7)
5 TD2(13)=AF*TD2(12)
      RETURN
      END
```

\$TBFTC SN5M

```
SUBROUTINE SN5(TDA,TD2,AE,AN,AS)
C   HEAT TRANSFER COEFFICIENTS FOR FLOW OVER FLAT PLATES
C   DIMENSION TD2(20),TDA(7)
C   REYNOLDS AND PRANDTL NUMBERS
C   TD2(8)=TD2(7)*TD2(6)/TD2(5)
C   TD2(9)=(TD2(2)*TD2(4)/TD2(2))**(1./3.)
C   LAMINAR OR TURBULENT COEFFICIENT
C   TF(TD2(8)=5(000.) 1,1,2
1  TD2(10)=.332*TD2(2)*(TD2(8)**.5)*TD2(9)/TD2(6)
C   GO TO 3
2  TD2(10)=.0288*TD2(2)*(TD2(8)**.8)*TD2(9)/TD2(6)
C   COEFFICIENT*AREA
3  NCR=TDA(6)
C   GO TO 4,5,6,7,NCR
4  AF=AF
C   GO TO 8
5  AF=AN
C   GO TO 8
6  AF=AS
C   GO TO 8
7  AF=TDA(7)
8  TD2(11)=AF*TD2(10)
RETURN
END
```

\$TBFTC FC1M

```
SUBROUTINE FC1(TDA,TD2,AE,AN,AS,T,JBPT,NDIM)
C
C      HEAT TRANSFER COEFFICIENTS FOR HORIZ.CYLINDER FREE CONVECTION
C
C      DIMENSION TDA(7),TD2(20),T(NDIM)
C
C      TD2(12)=ABS(TD2(1)-T(JBPT))
C      TD2(13)=.5*(TD2(1)+T(JBPT))+459.7
C      TD2(14)=TD2(2)/TD2(6)
C
C      PRANDTL AND GRASHOF NUMBERS
C      TD2(7)=TD2(3)*TD2(4)/TD2(2)
C      TD2(8)=TD2(6)*TD2(6)*TD2(6)*32.174*TD2(12)/(TD2(5)*TD2(5)*TD2(13))
C      TD2(11)=TD2(7)*TD2(8)
C
C      LAMINAR OR TURBULANT COEFFICIENT
C      IF (TD2(11)-.1F+10) 1,1,?
C      1 TD2(9)=.53*TD2(14)*TD2(11)**(1./4.)
C      GO TO 3
C      2 TD2(9)=.13*TD2(14)*TD2(11)**(1./3.)
C
C      COEFFICIENT*AREA
C      3 NCR=TDA(6)
C      GO TO 4,5,4,6,7),NCR
C      4 AF=AF
C      GO TO 8
C      5 AF=AN
C      GO TO 8
C      6 AF=AS
C      GO TO 8
C      7 AF=TDA(7)
C      8 TD2(10)=AF*TD2(9)
C      RETURN
C      END
```

```

$TBFTC FC2M

      SUBROUTINE FC2(TDA,TD2,AE,AN,AS,T,JBPT,NDEM)
C      HEAT TRANSFER COEFFICIENTS FOR VERT. SURFACE FREE CONVECTION
C      DIMENSION TDA(7),TD2(20),T(NDIM)
C
C      TC2(12)=ABS(TD2(1)+T(JBPT))
C      TC2(13)=.5*(TD2(1)+T(JBPT))+45.9.7
C      TC2(14)=TD2(2)/TD2(6)
C
C      PRANDTL AND GRASHOF NUMBERS
C      TD2(7)=TD2(3)*TD2(4)/TD2(2)
C      TD2(8)=TD2(6)*TD2(6)*TD2(6)*32.174*TD2(12)/(TD2(5)*TD2(5)*TD2(13))
C      TD2(11)=TD2(7)*TD2(8)
C
C      LAMINAR OR TURBULANT COEFFICIENT
C      IF (TD2(11)-.1F+10) 1,1,2
C      1  TD2(9)=.44*TC2(14)*TD2(11)**(1./4.)
C         GO TO 3
C      2  TC2(9)=.13*TC2(14)*TD2(11)**(1./3.)
C
C      COEFFICIENT*AF EA
C      3  NCR=TDA(6)
C         GO TO 4,5,4,6,71,NCR
C      4  AF=AF
C         GO TO 8
C      5  AF=AN
C         GO TO 8
C      6  AF=AS
C         GO TO 8
C      7  AF=TDA(7)
C      8  TC2(10)=AF*TC2(9)
C      RETURN
CEND

```

\$IBFTC FC3M

SUBROUTINE FC3(TDA,TD2,AE,AN,AS)

C HET TRANSFER COEFFICIENTS FROM HORIZONTAL CYLINDER TO LIQUID
C FILM (GRAVITY FLOW)
C
C DIMENSION TD2(20),TDA(7)
C
TD2(5)=TD2(2)*TD2(3)/TD2(4)
NCR=TDA(6)
GO TO (1,2,1,3,4),NCR
1 AF=AF
GO TO 5
2 AF=AN
GO TO 5
3 AF=AS
GO TO 5
4 AF=TDA(7)
5 TD2(6)=AF*TD2(5)
RETURN
END

\$IBFTC RA1M

SUBROUTINE RA1(TDA,TD2,AF,AN,AS,T,JBPT,NDIM)

C RADIATION(THERMAL)-GRAY BODY
C
C DIMENSION TDA(7),TD2(20),T(NDIM)
C
TAE=TD2(1)
TAS=T(JBPT)
TD2(8)=1.-TD2(4)
TD2(9)=1.-TD2(5)
TD2(10)=TAE*TAF*TAE+TAE*TAS+TAE*TAS+TAS*TAS+TAS*TAS
TD2(6)=4.83E-13*TD2(4)*TD2(9)*TD2(2)*TD2(10)/(1.-(TD2(2)*TD2(3)*TD
12(8)*TD2(9)))
NCR=TDA(6)
GO TO (1,2,1,3,4),NCR
1 AF=AF
GO TO 5
2 AF=AN
GO TO 5
3 AF=AS
GO TO 5
4 AF=TDA(7)
5 TD2(7)=AF*TD2(6)
RETURN
END

\$IBFTC QTM

```
SUBROUTINE QT(NBPT,NBDIM,NDIM,JBPT,H,SUMT,SUMH,TD1,TBND,T,CD,NVDIM
1,VIT,NTF,JNTF)
C
C      COMPUTE BOUNDARY HEAT FLUXES
C
DIMENSION H(NBDIM, 9),SUMT(NBDIM),SUMH(NBDIM),TD1(NDIM,19)
DIMENSION TBND(NVDIM),T(NDIM),CD(10),TS(100),JNTF(NDIM)
COMMON/BLK1/J3NT(400),KAN(200),NTF,NDR,NTR,QF(95),NQR
COMMON/BLK2/TCF(95),GFn(95),AFN(95),NBR(95),NM(5),NAT(5),NBT(5)
C
101 FORMAT(1H0,2X,39HC JMBINED FLOWS ELEMENT, COMBINATION NO.,I2,3X,12H
2C CONDUCT.VNU.=,I3,3X,10H NDRY.NO.=,I3,3X,31H PREVIOUS ELEMENT VAR.TEM
3P.NUS.=,I3,2X,3H AND,I4)
102 FORMAT(1H0,2X,19HC CONDUCT.ELEMENT NO.,I4,3X,20H VAR.TEMP.ELEMENT NO.
2,I4,3X,10H FLOW CODE=,I2)
C
      SUMT(NBPT)=0.0
      SUMH(NBPT)=0.0
      ITYPE=TD1(JBPT,17)
      IF (ITYPE.NE.7) GO TO 1
      GO TO 99
C
C      SPECIFIED FLUX
1 IF (H(NBPT,1).EQ.0.) GO TO 2
      SUMT(NBPT)=H(NBPT,1)
C
C      FORCED CONVECTION (INCL. SPECIFIED COEFF.)
2 IF (H(NBPT,2).EQ.0.) GO TO 3
      SUMH(NBPT)=H(NBPT,2)
      SUMT(NBPT)=SUMT(NBPT)+H(NBPT,3)-H(NBPT,2)*T(JBPT)
C
C      FREE CONVECTION
3 IF (H(NBPT,4).EQ.0.) GO TO 4
      SUMH(NBPT)=SUMH(NBPT)+H(NBPT,4)
      SUMT(NBPT)=SUMT(NBPT)+H(NBPT,5)-H(NBPT,4)*T(JBPT)
C
C      RADIATION
4 IF (H(NBPT,6).EQ.0.) GO TO 5
      SUMH(NBPT)=SUMH(NBPT)+H(NBPT,6)
      SUMT(NBPT)=SUMT(NBPT)+H(NBPT,7)-H(NBPT,6)*T(JBPT)
C
C      VARYING TEMPERATURE
5 IF (H(NBPT,8).EQ.0.) GO TO 99
      NTF=NTF+1
      VPT=0
      LHN=0
      WF1=0.
      SUMH(NBPT)=SUMH(NBPT)+H(NBPT,8)
      IF (KAN(NBPT).EQ.0) GO TO 6
      SUMT(NBPT)=SUMT(NBPT)+H(NBPT,8)*(TBND(NTF)-T(JBPT))
```

```

C
6 JNPT=AFN(NTF)
JLHN=GFN(NTF)
TS=0.
IF (JNPT.EQ.0) GO TO 7
NPT=JBNT(JNPT)
7 IF (JLHN.EQ.0) GO TO 8
LHN=JNTF(JLHN)
8 IF (NM(NDR)-JBPT) 14,9,14

C
C      COMBINED FLOWS
9 JNFR=NAT(NDR)
JNFS=NBT(NDR)
IF (JNFR.EQ.0) GO TO 10
NFR=JBNT(JNFR)
JAT=JNTF(JNFR)
GO TO 11
10 NFR=0
TBND(NFR)=0.
H(NFR,9)=0.
11 IF (JNFS.EQ.0) GO TO 12
NFS=JBNT(JNFS)
JBF=JNTF(JNFS)
GO TO 13
12 NFS=0
TBND(NFS)=0.
H(NFS,9)=0.
13 IF ((NIT-1).EQ.0) WRITE(6,101) NDR,JBPT,NTF,JAT,JBF
C
C      STARTING TEMP.FOR COMBINED FLOWS ELEMENT TEMP.CALC.
COMBF=H(NFR,9)+H(NFS,9)
PNFR=H(NFR,9)*TBND(NFR)/COMBF
PNFS=H(NFS,9)*TBND(NFS)/COMBF
STEMP=PNFR+PNFS
NDR=NDR+1
GO TO 18

C
C      STARTING TEMP.ORDINARY FLOW ELEMENT
14 NTR=NTR+1
NER=NBR(NTR)
IF ((NIT-1).EQ.0) WRITE(6,102) JBPT,NTR,NBR(NTR)
IF (LHN.NE.0) GO TO 17
GO TO (15,16),NER
15 STEMP=CD(6)
GO TO 18
16 STEMP=CD(7)
GO TO 18
17 STEMP=TBND(LHN)

C
18 IF (KAN(NBPT).NE.0) GO TO 99

C
C      CALC.TEMP.CHANGE
HINC=TCF(NTF)/CD(9)
IF (ZF(NTF).EQ.0.) GO TO 19
QF1=ZF(NTF)/(H(NBPT,9)*CD(9))
19 NCD=CD(9)

```

```

IF (NPT.NE.0) GO TO 22
C
C TEMP.CHANGE=NO ANN.NABOR
DO 21 INC=1,NCO
IF (INC.NE.1) GO TO 20
TS(INC)=STEMP+HINC*(T(JBPT)-STEMP)+QF1
GO TO 21
20 TS(INC)=TS(INC-1)+HINC*(T(JBPT)-TS(INC-1))+QF1
21 CONTINUE
TBND(NTF)=TS(INC)
GO TO 25
C
C TEMP.CHANGE=ANNULAR NABOR
22 HANC=H(NPT,8)/(H(NPT,9)*CD(9))
DO 24 INC=1,NCO
IF (INC.NE.1) GO TO 23
TS(INC)=STEMP+HINC*(T(JBPT)-STEMP)+HANC*(T(JNPT)-STEMP)+QF1
GO TO 24
23 TS(INC)=TS(INC-1)+HINC*(T(JBPT)-TS(INC-1))+HANC*(T(JNPT)-TS(INC-1)
1)+QF1
24 CONTINUE
TBND(NTF)=TS(INC)
TBND(NPT)=TBND(NTF)
KAN(NPT)=1
25 SUMT(NBPT)=SUMT(NBPT)+4(NBPT,8)*(TBND(NTF)-T(JBPT))
99 RETURN
END

```

\$TBFTC TATSM

```
SUBROUTINE TATS(TD1,JPT,NDIM,NBND,NBDIM,Q,T,H,RD,LD,CE,NK)
C
C      OVER-RELAXATION AND NEW TEMPERATURE CALCULATION
C
      DIMENSION TD1(NDIM,19),CE(NDIM,4),LD(10),RD(5)
      DIMENSION NBND(NBDIM),Q(NDIM),T(NDIM),H(NBDIM,9)
      COMMON/BLK1/JBNT(390),KAN(190),NTF,NDR,NTR,QF(95),NQR
C
      101 FORMAT(1HO.5X,5BHERROR IN BNDRY AND COND.NO CORRESP.(TATS CHECK OF
          ?ITERATION,16,13H)COND.ELEMENT,I4,25HGIVES BNDRY NO OF ELEMENT,I4)
C
      HSUM=0.
C
C      EAST CONDUCTANCE
      NE= TD1(JPT,5)
      IF (NE) 2,1,2
      1 CE(JPT,1)=0.C
      GO TO 3
      2 CE(JPT,1)=1./(TD1(JPT,4)/(2.*TD1(JPT,14)*TD1(JPT,18))+TD1(NE,4)/(2
          1.*TD1(NE,14)*TD1(NE,18))+TD1(JPT,10))
*C
C      NORTH CONDUCTANCE
      NN=TD1(JPT,6)
      IF (NN) 5,4,5
      4 CE(JPT,2)=0.C
      GO TO 6
      5 CE(JPT,2)=1./(2.*TD1(JPT,3)/(TD1(JPT,18)*(3.*TD1(JPT,15)+TD1(JPT,1
          16)))+2.*TD1(NN,3)/(TD1(NN,18)*(3.*TD1(NN,16)+TD1(NN,15)))+TD1(JPT,
          21)))
C
C      WEST CONDUCTANCE
      NW=TD1(JPT,7)
      IF (NW) 8,7,8
      7 CE(JPT,3)=0.C
      GO TO 9
      8 CE(JPT,3)=1./(TD1(JPT,4)/(2.*TD1(JPT,14)*TD1(JPT,18))+TD1(NW,4)/(2
          1.*TD1(NW,14)*TD1(NW,18))+TD1(JPT,12))
*C
C      SOUTH CONDUCTANCE
      NS= TD1(JPT,8)
      IF (NS) 11,10,11
      10 CE(JPT,4)=0.C
      GO TO 12
      11 CE(JPT,4)=1./(2.*TD1(JPT,3)/(TD1(JPT,18)*(3.*TD1(JPT,16)+TD1(JPT,1
          15)))+2.*TD1(NS,3)/(TD1(NS,18)*(3.*TD1(NS,15)+TD1(NS,16)))+TD1(JPT,
          21)))
C
      12 NTD=TD1(JPT,17)
      IF(NTD.EQ.7) GO TO 99
```

```

C COMPUTE RESIDUAL, OVER-RELAX
RES=CE(JPT,1)*(T(NE)-T(JPT))+CE(JPT,2)*(T(NN)-T(JPT))+CE(JPT,3)*(T
1(NW)-T(JPT))+CE(JPT,4)*(T(NS)-T(JPT))+O(JPT)
CSUM=CF(JPT,1)+CF(JPT,2)+CE(JPT,3)+CE(JPT,4)
C
C WRES=RD(1)*RES
C
C COMPUTE NEW TEMPERATURE
IF (O(JPT)) 13,15,13
13 NBPT=JBNT(JPT)
JPPT=NBND(NBPT)
IF (JPPT.FQ.JPT) GO TO 14
WRITE(6,101) NTT,JPT,JPPT
NK=1
GO TO 99
14 HSUM=H(NBPT,2)+H(NBPT,4)+H(NBPT,6)+H(NBPT,8)
15 T(JPT)=T(JPT)+WRES/(CSUM+HSUM)
C
99 RETURN
END

```

```

$TBFTC FITA

      SUBROUTINE FIT2(TD1,NDIM,JPT,ALPHA,THEXP)
C      FIT EXPANSION COEFFICIENT FROM POLYNOMINAL CURVE
C
C      DIMENSION TD1(NDIM,19),COS(5),CALC(6),ALPHA(15,11),THEXP(NDIM)
C
C      101 FORMAT(1H0,2CX,45HTEMPERATURE EXCFEDS CURVE FIT LIMIT FOR ALPHA)
C
      TFMP= TD1(JPT,19)
      MAN = TD1(JPT,9)
      DO 1 NCQ=1,5
1     COS(NCQ)= ALPHA(MAN,NCQ)
      IF(TFMP-COS(1)) 3,3,2
2     WRITE(6,101)
      GO TO 9
3     NOP = COS(3)
      NOP1=NOP+1
      DO 4 NCQ=1,NOP1
      LC = 5+NCQ
4     CALC(NCQ)= ALPHA(MAN,LC)
      TF(COS(3)) 6,5,6
5     Y= CALC(1)*COS(4)
      GO TO 8
6     Y = CALC(NOP1)
      TEM1 = TFMP*COS(5)
      DO 7 NPY=1,NOP
      J2 = NOP1-NPY
7     Y= CALC(J2)+Y*TEM1
      Y = Y*COS(4)
8     THEXP(JPT)=Y
C
9     RETURN
      END

```

```
$TBFTC CONCHC
```

```
      SUBROUTINE CONCHK(JPT,NDIM,T01,ERR,LD,NK,T)
C
C      CHECK FOR CONVERGENCE OF OVER-RELAXATION CALC.
C
C      DIMENSION TD1(NDIM,19),LD(10),T(NDIM)
C
C      101 FORMAT(24X,I4,4(5X,E14.7))
C
C      DIFF=T(JPT)-TD1(JPT,19)
C      IF (ABS(DIFF).LE.ERR) GO TO 1
C      NK=1
C      1 IF (LD(4).EQ.0) GO TO 9
C      WRITE(6,101) JPT,T(JPT),TD1(JPT,19),DIFF,ERR
C
C      9 RETURN
C      END
```

```
$TBFTC DEFRMM
```

```
      SUBROUTINE DEFRMM(JPT,NDIM,TD1,RD,LD,THEXP)
C
C      COMPUTE FREE THERMAL EXPANSION  ALPHA*DELTA TEMP
C
C      DIMENSION TD1(NDIM,19),THEXP(NDIM),RD(5),LD(10)
C
C      101 FORMAT(1H0,1CX,16HELEMENT COND.NO.,I4,3X,6HALPHA=,E13.6,3X,5HTEMP=
C      2,F12.5,3X,14HALPHA*(T1-T0)=,E13.6)
C
C      TIN=RD(2)
C      DELTFM=TD1(JPT,19)-TIN
C      A=THEXP(JPT)
C      ACT=THEXP(JPT)*DELTFM
C      THEXP(JPT)=ACT
C      IF (LD(10).EQ.0) GO TO 99
C      WRITE(6,101) JPT,A,TD1(JPT,19),THEXP(JPT)
C
C      99 RETURN
C      END
```

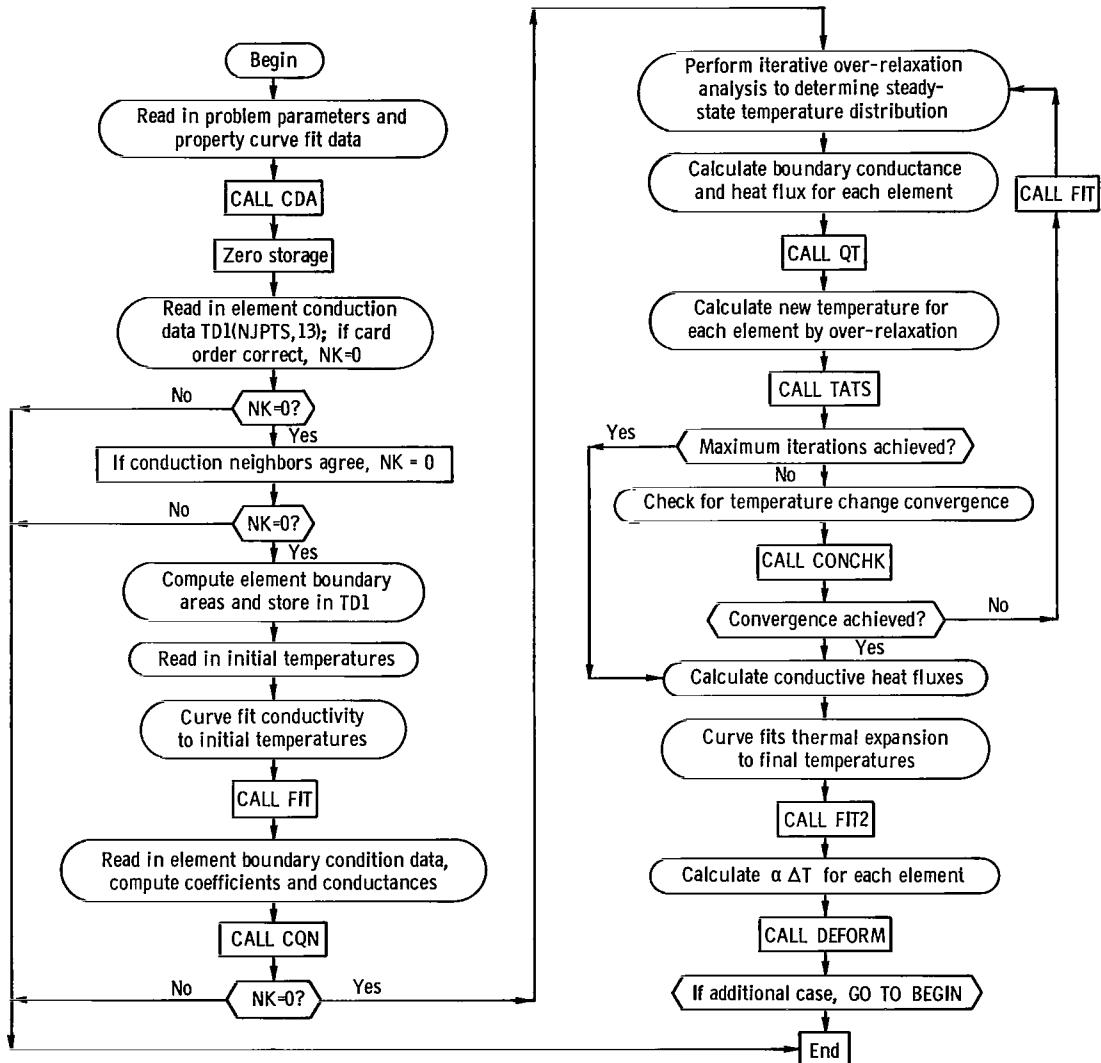


Figure 8. - Flow chart for main route SEAL2.

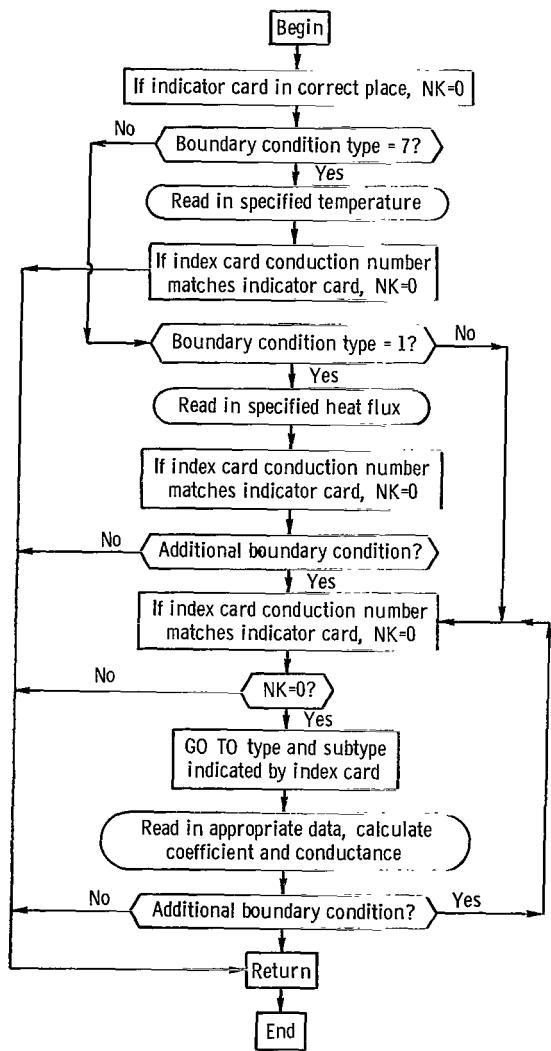


Figure 9. - Flow chart for subroutine CQN.

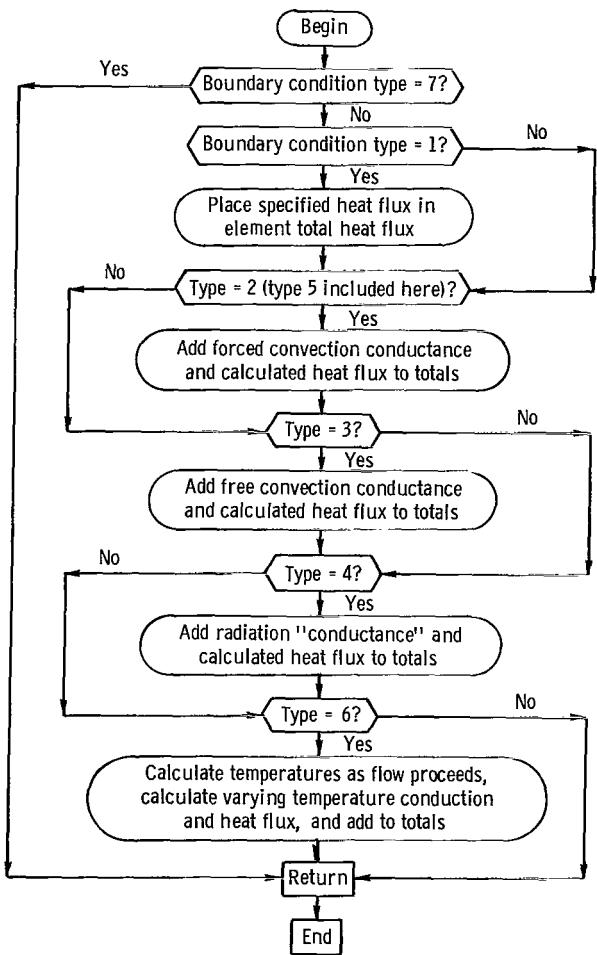


Figure 10. - Flow chart for subroutine QT.

APPENDIX B

CHANGING OF BOUNDARY CONDITION COEFFICIENTS

The program is designed to make the addition or substitution of equations for heat transfer coefficients relatively easy. The coefficients, the products of coefficient times boundary area and the products of coefficient times boundary area times bulk fluid (or environmental) temperature are calculated in subroutines SN1, SN2, SN3, SN4, SN5, FC1, FC2, FC3, and RA1.

The varying temperature coefficients, at present, use subroutines SN1 and SN3. Other calculations for the varying temperature boundary conditions are performed in subroutines CQN and QT.

Substitution of a Different Coefficient

To substitute a new expression for one of those presently used, the appropriate subroutine is rewritten using the present words in the TD2 list for the output (coefficient, etc.). This assumes that the same properties or at least the same number of properties are required. If not, the number of items to be read in must be changed in subroutine CQN. Also the TD2 words used for output must be changed in the coefficient subroutine as well as in subroutine CQN. The appropriate formats of subroutine CQN must also be changed to reflect the TD2 changes.

The TD2 list of a varying temperature condition must be compatible with the TD2 list of the coefficient subprogram used. Thus, if subroutine SN1 is changed to require more input data, subroutine VT1 (see table II) must also be changed. The output, which is common to both, must use the same new TD2 words.

TD2 word changes for a varying temperature subroutine must be made in subroutine QT as well as in subroutine CQN. Wherever a TD2 word (e.g., TD2(15)) appears in the varying temperature sections of subroutines CQN and QT, the new word must be substituted.

Also the two indicator flag words (TD2(10) and TD2(11)) must be the same for all VT (varying temperature) conditions. The calculations involving the flags require this. The sections in subroutines CQN and QT handling the temperature change along the flow and the effect of flow combination use the flags to control the flow in the subroutines. If one or both of the flag words are changed for one VT condition, it (they) must be changed for all conditions and the new word(s) must be used in subroutines CQN and QT.

A word of warning should be added. As implied previously, the TD2 list is used for both input to and output from the coefficient subroutines. This table is dimensioned for 20 items. If more are needed, the dimensions in SEAL2, CQN, and the coefficient subroutines must be increased.

Addition of New Coefficients

If an additional boundary condition is desired, a new subroutine must be written. A varying temperature condition involves the precautions mentioned under substitution. Also the TD2 list capacity must be remembered.

Also, for an added condition, a section must be added to subroutine CQN. This section will be analogous to the subtype sections already present. The products of coefficient times area and of coefficient times area times bulk fluid temperature must be stored in the correct places in the conductance matrix. An output format for the TD2 list must be composed. Unused statement and format numbers are provided for this purpose.

APPENDIX C

COMPUTER PROGRAM APPLICATION TO MAINSHAFT SEAL

Seal Description

This appendix is presented as an application of the computer program to a specific seal design. Figure 11 shows a schematic of a mainshaft seal being developed for gas-

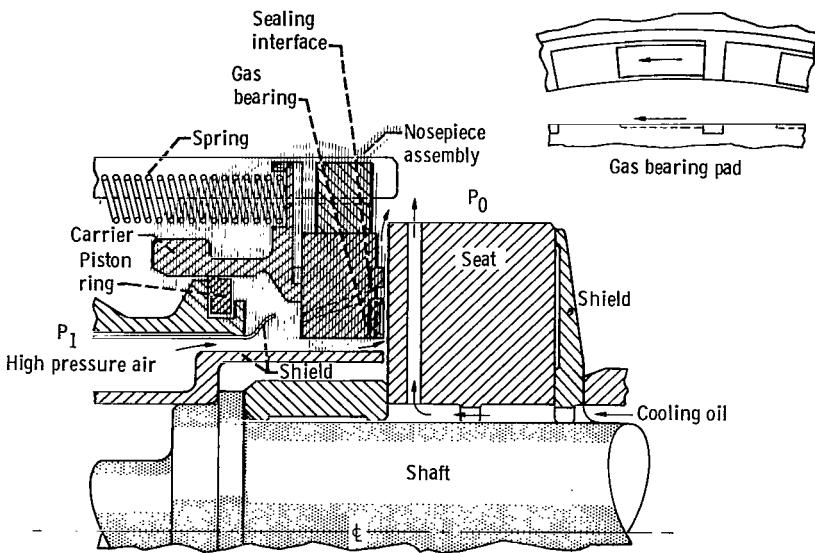


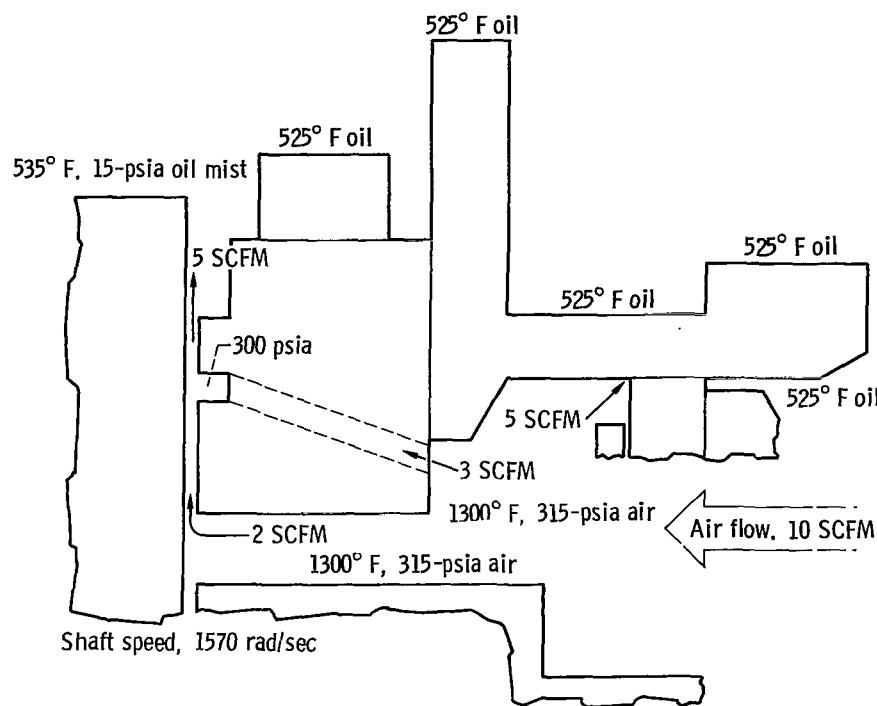
Figure 11. - Face seal with self-acting gas bearing for lift augmentation.

turbine engines. This is a face-type seal with a self-acting gas bearing which acts to prevent rubbing contact when deformation of the sealing faces occurs.

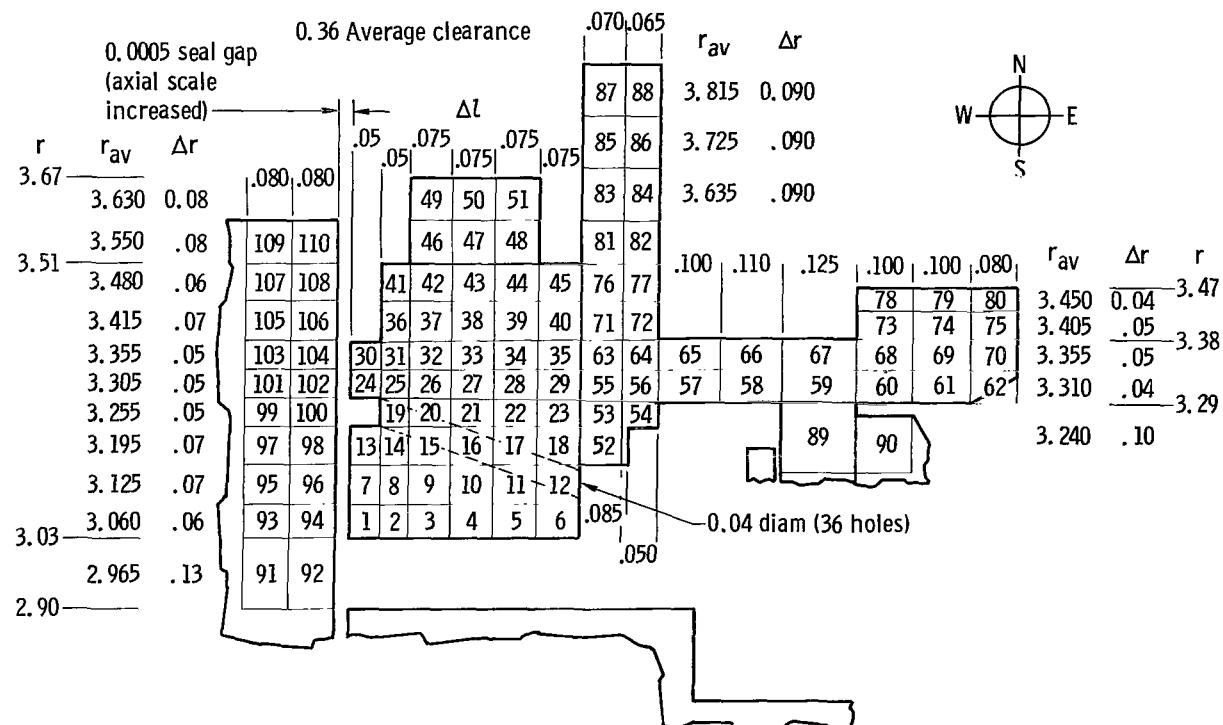
In figure 12(a) a modified version of the nosepiece assembly is presented and the boundary conditions are shown. This modification is for the purpose of concentrating on the mechanics of the program application.

Figure 12(b) shows the element schematic including conduction numbers and dimensions. A portion of the seal plate is included since it influences the temperature of the airflow through the seal gap and therefore has an effect on the nosepiece temperature. Also a portion of the piston ring and its holder, which form a conduction path to the nosepiece carrier, are included.

The numbering sequence starts with the nosepiece assembly since this is the region of interest for this problem. The desired printout is therefore available at the beginning of

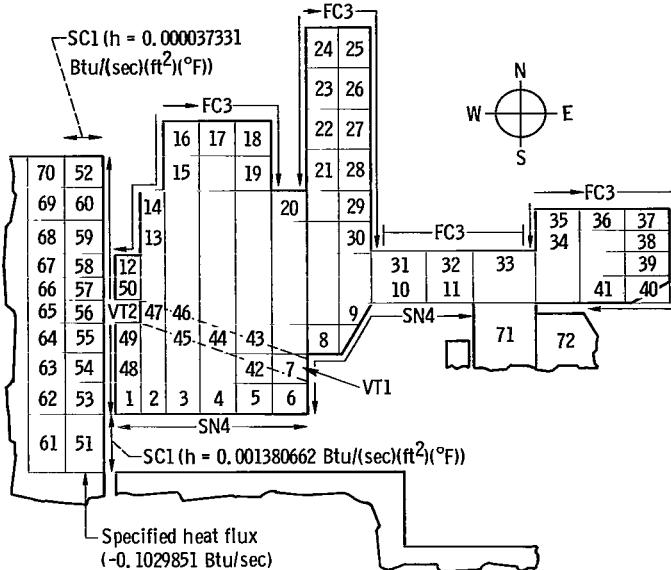


(a) Modification of and boundary conditions for nosepiece assembly of seal depicted in figure 11.



(b) Dimensions and conductance element numbering for nosepiece assembly depicted in figure 12(a). (All dimensions in inches.)

Figure 12. - Example problem.



(c) Boundary element numbering and boundary heat transfer conditions for nosepiece assembly depicted in figure 12(a).

Figure 12. - Concluded.

each section of output, and the remaining elements can be ignored. The piece by piece numbering is not necessary; any convenient order could be used.

Figure 12(c) shows the boundary numbers and the subroutines used to calculate the heat transfer coefficients. Here again, the sequence is a matter of convenience and the nosepiece assembly is numbered first. Numbers 1 to 11 are assigned to the region where concentric cylinder flow (SN4) is assumed. Conduction element 56 was ignored since only a relatively tiny part is a boundary of the piece. Numbers 12 to 41 were assigned to the liquid film cooled (FC3) boundaries. The varying temperature duct flow (VT1) is numbered next. Since conduction element 12 already has a boundary number (7), the sequence continues with 42 assigned to conduction element 11. The method used is an approximation to avoid the complexities involved if conduction elements 18 and 14 are included as should be done. For the varying temperature seal gap (VT2) flow, numbers 48 to 50 were assigned to the nosepiece elements not already given boundary numbers.

For the seal plate, the east face of conduction element 92 and the north face of 110 were assigned coefficients. The south face of 92 was assigned a heat flux. These values were obtained from a thermal analysis of the seal shown in figure 11. Boundary numbers 53 to 60 were assigned to the seal plate elements exposed to seal gap flow. The remaining boundary numbers, 61 to 72, were assigned to elements given specified temperatures obtained from the previous analysis mentioned.

The title and parameter cards (Items 1 to 5 under Computer Input in appendix A) were filled out as indicated in the first section of the printout. Also in this section, Items 6

and 7, the thermal conductivity and expansion data, are indicated.

Next are the conduction element cards (input Item 8). These are shown in the second section of printout (conduction element table). Words 1 to 8 of each card are obtained from the information in figure 12(b). In word 9, three materials were used. The nose-piece was material number 1. The piston ring and its holder were material number 3. The remaining parts were material number 2. The last four words are contact resistances.

It should be noted that each contact resistance must appear twice since the program ignores neighbor contact resistance in computing heat fluxes. Thus for elements 42 and 46, the contact resistance appears in word 11 (north contact resistance) of element 42 and in word 13 (south contact resistance) of element 46. Contact resistances between parts were calculated using a "conductance coefficient" ($h_c = 0.2$) for conductance across the interface. The resistance between elements 90 and 60 was the difference between the resistance of the air gap and the resistance of an equal volume of material number three (element 90 uses the same mean radius and radial width as element 89). The resistance between mismatched elements (elements 52 and 54 were changed in axial length to approximate the actual dimensions in the region) was calculated as illustrated in figure 13. It was assumed that the larger i^{th} element (e.g., 52) has a conduction path length of d' rather than $\Delta l_i/2$ as in figure 5. The area was based on Δl_m rather than Δl_i . The contact resistance was the difference between $d'/2\pi r_m \Delta l_m$ and $\Delta r_i/4\pi r_m \Delta l_i$.

The initial temperature estimates (input Item 9) follow the conduction cards. These values were obtained from a previous analysis in order to reduce the computer time required. However, any reasonable estimates can be used including the use of one temperature for all elements.

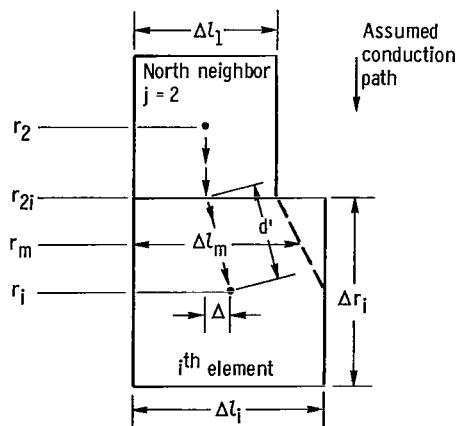


Figure 13. - Outline of calculation of contact resistance between elements of different axial dimensions. $d' = \sqrt{\Delta^2 + (\Delta l_i/2)^2}$; $\Delta l_m = (\Delta l_i + \Delta l_2)/2$.

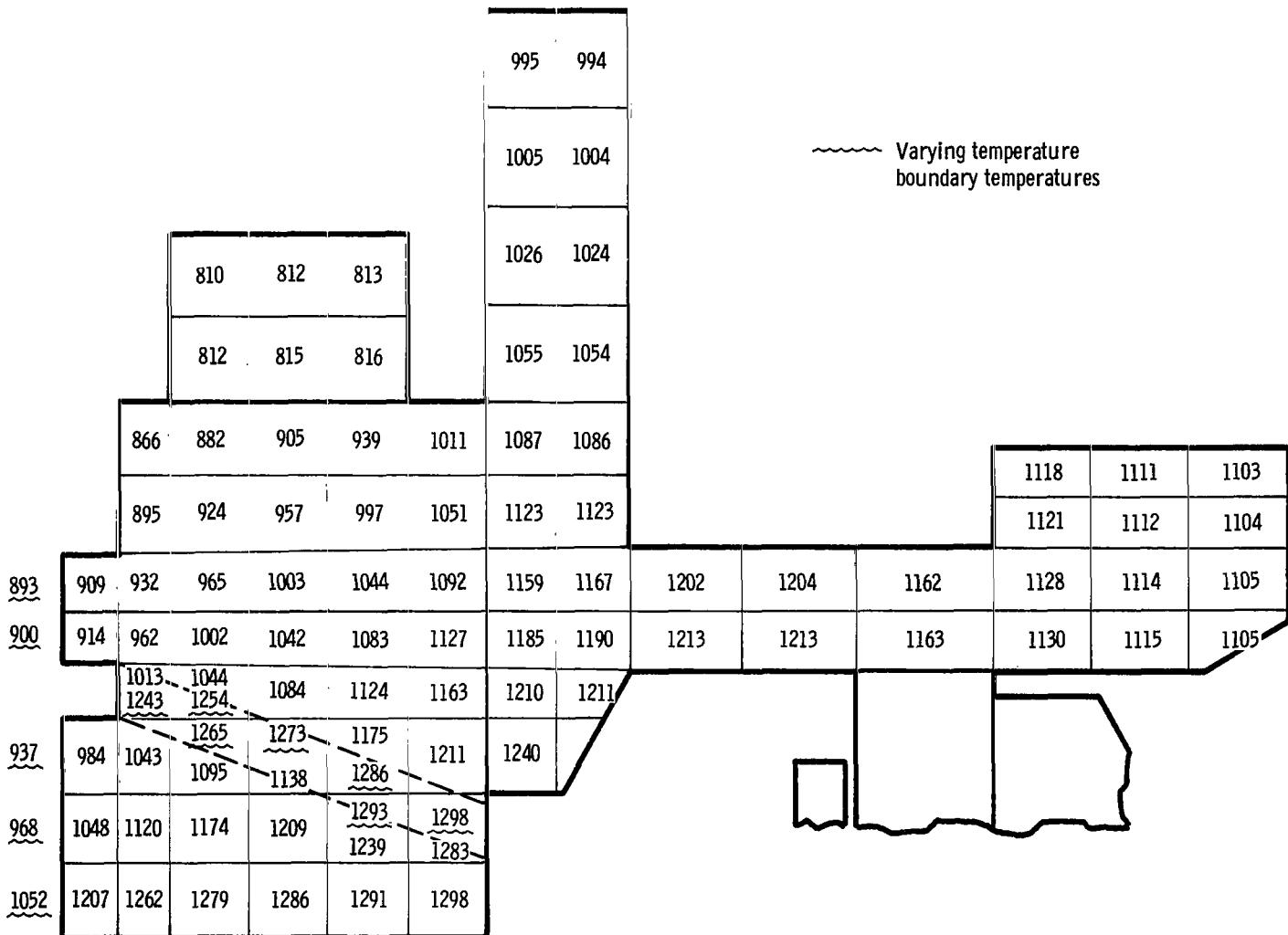


Figure 14. - Example problem of temperature distribution in °F for nosepiece assembly of seal depicted in figure 11.

The boundary heat transfer cards (input Item 9) are assembled element by element. The boundary numbers determine the order of the sets. A set consists of the indicator card for the element followed by the index card, plus any others required, for each "side" of the element that is a boundary. The indicator cards do not appear in the printout but the order of the other cards for each element is indicated in the section of printout following the initial temperatures. This section, as well as the conduction element table, are not standard output items but are included to indicate the cards required. Some calculated values (Reynolds or Prandtl numbers and the following items for each element side) are included in this printout.

In preparing the varying temperature boundary cards, the region at which the flows joined required the use of approximations because the program permits only one varying temperature condition per element. Boundary element 47 (fig. 12(c)) was assumed to be affected only by the duct flow. For boundary elements 49 and 50, special areas (code number 5) were used with the sums of the appropriate faces as the area values. Element 56 was made the combined flow element with 47 and 55 (conduction numbers 19 and 98) as the upstream elements.

The film cooled (FC3) boundary was another area where approximations were involved. It was assumed that flows originated at the northwest corners of boundary elements 16 (two 0.018 lbm/sec), 24 (two 0.018 lbm/sec), and 35 (two 0.012 lbm/sec) (see fig. 12(c)). The flows were assumed to be either toward or parallel to the axis except for elements 20 and 31 to 33. The arrows outlining the region indicate this. Elements 20 and 31 to 33 had flow around the circumference and were the only elements where the equation properly applied. For the other elements, the flow length was taken as the sum of the element sides over which the flow occurred and the length perpendicular to flow was the average circumference for the side.

After all cards were prepared and assembled, a preliminary run was made to check for errors. The LD card (input Item 2) options (or words) 1, 2, and 5 were used. Limits of 1 minute and 100 iterations were set. The results of the final run are presented in the sections of printout starting with the element center temperatures. These temperatures and the varying temperature boundary temperatures are also plotted in figure 14. Improved results could be obtained by using fluid properties based on the new film temperatures calculated from the results. This applies especially to the varying temperature flows where the properties were based on the initial flow temperatures (1300° F).

Computer Output for Sample Problem

SAMPLE PROBLEM# MAINSHAFT SEAL NOSEPIECE

```

ID= 1, 1    2, 1    3, 1    4, -0    5, 1    6, -0    7, -0    8, -0    9, -0    10, -0
NT= 1, 1    2, -0    3, -0    4, -0    5, -0
RD= 1, 1.50000E 00    2, 7.00000E 01    3, 1.00000E 02    4,-0.           5,-0.
CD= 1, 1.10000E 02    2, 7.20000E 01    3, 1.00000E 03    4, 5.00000E-02    5,-0.
       6, 1.30000E C3    7, 1.30000F 03    8,-0.           9, 2.00000E 01    10,-0.
          DATA FOR ALPHA.
1 1.500000E 03    2 1.000000F 00    3 1.000000F 00    4 1.000000E 00    5 1.000000E 00    6 1.350000E-06
7 1.500000E-09
          DATA FOR ALPHA.
1 1.800000E 03    2 2.000000E 00    3 1.000000E 00    4 1.000000E 00    5 1.000000E 00    6 2.944700E-06
7 2.540000E-C9
          DATA FOR ALPHA.
1 1.600000E 03    2 3.000000E 00    3 2.000000E 00    4 1.000000E 00    5 1.000000E 00    6 7.020000E-06
7 8.6071429E-10
8 3.5714290E-13

```

CONDUCTION ELEMENT TABLE (T01)

1	1, 1.0000F 00	2, 3.0600F 00	3, 6.0000F-02	4, 5.0000F-02	5, 2.0000E 00	6, 7.0000F 00	7, 0.
	8, 0.	9, 1.0000F 00	10,-0.	11,-0.	12,-0.	13,-0.	
2	1, 2.0000F 00	2, 3.0600E 00	3, 6.0000E-02	4, 5.0000E-02	5, 3.0000E 00	6, 8.0000E 00	7, 1.0000E 00
	8,-0.	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
3	1, 3.0000E 00	2, 3.0600E 00	3, 6.0000E-02	4, 7.5000F-02	5, 4.0000E 00	6, 9.0000E 00	7, 2.0000E 00
	8,-0.	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
4	1, 4.0000E 00	2, 3.0600E 00	3, 6.0000F-02	4, 7.5000E-02	5, 5.0000E 00	6, 1.0000E 01	7, 3.0000E 00
	8,-0.	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
5	1, 5.0000E 00	2, 3.0600F 00	3, 6.0000F-02	4, 7.5000E-02	5, 6.0000E 00	6, 1.1000E 01	7, 4.0000E 00
	8,-0.	9, 1.0000F 00	10,-0.	11,-0.	12,-0.	13,-0.	
6	1, 6.0000F 00	2, 3.0600E 00	3, 6.0000F-02	4, 7.5000E-02	5, 0.	6, 1.2000E 01	7, 5.0000E 00
	8,-0.	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
7	1, 7.0000E 00	2, 3.1250E 00	3, 7.0000F-02	4, 5.0000F-02	5, 8.0000E 00	6, 1.3000F 01	7, 0.
	8, 1.0000F 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
8	1, 8.0000E 00	2, 3.1250E 00	3, 7.0000F-02	4, 5.0000E-02	5, 9.0000E 00	6, 1.4000E 01	7, 7.0000E 00
	8, 2.0000E 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
9	1, 9.0000F 00	2, 3.1250E 00	3, 7.0000E-02	4, 7.5000E-02	5, 1.0000F 01	6, 1.5000E 01	7, 8.0000E 00
	8, 3.0000F 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
10	1, 1.0000F 01	2, 3.1250E 00	3, 7.0000F-02	4, 7.5000E-02	5, 1.1000F 01	6, 1.6000E 01	7, 9.0000E 00
	8, 4.0000F 00	9, 1.0000F 00	10,-0.	11,-0.	12,-0.	13,-0.	
11	1, 1.1000E 01	2, 3.1250E 00	3, 7.0000E-02	4, 7.5000E-02	5, 1.2000E 01	6, 1.7000E 01	7, 1.0000E 01
	8, 5.0000E 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
12	1, 1.2000E 01	2, 3.1250E 00	3, 7.0000E-02	4, 7.5000E-02	5, 0.	6, 1.8000E 01	7, 1.1000E 01
	8, 6.0000F 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
13	1, 1.3000E 01	2, 3.1950E 00	3, 7.0000F-02	4, 5.0000F-02	5, 1.4000E 01	6, 0.	7, 0.
	8, 7.0000F 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
14	1, 1.4000E 01	2, 3.1950E 00	3, 7.0000F-02	4, 5.0000E-02	5, 1.5000E 01	6, 1.9000E 01	7, 1.3000E 01
	8, 8.0000F 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
15	1, 1.5000E 01	2, 3.1950E 00	3, 7.0000E-02	4, 7.5000E-02	5, 1.6000E 01	6, 2.0000E 01	7, 1.4000E 01
	8, 9.0000F 00	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	
16	1, 1.6000F 01	2, 3.1950E 00	3, 7.0000E-02	4, 7.5000E-02	5, 1.7000E 01	6, 2.1000E 01	7, 1.5000E 01
	8, 1.0000F 01	9, 1.0000E 00	10,-0.	11,-0.	12,-0.	13,-0.	

17	1, 1.1000E 01 8, 1.1000E 01	2, 3.1950E 00 9, 1.0000E 00	3, 7.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 1.8000E 01 12,-0.	6, 2.2000E 01 13,-0.	7, 1.6000E 01
18	1, 1.8000E 01 8, 1.2000E 01	2, 3.1950E 00 9, 1.0000E 00	3, 7.0000E-02 10, 5.1200E 02	4, 7.5000E-02 11,-0.	5, 5.2000E 01 12,-0.	6, 2.3000E 01 13,-0.	7, 1.7000E 01
19	1, 1.9000E 01 8, 1.4000E 01	2, 3.2550E 00 9, 1.0000E 00	3, 5.0000E-02 10, 0.	4, 5.0000E-02 11,-0.	5, 2.0000E 01 12,-0.	6, 2.5000E 01 13,-0.	7, 0.
20	1, 2.0000E 01 8, 1.5000E 01	2, 3.2550E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 2.1000E 01 12,-0.	6, 2.6000E 01 13,-0.	7, 1.9000E 01
21	1, 2.1000E 01 8, 1.6000E 01	2, 3.2550E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 2.2000E 01 12,-0.	6, 2.7000E 01 13,-0.	7, 2.0000E 01
22	1, 2.2000E 01 8, 1.7000E 01	2, 3.2550E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 2.3000E 01 12,-0.	6, 2.8000E 01 13,-0.	7, 2.1000E 01
23	1, 2.3000E 01 8, 1.8000E 01	2, 3.2550E 00 9, 1.0000E 00	3, 5.0000E-02 10, 7.0400E 02	4, 7.5000E-02 11,-0.	5, 5.3000E 01 12,-0.	6, 2.9000E 01 13,-0.	7, 2.2000E 01
24	1, 2.4000E 01 8, 0.	2, 3.3050E 00 9, 1.0000E 00	3, 5.0000E-02 10, 0.	4, 5.0000E-02 11,-0.	5, 2.5000E 01 12,-0.	6, 3.0000E 01 13,-0.	7, 0.
25	1, 2.5000E 01 8, 1.9000E 01	2, 3.3050E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 5.0000E-02 11,-0.	5, 2.6000E 01 12,-0.	6, 3.1000E 01 13,-0.	7, 2.4000E 01
26	1, 2.6000E 01 8, 2.0000E 01	2, 3.3050E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 2.7000E 01 12,-0.	6, 3.2000E 01 13,-0.	7, 2.5000E 01
27	1, 2.7000E 01 8, 2.1000E 01	2, 3.3050E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 2.8000E 01 12,-0.	6, 3.3000E 01 13,-0.	7, 2.6000E 01
28	1, 2.8000E 01 8, 2.2000E 01	2, 3.3050E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 2.9000E 01 12,-0.	6, 3.4000E 01 13,-0.	7, 2.7000E 01
29	1, 2.9000E 01 8, 2.3000E 01	2, 3.3050E 00 9, 1.0000E 00	3, 5.0000E-02 10, 6.9300E 02	4, 7.5000E-02 11,-0.	5, 5.5000E 01 12,-0.	6, 3.5000E 01 13,-0.	7, 2.8000E 01
30	1, 3.0000E 01 8, 2.4000E 01	2, 3.3550E 00 9, 1.0000E 00	3, 5.0000E-02 10, 0.	4, 5.0000E-02 11,-0.	5, 3.1000E 01 12,-0.	6, 0. 13,-0.	7, 0.
31	1, 3.1000E 01 8, 2.5000E 01	2, 3.3550E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 5.0000E-02 11,-0.	5, 3.2000E 01 12,-0.	6, 3.6000E 01 13,-0.	7, 3.0000E 01
32	1, 3.2000E 01 8, 2.6000E 01	2, 3.3550E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 3.3000E 01 12,-0.	6, 3.7000E 01 13,-0.	7, 3.1000E 01
33	1, 3.3000E 01 8, 2.7000E 01	2, 3.3550E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 3.4000E 01 12,-0.	6, 3.8000E 01 13,-0.	7, 3.2000E 01
34	1, 3.4000E 01 8, 2.8000E 01	2, 3.3550E 00 9, 1.0000E 00	3, 5.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 3.5000E 01 12,-0.	6, 3.9000E 01 13,-0.	7, 3.3000E 01
35	1, 3.5000E 01 8, 2.9000E 01	2, 3.3550E 00 9, 1.0000E 00	3, 5.0000E-02 10, 6.8300E 02	4, 7.5000E-02 11,-0.	5, 6.3000E 01 12,-0.	6, 4.0000E 01 13,-0.	7, 3.4000E 01
36	1, 3.6000E 01 8, 3.1000E 01	2, 3.4150E 00 9, 1.0000E 00	3, 7.0000E-02 10, 0.	4, 5.0000E-02 11,-0.	5, 3.7000E 01 12,-0.	6, 4.1000E 01 13,-0.	7, 0.
37	1, 3.7000E 01 8, 3.2000E 01	2, 3.4150E 00 9, 1.0000E 00	3, 7.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 3.8000E 01 12,-0.	6, 4.2000E 01 13,-0.	7, 3.6000E 01
38	1, 3.8000E 01 8, 3.3000E 01	2, 3.4150E 00 9, 1.0000E 00	3, 7.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 3.9000E 01 12,-0.	6, 4.3000E 01 13,-0.	7, 3.7000E 01
39	1, 3.9000E 01 8, 3.4000E 01	2, 3.4150E 00 9, 1.0000E 00	3, 7.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 4.0000E 01 12,-0.	6, 4.4000E 01 13,-0.	7, 3.8000E 01
40	1, 4.0000E 01 8, 3.5000E 01	2, 3.4150E 00 9, 1.0000E 00	3, 7.0000E-02 10, 4.7900E 02	4, 7.5000E-02 11,-0.	5, 7.1000E 01 12,-0.	6, 4.5000E 01 13,-0.	7, 3.9000E 01
41	1, 4.1000E 01 8, 3.6000E 01	2, 3.4800E 00 9, 1.0000E 00	3, 6.0000E-02 10, 0.	4, 5.0000E-02 11,-0.	5, 4.2000E 01 12,-0.	6, 0. 13,-0.	7, 0.

42	1, 4.2000E 01 8, 3.7000E 01	2, 3.4800E 00 9, 1.0000E 00	3, 6.0000E-02 10,-0.	4, 7.5000E-02 11, 4.3500E 02	5, 4.3000E 01 12,-0.	6, 4.6000E 01 13,-0.	7, 4.1000E 01
43	1, 4.3000E 01 8, 3.8000E 01	2, 3.4800E 00 9, 1.0000E 00	3, 6.0000E-02 10,-0.	4, 7.5000E-02 11, 4.3500E 02	5, 4.4000E 01 12,-0.	6, 4.7000E 01 13,-0.	7, 4.2000E 01
44	1, 4.4000E 01 8, 3.9000E 01	2, 3.4800E 00 9, 1.0000E 00	3, 6.0000E-02 10,-0.	4, 7.5000E-02 11, 4.3500E 02	5, 4.5000E 01 12,-0.	6, 4.8000E 01 13,-0.	7, 4.3000E 01
45	1, 4.5000E 01 8, 4.0000E 01	2, 3.4900E 00 9, 1.0000E 00	3, 6.0000E-02 10, 5.4900E 02	4, 7.5000E-02 11, 0.	5, 7.6000E 01 12,-0.	6, 0. 13,-0.	7, 4.4000E 01
46	1, 4.6000E 01 8, 4.2000E 01	2, 3.5500E 00 9, 2.0000E 00	3, 8.0000E-02 10, 0.	4, 7.5000E-02 11,-0.	5, 4.7000E 01 12,-0.	6, 4.9000E 01 13, 4.3500E 02	7, 0.
47	1, 4.7000E 01 8, 4.3000E 01	2, 3.5500E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 4.8000E 01 12,-0.	6, 5.0000E 01 13, 4.3500E 02	7, 4.6000E 01
48	1, 4.8000E 01 8, 4.4000E 01	2, 3.5500E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 0. 12,-0.	6, 5.1000E 01 13, 4.3500E 02	7, 4.7000E 01
49	1, 4.9000E 01 8, 4.6000E 01	2, 3.6300E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 5.0000E 01 12,-0.	6, 0. 13, 0.	7, 0.
50	1, 5.0000E 01 8, 4.7000E 01	2, 3.6300E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 5.1000E 01 12,-0.	6, 0. 13,-0.	7, 4.9000E 01
51	1, 5.1000E 01 8, 4.8000E 01	2, 3.6300E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 7.5000E-02 11,-0.	5, 0. 12,-0.	6, 0. 13,-0.	7, 5.0000E 01
52	1, 5.2000E 01 8, 5.0000E 01	2, 3.1950E 00 9, 2.0000E 00	3, 7.0000E-02 10, 0.	4, 8.5000E-02 11, 1.6000E 00	5, 0. 12, 5.1200E 02	6, 5.3000E 01 13,-0.	7, 1.8000E 01
53	1, 5.3000E 01 8, 5.2000E 01	2, 3.2550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 7.0000E-02 11, 0.	5, 5.4000E 01 12, 7.0400E 02	6, 5.5000E 01 13, 1.6000E 00	7, 2.3000E 01
54	1, 5.4000E 01 8, 5.4000E 01	2, 3.2550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 5.0000E-02 11, 2.2000E 00	5, 0. 12, 0.	6, 5.6000E 01 13, 0.	7, 5.3000E 01
55	1, 5.5000E 01 8, 5.5000E 01	2, 3.3050E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 7.0000E-02 11, 0.	5, 5.6000E 01 12, 6.9300E 02	6, 6.3000E 01 13, 0.	7, 2.9000E 01
56	1, 5.6000E 01 8, 5.6000E 01	2, 3.3050E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 5.7000E 01 12, 0.	6, 6.4000E 01 13, 2.2000E 00	7, 5.5000E 01
57	1, 5.7000E 01 8, 5.7000E 01	2, 3.3100E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 5.8000E 01 12,-0.	6, 6.5000E 01 13, 0.	7, 5.6000E 01
58	1, 5.8000E 01 8, 5.8000E 01	2, 3.3100E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 1.1000E-01 11,-0.	5, 5.9000E 01 12,-0.	6, 6.6000E 01 13, 0.	7, 5.7000E 01
59	1, 5.9000E 01 8, 5.9000E 01	2, 3.3100E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 1.2500E-01 11,-0.	5, 6.0000E 01 12,-0.	6, 6.7000E 01 13, 2.7900E 02	7, 5.8000E 01
60	1, 5.0000E 01 8, 5.0000E 01	2, 3.3100E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 6.1000E 01 12,-0.	6, 6.8000E 01 13, 5.4438E 05	7, 5.9000E 01
61	1, 5.1000E 01 8, 5.1000E 01	2, 3.3100E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 6.2000E 01 12,-0.	6, 6.9000E 01 13, 0.	7, 6.0000E 01
62	1, 5.2000E 01 8, 5.2000E 01	2, 3.3100E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 7.0000E 01 13,-0.	7, 6.1000E 01
63	1, 5.3000E 01 8, 5.3000E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 7.0000E-02 11,-0.	5, 6.4000E 01 12, 6.8300E 02	6, 7.1000E 01 13,-0.	7, 3.5000E 01
64	1, 5.4000E 01 8, 5.4000E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 6.5000E 01 12, 0.	6, 7.2000E 01 13,-0.	7, 6.3000E 01
65	1, 5.5000E 01 8, 5.5000E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 6.6000E 01 12,-0.	6, 0. 13,-0.	7, 6.4000E 01
66	1, 5.6000E 01 8, 5.6000E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 1.1000E-01 11,-0.	5, 6.7000E 01 12,-0.	6, 0. 13,-0.	7, 6.5000E 01

67	1, 6.7000E 01 8, 5.9000E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 1.2500E-01 11,-0.	5, 6.8000E 01 12,-0.	6, 0. 13,-0.	7, 6.6000E 01
68	1, 6.8000E 01 8, 6.0000E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 6.9000E 01 12,-0.	6, 7.3000E 01 13,-0.	7, 6.7000E 01
69	1, 6.5000E 01 8, 6.1000E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 7.0000E 01 12,-0.	6, 7.4000E 01 13,-0.	7, 6.8000E 01
70	1, 7.0000E 01 8, 6.6200E 01	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 7.5000E 01 13,-0.	7, 6.9000E 01
71	1, 7.1000E 01 8, 6.3000E 01	2, 3.1450E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 7.0000E-02 11,-0.	5, 7.2000E 01 12, 4.7900E 02	6, 7.6000E 01 13,-0.	7, 4.0000E 01
72	1, 7.2000E 01 8, 6.4000E 01	2, 3.1450E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 0. 12, 0.	6, 7.7000E 01 13,-0.	7, 7.1000E 01
73	1, 7.3000E 01 8, 6.8000E 01	2, 3.0450E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 7.4000E 01 12,-0.	6, 7.8000E 01 13,-0.	7, 0.
74	1, 7.4000E 01 8, 6.9000E 01	2, 3.0450E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 7.5000E 01 12,-0.	6, 7.9000E 01 13,-0.	7, 7.3000E 01
75	1, 7.5000E 01 8, 7.0000E 01	2, 3.0450E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 8.0000E 01 13,-0.	7, 7.4000E 01
76	1, 7.6000E 01 8, 7.1000E 01	2, 3.4800E 00 9, 2.0000E 00	3, 6.0000E-02 10,-0.	4, 7.0000E-02 11,-0.	5, 7.7000E 01 12, 5.4900E 02	6, 8.1000E 01 13,-0.	7, 4.5000E 01
77	1, 7.7000E 01 8, 7.2000E 01	2, 3.4800E 00 9, 2.0000E 00	3, 6.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 0. 12, 0.	6, 8.2000E 01 13,-0.	7, 7.6000E 01
78	1, 7.8000E 01 8, 7.3000E 01	2, 3.4500E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 7.9000E 01 12,-0.	6, 0. 13,-0.	7, 0.
79	1, 7.5000E 01 8, 7.4000E 01	2, 3.4500E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 1.0000E-01 11,-0.	5, 8.0000E 01 12,-0.	6, 0. 13,-0.	7, 7.8000E 01
80	1, 8.0000E 01 9, 7.5000E 01	2, 3.4500E 00 9, 2.0000E 00	3, 4.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 0. 13,-0.	7, 7.9000E 01
81	1, 8.1000E 01 8, 7.6000E 01	2, 3.5500E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 7.0000E-02 11,-0.	5, 8.2000E 01 12,-0.	6, 8.3000E 01 13,-0.	7, 0.
82	1, 8.2000E 01 8, 7.7000E 01	2, 3.5500E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 0. 12,-0.	6, 8.4000E 01 13,-0.	7, 8.1000E 01
83	1, 8.3000E 01 8, 8.1000E 01	2, 3.6350E 00 9, 2.0000E 00	3, 9.0000E-02 10,-0.	4, 7.0000E-02 11,-0.	5, 8.4000E 01 12,-0.	6, 8.5000E 01 13,-0.	7, 0.
84	1, 8.4000E 01 8, 8.2000E 01	2, 3.6350E 00 9, 2.0000E 00	3, 9.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 0. 12,-0.	6, 8.6000E 01 13,-0.	7, 8.3000E 01
85	1, 8.5000E 01 8, 8.3000E 01	2, 3.7250E 00 9, 2.0000E 00	3, 9.0000E-02 10,-0.	4, 7.0000E-02 11,-0.	5, 8.6000E 01 12,-0.	6, 8.7000E 01 13,-0.	7, 0.
86	1, 8.6000E 01 8, 8.4000E 01	2, 3.7250E 00 9, 2.0000E 00	3, 9.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 0. 12,-0.	6, 8.8000E 01 13,-0.	7, 8.5000E 01
87	1, 8.7000E 01 8, 8.5000E 01	2, 3.8150E 00 9, 2.0000E 00	3, 9.0000E-02 10,-0.	4, 7.0000E-02 11,-0.	5, 8.8000E 01 12,-0.	6, 0. 13,-0.	7, 0.
88	1, 8.8000E 01 8, 8.6000E 01	2, 3.8150E 00 9, 2.0000E 00	3, 9.0000E-02 10,-0.	4, 6.5000E-02 11,-0.	5, 0. 12,-0.	6, 0. 13,-0.	7, 8.7000E 01
89	1, 8.9000E 01 8, 0.	2, 3.2400E 00 9, 3.0000E 00	3, 1.0000E-01 10,-0.	4, 1.2500E-01 11, 2.7900E 02	5, 9.0000E 01 12,-0.	6, 5.9000E 01 13,-0.	7, 0.
90	1, 9.0000E 01 8, 0.	2, 3.2400E 00 9, 3.0000E 00	3, 1.0000E-01 10,-0.	4, 1.0000E-01 11, 5.4438E 05	5, 0. 12,-0.	6, 6.0000E 01 13,-0.	7, 8.9000E 01
91	1, 9.1000E 01 8, 0.	2, 2.9650E 00 9, 2.0000E 00	3, 1.3000E-01 10,-0.	4, 8.0000E-02 11, 0.	5, 9.2000E 01 12,-0.	6, 9.3000E 01 13,-0.	7, 0.

92	1, 9.2000E 01 8, 0.	2, 2.9650E 00 9, 2.0000E 00	3, 1.3000E-01 10,-0.	4, 6.0000E-02 11,-0.	5, 0. 12,-0.	6, 9.4000E 01 13,-0.	7, 9.1000E 01
93	1, 9.3000E 01 8, 9.1000E 01	2, 3.0600E 00 9, 2.0000E 00	3, 6.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 9.4000E 01 12,-0.	6, 9.5000E 01 13,-0.	7, 0.
94	1, 9.4000E 01 8, 9.2000E 01	2, 3.0600E 00 9, 2.0000E 00	3, 6.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 9.6000E 01 13,-0.	7, 9.3000E 01
95	1, 9.5000E 01 8, 9.3000E 01	2, 3.1250E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 9.6000E 01 12,-0.	6, 9.7000E 01 13,-0.	7, 0.
96	1, 9.6000E 01 8, 9.4000E 01	2, 3.1250E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 9.8000E 01 13,-0.	7, 9.5000E 01
97	1, 9.7000E 01 8, 9.5000E 01	2, 3.1950E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 9.8000E 01 12,-0.	6, 9.9000E 01 13,-0.	7, 0.
98	1, 9.8000E 01 8, 9.6000E 01	2, 3.1950E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 1.0000E 02 13,-0.	7, 9.7000E 01
99	1, 9.9000E 01 8, 9.7000E 01	2, 3.2550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 1.0000E 02 12,-0.	6, 1.0100E 02 13,-0.	7, 0.
100	1, 1.0000E 02 8, 9.8000E 01	2, 3.2550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 1.0200E 02 13,-0.	7, 9.9000E 01
101	1, 1.0100E 02 8, 9.9000E 01	2, 3.3050E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 1.0200E 02 12,-0.	6, 1.0300E 02 13,-0.	7, 0.
102	1, 1.0200E 02 8, 1.0000E 02	2, 3.3050E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 1.0400E 02 13,-0.	7, 1.0100E 02
103	1, 1.0300E 02 8, 1.0100E 02	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 1.0400E 02 12,-0.	6, 1.0500E 02 13,-0.	7, 0.
104	1, 1.0400E 02 8, 1.0200E 02	2, 3.3550E 00 9, 2.0000E 00	3, 5.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 1.0600E 02 13,-0.	7, 1.0300E 02
105	1, 1.0500E 02 8, 1.0300E 02	2, 3.4150E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 1.0600E 02 12,-0.	6, 1.0700E 02 13,-0.	7, 0.
106	1, 1.0600E 02 8, 1.0400E 02	2, 3.4150E 00 9, 2.0000E 00	3, 7.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 1.0800E 02 13,-0.	7, 1.0500E 02
107	1, 1.0700E 02 8, 1.0500E 02	2, 3.4800E 00 9, 2.0000E 00	3, 6.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 1.0800E 02 12,-0.	6, 1.0900E 02 13,-0.	7, 0.
108	1, 1.0800E 02 8, 1.0600E 02	2, 3.4800E 00 9, 2.0000E 00	3, 6.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 1.1000E 02 13,-0.	7, 1.0700E 02
109	1, 1.0900E 02 8, 1.0700E 02	2, 3.5500E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 1.1000E 02 12,-0.	6, 0. 13,-0.	7, 0.
110	1, 1.1000E 02 8, 1.0800E 02	2, 3.5500E 00 9, 2.0000E 00	3, 8.0000E-02 10,-0.	4, 8.0000E-02 11,-0.	5, 0. 12,-0.	6, 0. 13,-0.	7, 1.0900E 02

ELFMFNT STARTING TEMPERATURES

1 1057.0	2 1110.0	3 1123.0	4 1163.0	5 1205.0	6 1251.0	7 1042.0	8 1157.0	9 1080.0	10 1127.0
11 1172.0	12 1223.0	13 1016.0	14 1130.0	15 1052.0	16 1100.0	17 1141.0	18 1174.0	19 1040.0	20 1053.0
21 1050.0	22 1129.0	23 1158.0	24 943.0	25 947.0	26 1054.0	27 1085.0	28 1120.0	29 1166.0	30 941.0
31 946.0	32 1053.0	33 1085.0	34 1113.0	35 1138.0	36 1058.0	37 1065.0	38 1086.0	39 1108.0	40 1132.0
41 1062.0	42 1073.0	43 1086.0	44 1101.0	45 1120.0	46 1005.0	47 1007.0	48 1009.0	49 995.0	50 987.0
51 989.0	52 1181.0	53 1179.0	54 1180.0	55 1177.0	56 1177.0	57 1179.0	58 1175.0	59 1169.0	60 1165.0
61 1163.0	62 1162.0	63 1174.0	64 1175.0	65 1176.0	66 1174.0	67 1169.0	68 1165.0	69 1163.0	70 1163.0
71 1172.0	72 1173.0	73 1164.0	74 1163.0	75 1163.0	76 1170.0	77 1171.0	78 1164.0	79 1163.0	80 1162.0
81 1169.0	82 1169.0	83 1167.0	84 1167.0	85 1166.0	86 1166.0	87 1165.0	88 1165.0	89 1107.0	90 1060.0
91 871.0	92 881.0	93 869.0	94 877.0	95 866.0	96 872.0	97 864.0	98 868.0	99 861.0	100 865.0
101 860.0	102 864.0	103 858.0	104 860.0	105 856.0	106 858.0	107 855.0	108 856.0	109 853.0	110 854.0

E1 FFMFT= 1. TYPEF=2. SURTYPF=4. NEXT=1. ITEMS READ= 9. AREA CODE=4. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= 0.1018F-04 C-P= 0.2679F 00 MU= 0.2683F-04 NU= 0.5593F-04 R-O= 0.2525E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= 0.3134F 00 RF= 0.1502E 06 PR**1/3= 0.8903F 00 H COEFF= 0.9706356F 00 COEFF*AREA= 0.6416322E-02
 E1 FFMFT= 1. TYPEF=6. SUBTYPF=2. NFXT=0. ITFMS READ=14. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 VAR.TEMP.RADIAL SFAI GAP
 T-B=1062. K-F= 0.0654F-C5 C-P= 0.2647E 00 MU= 0.2562E-04 NU= 0.4990F-04 R-AV= 0.2550E 00 GAP= 0.4333E-04 OMEGA= 1570.
 R-O= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR= 94. PLO.NRR= 0. MASS FLOW= 0.2382E-02
 RF= 0.2046F 07 PR**1/3= 0.889CF 00 RE-C= 0.6754F 07 H COEFF= 0.3961579E 00 COEFF*AREA= 0.3173645E-02
 HT.CFN.FACTOR= C.10000F 01
 E1 FFMFT= 2. TYPEF=2. SUBTYPF=4. NEXT=0. ITEMS READ= 9. AREA CODE=4. SPECIAL ARFA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= 0.1021E-04 C-P= 0.2680F 00 MU= 0.2690F-04 NU= 0.5632E-04 R-O= 0.2525E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= 0.3134F 00 RF= 0.1492F 06 PR**1/3= 0.8904F 00 H COEFF= 0.9672406F 00 COEFF*AREA= 0.6393880E-02
 E1 FFMFT= 3. TYPEF=2. SUBTYPF=4. NEXT=0. ITFMS READ= 9. AREA CODE=4. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= 0.1024F-04 C-P= 0.2682F 00 MU= 0.2696F-04 NU= 0.5664E-04 R-O= 0.2525E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= 0.3134F 00 RF= 0.1483E 06 PR**1/3= 0.8905E 00 H COEFF= 0.9643760E 00 COEFF*AREA= 0.9562416E-02
 E1 FFMFT= 4. TYPEF=2. SUBTYPF=4. NFXT=0. ITFMS READ= 9. AREA CODE=4. SPFCIAL ARFA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= 0.1033F-04 C-P= 0.2687F 00 MU= 0.2716E-04 NU= 0.5774F-04 R-O= 0.2525E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= 0.3134F 00 RF= 0.1455F 06 PR**1/3= 0.8907E 00 H COEFF= 0.9549769E 00 COEFF*AREA= 0.9469218E-02
 E1 FFMFT= 5. TYPEF=2. SURTYPF=4. NEXT=0. ITFMS READ= 9. AREA CODE=4. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= 0.1042E-04 C-P= 0.2692F 00 MU= 0.2736F-04 NU= 0.5890E-04 R-O= 0.2525E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= 0.3134F 00 RF= 0.1427F 06 PR**1/3= 0.8910F 00 H COEFF= 0.9452609F 00 COEFF*AREA= 0.9372877E-02
 E1 FFMFT= 6. TYPEF=2. SURTYPF=4. NEXT=1. ITEMS READ= 9. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1051E-04 C-P= 0.2698F 00 MU= 0.2759F-04 NU= 0.6018E-04 R-O= 0.2525E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C. RF= 0.1727F 06 PR**1/3= 0.8912E 00 H COEFF= 0.9318566E 00 COEFF*AREA= 0.7465160E-02
 E1 FFMFT= 6. SURTYPF=4. NEXT=0. ITFMS READ= 9. AREA CODE=4. SPECIAL ARFA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1051E-04 C-P= 0.2698E 00 MU= 0.2759E-04 NU= 0.6018E-04 R-O= 0.2525E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C.3134F 00 RF= 0.1396F 06 PR**1/3= 0.8912F 00 H COEFF= 0.9348986F 00 COEFF*ARFA= 0.9270129E-02
 E1 FFMFT= 12. TYPEF=2. SUBTYPF=4. NFXT=1. ITFMS READ= 9. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= 0.1045F-04 C-P= 0.2694E 00 MU= 0.2745E-04 NU= 0.5940F-04 R-O= 0.2608E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C. RF= 0.2543E 06 PR**1/3= 0.8911F 00 H COEFF= 0.9354691F 00 COEFF*AREA= 0.8928836E-02
 E1 FFMFT= 12. TYPEF=6. SUBTYPF=1. NFXT=0. ITFMS READ=12. AREA CODE=5. SPECIAL AREA= 0.23562E-02 SQ.FEET
 VAR.TEMP.JUXT FLDW, LIQUID
 T-B=1265. K-F= 0.1042E-04 C-P= 0.2693E 00 MU= 0.2732E-04 MASS FLDW= 0.5685E 01 D-HYDR= 0.3333E-02 L-LDW= 0.3125E-02
 ANN.NBR= 0. FLDW.NBR= 0. FLAG-C=0. FLAG-I=1. X-SEC= 0.3142E-03
 RE= 0.6920E 03 PR= 0.7074E 00 H COEFF= 0.3122549F-01 COEFF*ARFA= 0.7357350F-04
 E1 FFMFT= 52. TYPEF=2. SURTYPF=4. NEXT=1. ITFMS READ= 9. AREA CODE=1. SPECIAL ARFA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1036F-C4 C-P= 0.2689F 00 MU= 0.2725F-04 NU= 0.5824E-04 R-O= 0.2662F 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C.4726F 00 RF= 0.3366F 06 PR**1/3= 0.8908E 00 H COEFF= 0.9456614E 00 COEFF*AREA= 0.9228304E-02
 E1 FFMFT= 52. TYPEF=2. SUBTYPF=4. NEXT=0. ITFMS READ= 9. AREA CODE=4. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1036F-04 C-P= 0.2689F 00 MU= 0.2725F-04 NU= 0.5824F-04 R-O= 0.2633F 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C.4726F 00 RF= 0.2949F 06 PR**1/3= 0.8909F 00 H COEFF= 0.9450770F 00 COEFF*AREA= 0.1107619E-01
 E1 FFMFT= 54. TYPEF=2. SUBTYPF=4. NFXT=1. ITFMS READ= 9. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1036E-04 C-P= 0.2689E 00 MU= 0.2725E-04 NU= 0.5824E-04 R-O= 0.2712F 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C.4726F 00 RF= 0.4090E 06 PR**1/3= 0.8909E 00 H COEFF= 0.9476610E 00 COEFF*ARFA= 0.6729633E-02
 E1 FFMFT= 54. TYPEF=2. SURTYPF=4. NEXT=0. ITFMS READ= 9. AREA CODE=5. SPECIAL AREA= 0.17617E-02 SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1036E-04 C-P= 0.2689E 00 MU= 0.2725F-04 NU= 0.5824E-04 R-O= 0.2692E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C.4726E 00 RF= 0.3787E 06 PR**1/3= 0.8909E 00 H COEFF= 0.9467012E 00 COEFF*AREA= 0.1667804E-02
 E1 FFMFT= 57. TYPEF=2. SURTYPF=4. NFXT=0. ITFMS READ= 9. ARFA CODE=4. SPECIAL AREA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1036E-04 C-P= 0.2689E 00 MU= 0.2724F-04 NU= 0.5818E-04 R-O= 0.2742E 00 R-I= 0.2417E 00 OMEGA= 1570.
 V-AX= C.4726F 00 RF= 0.4524E 06 PR**1/3= 0.8908E 00 H COEFF= 0.9497571F 00 COEFF*ARFA= 0.1363408E-01
 E1 FFMFT= 58. TYPEF=2. SURTYPF=4. NFXT=0. ITFMS READ= 9. ARFA CODE=4. SPECIAL ARFA=-0. SQ.FEET
 CONCENTRIC CYL INFRS
 T-B=1300. K-F= C.1035E-04 C-P= 0.2688E 00 MU= 0.2722F-04 NU= 0.5807E-04 R-O= 0.2742F 00 R-I= 0.2283E 00 OMEGA= 1570.
 V-AX= C.9321F 00 RF= 0.6228F 06 PR**1/3= 0.8908E 00 H COEFF= 0.9274974E 00 COEFF*AREA= 0.1464599E-01

ELEMNT= 30. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. ARFA CODE=2. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1000E-01 C-P= 0.5030E 00 L-FLOW= 0.8849E 00 H COEFF= 0.5684258E-02 COEFF*AREA= 0.4191581E-04
 ELEMNT= 30. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 VAR TEMP RADIAL SFAL GAP
 T-B= 955. K-F= 0.9048E-05 C-P= 0.2611E 00 MU= 0.2423E-04 NJ= 0.1571E-03 R-AV= 0.2796E 00 GAP= 0.4333E-04 OMEGA= 1570.
 R-D= 0.2997E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.=104. FLC.NBR.= 24. MASS FLOW= 0.5954E-02
 RF= 0.7811E 06 PR*=1/3= C.8876E 00 RE-C= 0.6754E 07 H COEFF= 0.3706926E 00 COEFF*ARFA= 0.2713275E-02
 HT.GEN.FACTOR= 0.1000E 01
 ELEMNT= 36. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1000E-01 C-P= 0.5030E 00 L-FLOW= 0.2339E 00 H COEFF= 0.2150492E-01 COEFF*AREA= 0.2243075E-03
 ELEMNT= 41. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1000E-01 C-P= 0.5030E 00 L-FLOW= 0.9189E 00 H COEFF= 0.5473936E-02 COEFF*AREA= 0.4191739E-04
 ELEMNT= 41. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1000E-01 C-P= 0.5030E 00 L-FLOW= 0.2339E 00 H COEFF= 0.2150492E-01 COEFF*AREA= 0.1959231E-03
 ELEMNT= 46. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL ARFA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.2000E-01 C-P= 0.5030E 00 L-FLOW= 0.2450E 00 H COEFF= 0.4106122E-01 COEFF*AREA= 0.5088240E-03
 ELEMNT= 49. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. AREA CODE=2. SPFCL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.9608E 00 H COEFF= 0.7852831E-02 COEFF*AREA= 0.9431286E-04
 ELEMNT= 49. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL ARFA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.2000E-01 C-P= 0.5030E 00 L-FLOW= 0.2450E 00 H COEFF= 0.4106122E-01 COEFF*AREA= 0.5202905E-03
 ELEMNT= 50. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.9608E 00 H COEFF= 0.7852831E-02 COEFF*AREA= 0.9431286E-04
 ELEMNT= 51. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. ARFA CODE=1. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.5000E-02 C-P= 0.5030E 00 L-FLOW= 0.2450E 00 H COEFF= 0.1026531E-01 COEFF*AREA= 0.1300726E-03
 ELEMNT= 51. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL ARFA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.9608E 00 H COEFF= 0.7852831E-02 COEFF*AREA= 0.9431286E-04
 ELEMNT= 48. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPFCL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= 0.5000E-02 C-P= 0.5030E 00 L-FLOW= 0.2450E 00 H COEFF= 0.1026531E-01 COFFF*ARFA= 0.1272060E-03
 ELEMNT= 45. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL ARFA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.2000E-01 C-P= 0.5030E 00 L-FLOW= 0.9189E 00 H COFFF= 0.1094787E-01 COEFF*AREA= 0.1257522E-03
 ELEMNT= 81. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2361E 00 H COFFF= 0.3195680E-01 COFFF*AREA= 0.3960034E-03
 ELEMNT= 83. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPFCL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2361E 00 H COFFF= 0.3195680E-01 COEFF*AREA= 0.4561709E-03
 ELEMNT= 85. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. ARFA CODE=3. SPECIAL ARFA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2361E 00 H COFFF= 0.3195680E-01 COEFF*AREA= 0.4674653E-03
 ELEMNT= 87. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. AREA CODE=2. SPECIAL ARFA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.1010E 01 H COFFF= 0.7466601E-02 COEFF*AREA= 0.8802897E-04
 ELEMNT= 87. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2669E 00 H COFFF= 0.2867731E-01 COFFF*AREA= 0.4296282E-03
 ELEMNT= 88. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 LIQUID FILM COOLING
 T-B= 525. W/L= C.2500E-01 C-P= 0.5030E 00 L-FLOW= 0.2669E 00 H COFFF= 0.4711502E-01 COEFF*AREA= 0.7058523E-03
 ELEMNT= 88. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPFCL AREA=-0. SQ.FEET

I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.1010E 01 H COEFF= 0.746660IE-02 COEFF*AREA= 0.8174119E-04
 ELEMENT= 96. TYPE=3. SURTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 L TOUID FILM COOLING
 T-R= 525. W/L = 0.2500E-01 C-P= 0.5030E 00 L-FLOW= 0.2669E 00 H COEFF= 0.4711502E-01 COEFF*AREA= 0.6892005E-03
 ELEMENT= 84. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.2500E-01 C-P= 0.5030E 00 L-FLOW= 0.2669E 00 H COEFF= 0.4711502E-01 COEFF*AREA= 0.6725486E-03
 ELEMENT= 82. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.2500E-01 C-P= 0.5030E 00 L-FLOW= 0.2669E 00 H COEFF= 0.4711502E-01 COEFF*AREA= 0.5838417E-03
 ELEMENT= 77. TYPE=3. SURTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 L TOUID FILM COOLING
 T-R= 525. W/L = 0.2500E-01 C-P= 0.5030E 00 L-FLOW= 0.2669E 00 H COEFF= 0.4711502E-01 COEFF*AREA= 0.4292470E-03
 ELEMENT= 72. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.2500E-01 C-P= 0.5030E 00 L-FLOW= 0.2669E 00 H COEFF= 0.4711502F-01 COEFF*AREA= 0.4525801E-03
 ELEMENT= 65. TYPE=3. SURTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 L TOUID FILM COOLING
 T-R= 525. W/L = 0.1200E-01 C-P= 0.5030E 00 L-FLOW= 0.8849E 00 H COEFF= 0.6821110E-02 COEFF*AREA= 0.1005979E-03
 ELEMENT= 66. TYPE=3. SURTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1100E-01 C-P= 0.5030E 00 L-FLOW= 0.8849E 00 H COEFF= 0.6252684E-02 COEFF*AREA= 0.1014363E-03
 ELEMENT= 67. TYPE=3. SURTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1200E-01 C-P= 0.5030E 00 L-FLOW= 0.8849E 00 H COEFF= 0.6821110F-02 COEFF*AREA= 0.1257474E-03
 ELEMENT= 73. TYPE=3. SURTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1000E-01 C-P= 0.5030E 00 L-FLOW= 0.2298E 00 H COEFF= 0.2188860E-01 COEFF*AREA= 0.1454094E-03
 ELEMENT= 78. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.9084E 00 H COEFF= 0.8305812E-02 COEFF*AREA= 0.1257561E-03
 ELEMENT= 78. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1000E-01 C-P= 0.5030E 00 L-FLOW= 0.2298E 00 H COEFF= 0.2188860E-01 COEFF*AREA= 0.1317997E-03
 ELEMENT= 79. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.9084E 00 H COEFF= 0.8305812F-02 COEFF*AREA= 0.1257561E-03
 ELEMENT= 80. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2325E 00 H COEFF= 0.3245161F-01 COEFF*AREA= 0.1954037E-03
 ELEMENT= 80. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.9084F 00 H COEFF= 0.8305812E-02 COEFF*AREA= 0.1006049E-03
 ELEMENT= 75. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2325F 00 H COEFF= 0.3245161E-01 COEFF*AREA= 0.2155812E-03
 ELEMENT= 70. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2325F 00 H COEFF= 0.3245161F-01 COEFF*AREA= 0.2375287E-03
 ELEMENT= 62. TYPE=3. SUBTYPE=3. NEXT=1. ITEMS READ= 4. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1500E-01 C-P= 0.5030E 00 L-FLOW= 0.2325F 00 H COEFF= 0.3245161E-01 COEFF*AREA= 0.1874742E-03
 ELEMENT= 62. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=4. SPECIAL AREA=-0. SQ.FEET
 I TOUID FILM COOLING
 T-R= 525. W/L = 0.1000E-01 C-P= 0.5030E 00 L-FLOW= 0.8613F 00 H COEFF= 0.5840C09E-02 COEFF*AREA= 0.6706822E-04
 ELEMENT= 61. TYPE=3. SUBTYPE=3. NEXT=0. ITEMS READ= 4. AREA CODE=4. SPECIAL AREA=-0. SQ.FEET
 L TOUID FILM COOLING
 T-R= 525. W/L = 0.5000E-02 C-P= 0.5030E 00 L-FLOW= 0.8613E 00 H COEFF= 0.2920005E-02 COEFF*AREA= 0.4191764E-04
 ELEMENT= 11. TYPE=6. SUBTYPE=1. NEXT=0. ITEMS READ=12. AREA CODE=5. SPECIAL AREA= 0.16115E-02 SQ.FEET

VAR.TEMP.DUCT FLOW, LIQUID
 T-B=1255. K-F= 0.103E-04 C-P= 0.268E 00 MU= 0.2721E-04 MASS FLOW= 0.5685E 01 D-HYDR= 0.3333E-02 L-LOW= 0.7835E-02
 ANN.NBR.= 0. FLJW NBR= 12. FLAG-C=0. FLAG-I=1. X-SEC= 0.3142E-03
 RE= 0.6965E 03 PR= 0.7069E 00 H COEFF= 0.2280963E-01 COEFF*AREA= 0.3675772E-04
 ELEMENT= 17. TYPE=6. SUBTYPE=1. NEXT=0. ITEMS READ=12. AREA CODE=5. SPECIAL AREA= 0.16115E-02 SQ.FEET

 VAR.TEMP.DUCT FLOW, LIQUID
 T-B=1240. K-F= 0.1028E-04 C-P= 0.2684E 00 MU= 0.2705E-04 MASS FLOW= 0.5685E 01 D-HYDR= 0.3333E-02 L-LOW= 0.1133E-01
 ANN.NBR.= 0. FLJW NBR= 11. FLAG-C=0. FLAG-I=1. X-SEC= 0.3142E-03
 RE= 0.7006E 03 PR= 0.7064E 00 H COEFF= 0.1982752E-01 COEFF*AREA= 0.3195205E-04
 ELEMENT= 16. TYPE=6. SUBTYPE=1. NEXT=0. ITEMS READ=12. AREA CODE=5. SPECIAL AREA= 0.23562E-02 SQ.FEET

 VAR.TEMP.DUCT FLOW, LIQUID
 T-B=1210. K-F= 0.1019E-04 C-P= 0.2679E 00 MU= 0.2685E-04 MASS FLOW= 0.5685E 01 D-HYDR= 0.3333E-02 L-FLOW= 0.1643E-01
 ANN.NBR.= 0. FLJW NBR= 17. FLAG-C=0. FLAG-I=1. X-SEC= 0.3142E-03
 RE= 0.7057E 03 PR= 0.7059E 00 H COEFF= 0.1755946E-01 COEFF*AREA= 0.4160923E-04
 ELEMENT= 15. TYPE=6. SUBTYPE=1. NEXT=0. ITEMS READ=12. AREA CODE=5. SPECIAL AREA= 0.15087E-02 SQ.FEET

 VAR.TEMP.DUCT FLOW, LIQUID
 T-B=1180. K-F= 0.1009E-04 C-P= 0.2673E 00 MU= 0.2661E-04 MASS FLOW= 0.5685E 01 D-HYDR= 0.3333E-02 L-FLOW= 0.2103E-01
 ANN.NBR.= 0. FLJW NBR= 16. FLAG-C=0. FLAG-I=1. X-SEC= 0.3142E-03
 RE= 0.7121E 03 PR= 0.7053E 00 H COEFF= 0.1514910E-01 COEFF*AREA= 0.2435057E-04
 ELEMENT= 20. TYPE=6. SUBTYPE=1. NEXT=0. ITEMS READ=12. AREA CODE=5. SPECIAL AREA= 0.15087E-02 SQ.FEET

 VAR.TEMP.DUCT FLOW, LIQUID
 T-B=1150. K-F= 0.1009E-04 C-P= 0.2673E 00 MU= 0.2661E-04 MASS FLOW= 0.5685E 01 D-HYDR= 0.3333E-02 L-FLOW= 0.2497E-01
 ANN.NBR.= 0. FLJW NBR= 15. FLAG-C=0. FLAG-I=1. X-SEC= 0.3142E-03
 RE= 0.7121E 03 PR= 0.7053E 00 H COEFF= 0.1524155E-01 COEFF*AREA= 0.2299492E-04
 ELEMENT= 19. TYPE=6. SUBTYPE=1. NEXT=0. ITEMS READ=12. AREA CODE=5. SPECIAL AREA= 0.15708E-02 SQ.FEET

 VAR.TEMP.DUCT FLOW, LIQUID
 T-B=1150. K-F= 0.1009E-04 C-P= 0.2671E 00 MU= 0.2655E-04 MASS FLOW= 0.5685E 01 D-HYDR= 0.3333E-02 L-FLOW= 0.2848E-01
 ANN.NBR.= 0. FLJW NBR= 20. FLAG-C=0. FLAG-I=1. X-SEC= 0.3142E-03
 RE= 0.7137E 03 PR= 0.7051E 00 H COEFF= 0.1555088E-01 COEFF*AREA= 0.2287223E-04
 ELEMENT= 7. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=3. SPECIAL AREA=-0. SQ.FEET

 VAR.TEMP.RADIAL SEAL GAP
 T-B= 975. K-F= C.9729F-05 C-P= C.2628E 00 MU= 0.2488E-04 NU= 0.4696E-04 R-AV= 0.2604E 0C GAP= 0.4333E-04 OMEGA= 1570.
 R-N= 0.2992F 00 FLAG-C=0. FLAG-I=1. ANN.NBR.= 96. FLO.NBR.= 1. MASS FLOW= 0.2382F-02
 RE= 0.2267F 07 PR**1/3= C.8883E 00 RE-C= 0.6754F 07 H COEFF= 0.3824877E 00 COEFF*AREA= 0.3650757E-02
 HT.GEN.FACTOR= 0.10000E 01
 ELEMENT= 13. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=5. SPECIAL AREA= 0.16805E-01 SQ.FEET

 VAR.TEMP.RADIAL SEAL GAP
 T-B= 945. K-F= 0.9431E-05 C-P= C.2634E 00 MU= 0.2511E-04 NU= 0.4919E-04 R-AV= 0.2675E 0C GAP= 0.9152E-03 OMEGA= 1570.
 R-N= 0.2992F 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 98. FLO.NBR.= 7. MASS FLOW= 0.2382E-02
 RE= 0.2294F 07 PR**1/3= C.8885F 00 RE-C= 0.2278E 06 H COEFF= 0.2927813E 00 COEFF*AREA= 0.4920307E-02
 HT.GEN.FACTOR= 0.19315E 01
 ELEMENT= 24. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=5. SPECIAL AREA= 0.14366E-01 SQ.FEET

 VAR.TEMP.RADIAL SEAL GAP
 T-B=1005. K-F= 0.9170E-05 C-P= C.2618F 00 MU= 0.2451F-04 NU= 0.2928E-04 R-AV= 0.2744E 00 GAP= 0.1078E-02 OMEGA= 1570.
 R-N= 0.2952F 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 102. FLO.NBR.= 100. MASS FLOW= 0.5954E-02
 RE= 0.4037F 07 PR**1/3= 0.8879E 00 RE-C= 0.1900F 06 H COEFF= 0.4274941E 00 COEFF*AREA= 0.6141509F-02
 HT.GEN.FACTOR= 0.18512F 01
 ELEMENT= 92. TYPE=5. SUBTYPE=C. NEXT=0. ITEMS READ= 2. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

 SPECIFIC COEFFICIENT
 T-B=1300. H COFFF= C.1380662E-02 COFFF*AREA= 0.2322056E-04
 ELEMENT= 110. TYPE=5. SUBTYPE=0. NEXT=1. ITEMS READ= 2. AREA CODE=2. SPECIAL AREA=-0. SQ.FEET

 SPECIFIC COEFFICIENT
 T-B= 535. H COEFF= C.3733100F-04 COEFF*AREA= 0.4678121E-06
 ELEMENT= 110. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

 VAR.TEMP.RADIAL SEAL GAP
 T-B= 900. K-F= C.8707E-05 C-P= 0.2590E 00 MU= 0.2345F-04 NU= 0.8278E-03 R-AV= 0.2958E 00 GAP= 0.8375E-02 OMEGA= 1570.
 R-N= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 0. FLO.NBR.= 108. MASS FLOW= 0.5954E-02
 RE= 0.1659F 06 PR**1/3= 0.8869E 00 RE-C= 0.1947F 05 H COEFF= 0.2106143E-01 COEFF*AREA= 0.2609898E-03
 HT.GEN.FACTOR= 0.16334E 01
 ELEMENT= 94. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

 VAR.TEMP.RADIAL SEAL GAP
 T-B=1067. K-F= 0.9147E-05 C-P= 0.2617E 00 MU= 0.2446E-04 NU= 0.4423E-04 R-AV= 0.2550E 00 GAP= 0.4333E-04 OMEGA= 1570.
 R-N= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 1. FLO.NBR.= 0. MASS FLOW= 0.2382E-02
 RE= 0.2306F 07 PR**1/3= 0.8878F 00 RE-C= 0.6754E 07 H COEFF= 0.3748462E 00 COEFF*AREA= 0.3002915E-02
 HT.GEN.FACTOR= 0.10000E 01
 ELEMENT= 96. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

 VAR.TEMP.RADIAL SEAL GAP
 T-B= 975. K-F= 0.8929F-05 C-P= 0.2604E 00 MU= 0.2396E-04 NU= 0.4261E-04 R-AV= 0.2604E 00 GAP= 0.4333E-04 OMEGA= 1570.
 R-N= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 7. FLO.NBR.= 94. MASS FLOW= 0.2382E-02
 RE= 0.2494F 07 PR**1/3= 0.8874F 00 RE-C= 0.6754E 07 H COEFF= 0.3657236E 00 COEFF*AREA= 0.3490747E-02
 HT.GEN.FACTOR= 0.10CCCC 01
 ELEMENT= 98. TYPE=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

VAR.TEMP.RADIAL SFAL GAP
 T-R= 945. K-F= 0.8847E-05 C-P= 0.2599E 00 MU= 0.2377E-04 NU= 0.4245E-04 R-AV= 0.2663E 00 GAP= 0.4333E-04 OMEGA= 1570.
 R-D= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 13. FL0.NBR.= 96. MASS FLOW= 0.2382E-02
 RF= 0.2623E 07 PR**1/3= 0.8872E 00 RE-C= 0.6754E 07 H COEFF= 0.362305E 00 COEFF*AREA= 0.3535583E-02
 HT.GEN.FACTOR= 0.1000CF 01

EL FMENT=100. TYPF=6. SUBTYPE=2. NEXT=0. ITEMS READ=14. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

VAR.TEMP.RADIAL SFAL GAP
 T-R=10E0. K-F= 0.2614E 00 C-P= 0.2614E-05 MU= 0.2433E-04 NU= 0.4552E-04 R-AV= 0.2713E 00 GAP= 0.42C8E-02 OMEGA= 1570.
 R-D= 0.2992E 00 FLAG-C=1. FLAG-I=0. ANN.NBR.= 0. FL0.NBR.= 98. MASS FLOW= 0.5954E-02
 RF= 0.2539E 07 PR**1/3= 0.8877E 00 RE-C= 0.4183E 05 H COEFF= 0.2351904E 00 COEFF*AREA= 0.1670160E-02
 HT.GEN.FACTOR= 0.1PP6E 01

COMBINED FLOW ELEMENT, CONDUCTION NO.= 100 FLOW FROM CCND.ELEMENTS 98 AND 19

FI FMENT=102. TYPF=6. SURTYPF=2. NEXT=0. ITEMS READ=14. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

VAR.TEMP.RADIAL SFAL GAP
 T-R=10C5. K-F= 0.9891E-05 C-P= 0.26C7E 00 ML= 0.2408E-04 MU= 0.5563E-04 R-AV= 0.2754E 00 GAP= 0.4333E-04 OMEGA= 1570.
 R-D= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 24. FL0.NBR.=100. MASS FLOW= 0.5954E-02
 RF= 0.2141E 07 PR**1/3= 0.8875E 00 RE-C= 0.6754E 07 H COEFF= 0.3679046E 00 COEFF*AREA= 0.2652736E-02
 HT.GEN.FACTOR= 0.1000CF 01

FL FMENT=104. TYPF=6. SUBTYPF=2. NEXT=0. ITEMS READ=14. AREA CODE=1. SPECIAL ARFA=-0. SQ.FEET

VAR.TEMP.RADIAL SFAL GAP
 T-B= 955. K-F= 0.2599E-05 C-P= 0.2599E 00 MU= 0.2378E-04 NU= 0.1497E-03 R-AV= 0.2796E 00 GAP= 0.4333E-04 OMEGA= 1570.
 R-D= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 30. FL0.NBR.=102. MASS FLOW= 0.5954E-02
 RF= 0.2197E 06 PR**1/3= 0.8872E 00 RE-C= 0.6754E 07 H COEFF= 0.3625071E 00 COEFF*AREA= 0.2653361E-02
 HT.GEN.FACTOR= 0.10000E 01

FL FMENT=106. TYPF=6. SUBTYPF=2. NXFT=0. ITEMS READ=14. AREA CODE=1. SPECIAL AREA=-0. SQ.FEET

VAR.TEMP.RADIAL SEAL GAP
 T-B= 925. K-F= 0.8799E-05 C-P= 0.2596E 00 MU= 0.2366E-04 NU= 0.8472E-03 R-AV= 0.2846E 00 GAP= 0.42C8E-02 OMEGA= 1570.
 R-D= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 0. FL0.NBR.=104. MASS FLOW= 0.5954E-02
 RF= 0.1501E 06 PR**1/3= 0.8871E 00 RF-C= 0.4183E 05 H COEFF= 0.2275467E-01 COEFF*AREA= 0.2373432E-03
 HT.GEN.FACTOR= 0.17420E 01

FL FMENT=108. TYPF=6. SUBTYPF=2. NXFT=0. ITEMS READ=14. AREA CODE=1. SPECIAL ARFA=-0. SQ.FEET

VAR.TEMP.RADIAL SFAL GAP
 T-B= 915. K-F= 0.8746E-05 C-P= 0.2593E 00 MU= 0.2354E-04 NU= 0.8360E-03 R-AV= 0.2900E 00 GAP= 0.4208E-02 OMEGA= 1570.
 R-D= 0.2992E 00 FLAG-C=0. FLAG-I=2. ANN.NBR.= 0. FL0.NBR.=106. MASS FLOW= 0.5954E-02
 RF= 0.1579E 06 PR**1/3= 0.8870E 00 RF-C= 0.4183E 05 H COEFF= 0.2318910E-01 COEFF*ARFA= 0.2112670E-03
 HT.GEN.FACTOR= 0.16882E 01

BOUNDARY COEFFICIENT MATRIX -(H*A)BTU/F.SEC AND (H*A*T-B) OR H*C-P BTU/SEC

BNDY	COND.	FIXED FLUX	FORCED CONVECTION	FREE CONVECTION	RADIATION	VAR.TEMP.CONVECTION			
F M	F E	W	H*A	H*A*T-B	H*A	H*A*T-E	H*A	H*C-P	
1	1	0.	0.64163F-02	0.83412E 01	0.	0.	0.	0.31736F-02	0.63061E-03
2	2	0.	0.63939F-02	0.83120E 01	0.	0.	0.	0.	0.
3	3	0.	0.95624F-02	0.12431E 02	0.	0.	0.	0.	0.
4	4	0.	0.94652F-02	0.12310E 02	0.	0.	0.	0.	0.
5	5	0.	0.93729F-02	0.12185E 02	0.	0.	0.	0.	0.
6	6	0.	0.16735F-02	0.21756E 02	0.	0.	0.	0.	0.
7	12	0.	0.89288F-02	0.11607E 02	0.	0.	0.	0.	0.
8	52	0.	0.20304E-01	0.26396E 02	0.	0.	0.	0.	0.
9	54	0.	0.83974F-02	0.10917E 02	0.	0.	0.	0.	0.
10	57	0.	0.13634E-01	0.17724E 02	0.	0.	0.	0.	0.
11	58	0.	0.14646F-01	0.19040E 02	0.	0.	0.	0.	0.
12	20	0.	0.	0.	0.	0.	0.	0.27133E-02	0.15546E-02
13	26	0.	0.	0.	0.	0.	0.	0.	0.
14	41	0.	0.	0.	0.	0.	0.	0.	0.
15	46	0.	0.	0.	0.	0.	0.	0.	0.
16	49	0.	0.	0.	0.	0.	0.	0.	0.
17	50	0.	0.	0.	0.	0.	0.	0.	0.
18	51	0.	0.	0.	0.	0.	0.	0.	0.
19	48	0.	0.	0.	0.	0.	0.	0.	0.
20	45	0.	0.	0.	0.	0.	0.	0.	0.
21	81	0.	0.	0.	0.	0.	0.	0.	0.
22	83	0.	0.	0.	0.	0.	0.	0.	0.
23	85	0.	0.	0.	0.	0.	0.	0.	0.
24	87	0.	0.	0.	0.	0.	0.	0.	0.
25	88	0.	0.	0.	0.	0.	0.	0.	0.
26	86	0.	0.	0.	0.	0.	0.	0.	0.
27	84	0.	0.	0.	0.	0.	0.	0.	0.
28	82	0.	0.	0.	0.	0.	0.	0.	0.
29	77	0.	0.	0.	0.	0.	0.	0.	0.
30	72	0.	0.	0.	0.	0.	0.	0.	0.
31	65	0.	0.	0.	0.	0.	0.	0.	0.
32	66	0.	0.	0.	0.	0.	0.	0.	0.
33	67	0.	0.	0.	0.	0.	0.	0.	0.
34	73	0.	0.	0.	0.	0.	0.	0.	0.
35	78	0.	0.	0.	0.	0.	0.	0.	0.
36	79	0.	0.	0.	0.	0.	0.	0.	0.
37	80	0.	0.	0.	0.	0.	0.	0.	0.
38	75	0.	0.	0.	0.	0.	0.	0.	0.
39	70	0.	0.	0.	0.	0.	0.	0.	0.
40	62	0.	0.	0.	0.	0.	0.	0.	0.
41	61	0.	0.	0.	0.	0.	0.	0.	0.

42	11	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
43	17	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
44	16	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
45	15	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
46	20	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
47	19	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
48	7	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
49	13	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
50	24	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
51	92	-0.10299E 00	0.23221E-04	0.30187E-01	0.	0.	0.	0.	0.	0.	0.	0.	0.
52	110	0.	0.46781E-06	0.25028E-03	0.	0.	0.	0.	0.	0.	0.	0.	0.
53	94	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
54	96	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
55	98	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
56	100	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
57	102	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
58	104	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
59	106	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
60	108	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
61	91	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
62	93	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
63	95	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
64	97	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
65	99	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
66	101	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
67	103	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
68	105	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
69	107	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
70	109	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
71	89	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
72	90	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.

VAR TEMP CONVECTION DIMENSIONLESS COEFFICIENTS (H*A/W*C-P)

1	1,	5.0327E 00	2	12,	1.5299E-01	3	30,	1.7453E 00	4	11,	7.6561E-02	5	17,	6.6650E-02	6	15,	8.5960E-02
7	15,	5.1017E-02	8	20,	4.8167E-02	9	19,	4.7337E-02	10	7,	5.8320E 00	11	13,	7.8418E 00	12	24,	3.9393E -03
13	110,	1.6921E-01	14	94,	4.8172E 00	15	96,	5.6280E 00	16	98,	5.7110E 00	17	100,	1.0733E 00	18	102,	1.7089E 00
19	104,	1.7145E 00	20	106,	1.5355E-01	21	138,	1.3695E-01									

FLUID SHEAR HEAT GENERATION, BTU/SEC

1	1,	3.0329E-02	2	12,	0.	3	30,	3.1501E-02	4	11,	0.	5	17,	0.	6	16,	0.
7	15,	0.	8	20,	0.	9	19,	0.	10	7,	3.6591E-02	11	13,	3.6094E-03	12	24,	2.2674E-03
13	110,	4.8837E-04	14	94,	2.8952E-02	15	96,	3.5241E-02	16	98,	3.7368E-02	17	100,	5.6112E-04	18	102,	2.9926E-02
19	104,	3.0920E-02	20	106,	8.1461E-04	21	138,	7.1239E-04									

DATA TIME= 0.130E MINUTES

CONDUCT.ELEMENT NO.	1	VAR TEMP ELEMENT NO.	1	FLOW CODE=	2
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CONDUCT.ELEMENT NO.	30	VAR.TEMP.ELEMENT NO.	3	FLOW CODE=	2
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CONDUCT.ELEMENT NO.	15	VAR TEMP ELEMENT NO.	7	FLOW CODE=	1
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CONDUCT.ELEMENT NO.	7	VAR TEMP ELEMENT NO.	10	FLOW CODE=	2
CONDUCT.ELEMENT NO.	13	VAR TEMP ELEMENT NO.	11	FLOW CODE=	2
CONDUCT.ELEMENT NO.	24	VAR TEMP ELEMENT NO.	12	FLOW CODE=	2
CONDUCT.ELEMENT NO.	110	VAR TEMP ELEMENT NO.	13	FLOW CODE=	2
CONDUCT.ELEMENT NO.	94	VAR TEMP ELEMENT NO.	14	FLOW CODE=	2
CONDUCT.ELEMENT NO.	96	VAR TEMP ELEMENT NO.	15	FLOW CODE=	2
CONDUCT.ELEMENT NO.	98	VAR TEMP ELEMENT NO.	16	FLOW CODE=	2
COMBINED FLOWS ELEMENT COMBINATION NO.	1	CONDUCT.NO.=100	BNDRY.NO.= 17	PREVIOUS ELEMENT VAR TEMP.NOS.=	16 AND 9
CONDUCT.ELEMENT NO.	102	VAR TEMP ELEMENT NO.	17	FLOW CODE=	2
CONDUCT.ELEMENT NO.	104	VAR TEMP ELEMENT NO.	18	FLOW CODE=	2
CONDUCT.ELEMENT NO.	106	VAR TEMP ELEMENT NO.	19	FLOW CODE=	2
CONDUCT.ELEMENT NO.	108	VAR TEMP ELEMENT NO.	20	FLOW CODE=	2

APPENDIX D

HEAT TRANSFER COEFFICIENT EQUATIONS

The equations used to calculate boundary heat transfer coefficients are mostly obtained from books by McAdams (ref. 9) and by Kreith (ref. 10).

Radiation

The radiation equation is based on information from chapter 4 of Kreith and chapter 5 of McAdams. The basic expression is in terms of the heat flux but can also be expressed as

$$h = \frac{Q}{A \Delta T}$$

The number of properties required is reduced by substitution of others as explained in the references.

Liquid Film Cooling

The gravity-flow liquid film cooling equation can be found in chapter 9 of McAdams. Strictly, it applies only to flow over horizontal cylinders. However, in the program, it is also used for flow down vertical surfaces.

Other Free Convection Coefficients

The two other free convection subtype expressions are obtained from a study of chapter 7 of McAdams and of chapter 7 of Kreith. They are actually for nonenclosed spaces, but are considered acceptable for two reasons. First, the boundaries at which free convection occurs are far enough from the parts of interest (seal plate and nosepiece) that they have little influence. Second, the knowledge of coefficients in enclosed spaces appears to be limited and to be expressed in terms of overall coefficients.

Comparison of the two conditions (table I) shows the equations for turbulent flow are identical and those for laminar flow differ only in the constant used. Transition from laminar to turbulent flow is considered to occur at $GrPr = 10^9$ (ref. 9).

Use of Local Coefficients

The expression for free convection at vertical surfaces is for a local coefficient instead of an average as is the case for the other cases already mentioned.

The program deals with small sections of boundary surfaces. There are few, if any, places where a fully established velocity profile (e.g., in duct flow) or boundary film (e.g., in flat plate flow) exists in seal applications. In the problem of appendix C, as an example, the use of a local coefficient is generally preferable.

While free convection around a horizontal cylinder should properly be considered a circumferential flow, the assumption of an axisymmetric temperature distribution implies a uniform coefficient around the circumference as well as along the cylinder.

The conversion of average coefficients to local coefficients is based on text and equations in chapter 6 of Kreith.

Flat Plate

These coefficients and the critical Reynolds number for laminar turbulent transition are obtained directly from chapter 6 of Kreith's book.

Duct Flow, Liquid

For the most accurate result, the equation used for duct flow depends on the shape of the cross section and on the viscosity of the fluid. However, McAdams and also Jakob (ref. 11) indicate that the use of pipe flow equations with an equivalent (hydraulic) diameter is acceptable.

In the example of appendix C, the only fluid flowing in a duct is a synthetic oil with a viscosity in the range covered by McAdams recommended equation for turbulent flow. The laminar flow expression as well as that for turbulent flow are taken from chapter 9 of McAdams.

McAdams' data indicate that transition from laminar to turbulent flow can be considered as occurring over the Reynolds number range between 2500 and 7500. Kreith and also Jakob agree with the overall trend during transition. The equation presented in table I seems to be an acceptable approximation of the coefficient in this range.

Concentric Cylinders

This expression is obtained from reference 12. The experimental conditions are similar to those found in the problem of appendix C. One assumption is made in the problem; the axial flow has a negligible effect on the boundary film. This seems reasonable for the high rotational speed and the low axial flow velocities. Therefore, the entrance effect term is dropped.

Rotors

The equations for the remaining two flow types are derived from the results of reference 13. While the completely shrouded disk used does not duplicate the flow in a seal gap, no work applicable to laminar flow (the most probable regime in a seal gap) has yet been found. Also the derivation involves using the Reynolds analogy so the resulting expressions are only rough approximations.

In applying the results, the assumption is made that one or the other of the following situations exists:

- (1) The clearance between the side of a rotating part and the housing or other stationary part is so small that the boundary layers are merged at all times (seal gap).
- (2) The clearance is large enough that the boundary layers are separate at all times (sides of rotors). This should be a good approximation of the situation in the problem of appendix C except for the seal gap.

The laminar to turbulent transition for the sides of rotors case occurs at a Reynolds number of 158 000. For the seal gap case, the critical Reynolds number is a function of the ratio of gap clearance to rotor outer radius, that is,

$$Re_c = \frac{366.34}{\left(\frac{s}{r_o}\right)^{1019}}$$

Derivation of Equations for the Rotor Coefficients

The Reynolds analogy (ref. 14)

$$Nu = \frac{C_f Re Pr^{1/3}}{2} \quad (D1)$$

requires an expression for the wall shear stress τ_t because the skin friction coefficient

$$C_f = \frac{2\tau_t}{\rho V_\infty^2} \quad (D2)$$

The torque coefficients C_M obtained in reference 13 are, in effect, functions of τ_t ; that is

$$C_M = \frac{8\pi}{\rho \omega^2 a^5} \int_0^a r^2 \tau_t dr \quad (D3)$$

A general form of the equation for shear stress in a pipe (ref. 14, p. 509)

$$\tau_t = A \rho^V \omega^W r^X \nu^Y s^Z \quad (D4)$$

is used to obtain the following expression for the torque coefficient:

$$C_M = \frac{8\pi A}{3 + X} \frac{\rho^{V-1} \nu^Y s^Z}{\omega^{2-W} a^{2-X}} \quad (D5)$$

This is matched with an empirical equation from reference 13 to evaluate the constant A and the coefficients of the properties. Substitution in equations (D4), (D2), and (D1) gives an expression for the Nusselt number. The heat transfer coefficient h is a factor of the Nusselt number; that is,

$$Nu = \frac{hr_{av}}{k}$$

The free stream velocity V_∞ must still be evaluated. For the seal gap with merged boundary layers, $V_\infty = r\omega/2$. For the case of separated boundary layers, the difference between the free stream velocity and the rotor velocity is required for a rotating part. For a nonrotating part, of course, the difference is the free stream velocity $V_\infty = \beta r$. Information in reference 13 indicates that β is a function of the rotor angular velocity and the ratio s/a , or that $\beta = K\omega$ where $K = F(s/a)$. Evaluating the data presented yields the following expressions for K (the coefficient equation can be expressed in terms of K , see table I):

$$\left. \begin{array}{l} K_{\text{stator}} = 0.50185 - 0.6508 \left(\frac{s}{a} \right) \\ K_{\text{rotor}} = 0.49815 + 0.6508 \left(\frac{s}{a} \right) \end{array} \right\} \text{laminar flow}$$

$$\left. \begin{array}{l} K_{\text{stator}} = 0.48558 - 0.35778 \left(\frac{s}{a} \right) \\ K_{\text{rotor}} = 0.51442 + 0.35778 \left(\frac{s}{a} \right) \end{array} \right\} \text{turbulent flow}$$

APPENDIX E

SAMPLE THERMAL PROBLEM FOR COMPARISON WITH EXACT SOLUTION

To demonstrate the accuracy of the program, the following sample problem (see fig. 15) was solved.

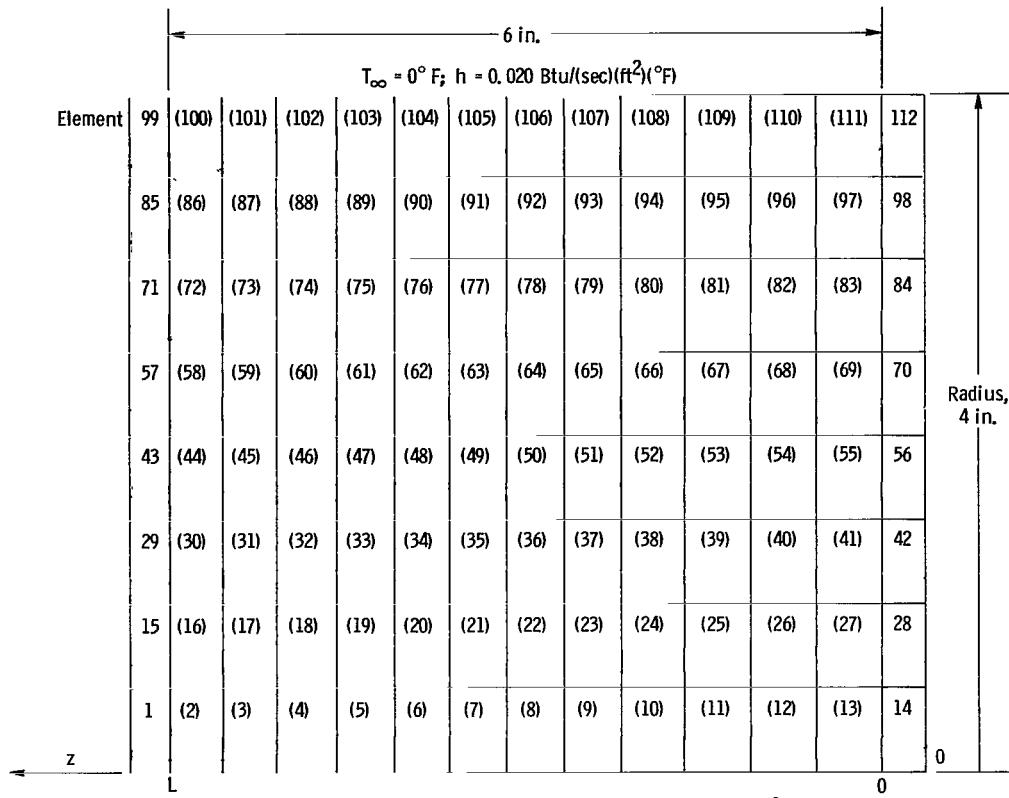


Figure 15. - Thermal sample problem. Solid cylinder with right end ($z = L$) held at 200° F and left end ($z = 0$) held at 0° F . Right side boundary elements (i.e., 14, 28, 42, 56, 70, 84, 98, and 112) held at 200° F . Left side elements held at 0° F .

For the finite cylinder with $0 \leq r \leq a$ and $0 \leq z \leq L$,

$$z = 0 \text{ held at } 200^{\circ}\text{ F (366 K)}$$

$$z = L \text{ held at } 0^{\circ}\text{ F (255 K)}$$

Forced convection into a medium at $T_{\infty} = 0^{\circ}\text{ F (255 K)}$ occurs at $r = a$.

For an exact solution, the temperature has to satisfy the following equation for an isotropic homogeneous solid:

$$\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial z^2} = 0 \quad 0 \leq r \leq a, \quad 0 \leq z \leq L$$

which is subject to the following boundary conditions:

$$T = 0^\circ F (255 K) \text{ at } z = L \text{ and } 0 \leq r \leq a$$

$$T = 200^\circ F (366 K) \text{ at } z = 0 \text{ and } 0 \leq r \leq a$$

$$k \frac{\partial T}{\partial r} + h T = 0 \text{ at } r = a \text{ and } 0 < z < L$$

If the following definitions are used:

J_0 Bessel function of first kind, zero order

J'_0 derivative with respect to its arguments

α root of equation $\alpha J'_0(\alpha a) + h_c J_0(\alpha a) = 0$

the exact solution is given by

$$T = T_\infty \sum_{n=1}^{\infty} \frac{2h_c J_0(r \alpha_n) \sinh[(L - z)\alpha_n]}{a h_c^2 + \alpha_n^2 J_0(a \alpha_n) \sinh(L \alpha_n)} \quad (E1)$$

For the numerical solution, a coarse mesh of 112 elements was chosen. As indicated in figure 15, the 96 elements between $z = 0$ and $z = L$ had 0.5-inch (1.27-cm) radial and axial dimensions. The 16 elements constituting boundary conditions had 0.25-inch (0.635-cm) axial dimensions.

The temperatures were calculated by means of the program and of equation (E1). The following values were required to obtain solutions:

$$a = 4.0 \text{ in. (10 cm)}$$

$$h_c = 0.020 \text{ Btu/(sec)(ft}^2\text{)(}^{\circ}\text{F}); 0.0098 \text{ cal/(sec)(cm}^2\text{)(}^{\circ}\text{C)}$$

$$L = 6.0 \text{ in. (15 cm)}$$

$$k = 0.00361 \text{ Btu/(sec)(ft)(}^{\circ}\text{F}); 0.0537 \text{ cal/(sec)(cm)(}^{\circ}\text{C)}$$

The results are shown in figure 16 and table III. The maximum error using this coarse mesh is 15 percent. A finer mesh would be expected to show a lesser error.

(Element)	(99)	(100)	(101)	(102)	(103)	(104)	(105)	(106)	(107)	(108)	(109)	(110)	(111)	(112)
Exact solution	0	2.71	8.23	14.09	20.55	27.90	36.50	46.81	59.50	75.54	96.55	125.55	169.61	200
Program solution	0	2.57	7.26	12.94	19.22	26.41	34.90	45.17	57.91	74.15	95.52	124.98	163.09	200
	(85)	(86)	(87)	(88)	(89)	(90)	(91)	(92)	(93)	(94)	(95)	(96)	(97)	(92)
0	3.23	9.81	16.80	24.48	33.19	43.33	55.42	70.11	88.35	111.44	141.15	178.86	200	3.11
	(71)	(72)	(73)	(74)	(75)	(76)	(77)	(78)	(79)	(80)	(81)	(82)	(83)	(84)
0	3.70	11.23	19.21	27.95	37.82	49.23	62.66	78.72	98.13	121.68	149.99	182.68	200	3.55
	(57)	(58)	(59)	(60)	(61)	(62)	(63)	(64)	(65)	(66)	(67)	(68)	(69)	(70)
0	4.10	12.45	21.27	30.90	41.71	54.09	68.49	85.39	105.30	128.59	155.30	184.74	200	3.92
	(43)	(44)	(45)	(46)	(47)	(48)	(49)	(50)	(51)	(52)	(53)	(54)	(55)	(56)
0	4.43	13.44	22.94	33.28	44.80	57.90	72.95	90.34	110.38	133.22	158.65	185.99	200	4.21
	(29)	(30)	(31)	(32)	(33)	(34)	(35)	(36)	(37)	(38)	(39)	(40)	(41)	(42)
0	4.67	14.19	24.20	35.06	47.10	60.69	76.16	93.82	113.84	136.25	160.77	186.77	200	4.41
	(15)	(16)	(17)	(18)	(19)	(20)	(21)	(22)	(23)	(24)	(25)	(26)	(27)	(28)
0	4.84	14.69	25.04	36.24	48.62	62.52	78.23	96.02	115.99	138.10	162.03	187.22	200	4.53
	(1)	(2)	(3)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)	(13)	(14)
0	4.93	14.94	25.47	36.83	49.37	63.42	79.25	97.08	117.02	138.97	162.62	187.41	200	4.57
	12.68	22.47	33.15	45.11	58.75	74.45	92.55	113.27	136.63	162.31	186.14			

Figure 16. - Thermal sample problem showing thermal distribution.

TABLE III. - THERMAL SAMPLE PROBLEM COMPARISON WITH EXACT SOLUTION

Element number	Exact temperature, °F	Calculated temperature, °F	Percent error	Element number	Exact temperature, °F	Calculated temperature, °F	Percent error
2	4.925	4.571	7.19	58	4.097	3.920	4.32
3	14.943	12.682	15.13	59	12.448	10.883	12.57
4	25.465	22.471	11.76	60	21.270	19.322	9.16
5	36.830	33.150	9.99	61	30.903	28.592	7.48
6	49.372	45.109	8.63	62	41.707	39.088	6.28
7	63.415	58.746	7.36	63	54.087	51.250	5.25
8	79.246	74.446	6.06	64	68.487	65.576	4.25
9	97.082	92.548	4.67	65	85.394	82.621	3.25
10	117.018	113.272	3.20	66	105.298	102.978	2.20
11	138.969	136.631	1.68	67	128.585	127.185	1.09
12	162.620	162.308	.19	68	155.300	155.304	.13
13	187.408	186.137	.68	69	184.744	183.395	.73
16	4.841	4.532	6.38	72	3.695	3.552	3.87
17	14.691	12.573	14.42	73	11.230	9.868	12.13
18	25.044	22.281	11.03	74	19.210	17.536	8.71
19	36.240	32.876	9.28	75	27.954	25.986	7.06
20	48.619	44.749	7.96	76	37.822	35.598	5.88
21	62.515	58.303	6.74	77	49.226	46.819	4.89
22	78.233	73.932	5.50	78	62.661	60.178	3.96
23	96.016	91.985	4.20	79	78.724	76.328	3.04
24	115.990	112.708	2.83	80	98.134	96.063	2.11
25	138.096	136.134	1.42	81	121.684	120.316	1.12
26	162.028	161.968	.04	82	149.987	150.003	.11
27	187.216	186.004	.65	83	182.681	180.937	.95
30	4.670	4.412	5.52	86	3.227	3.106	3.75
31	14.188	12.242	13.72	87	9.811	8.650	11.83
32	24.202	21.702	10.33	88	16.797	15.391	8.37
33	35.056	32.041	8.60	89	24.477	22.837	6.70
34	47.102	43.654	7.32	90	33.187	31.344	5.55
35	60.690	56.952	6.16	91	43.330	41.338	4.60
36	76.162	72.354	5.00	92	55.415	53.359	3.71
37	93.815	90.252	3.80	93	70.114	68.116	2.85
38	113.843	110.955	2.54	94	88.353	86.586	2.00
39	136.253	134.579	1.23	95	111.444	110.157	1.15
40	160.767	160.892	.08	96	141.150	140.806	.24
41	186.765	185.584	.63	97	178.863	175.963	1.62
44	4.425	4.207	4.93	100	2.705	2.574	4.84
45	13.437	11.678	13.09	101	8.227	7.260	11.75
46	22.941	20.716	9.70	102	14.091	12.941	8.16
47	33.276	30.616	7.99	103	20.551	19.220	6.48
48	44.802	41.774	6.76	104	27.899	26.411	5.33
49	57.897	54.618	5.66	105	36.497	34.896	4.39
50	72.951	69.603	4.59	106	46.814	45.168	3.52
51	90.343	87.192	3.49	107	59.503	57.913	2.67
52	110.384	107.809	2.33	108	75.544	74.148	1.85
53	133.215	131.727	1.12	109	96.548	95.518	1.07
54	158.647	158.871	.14	110	125.551	124.981	.45
55	185.989	184.781	.65	111	169.610	163.090	3.84

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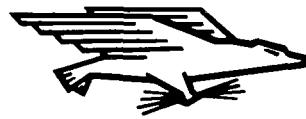
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